

REPORT DOCUMENTATION PAGE

Form Approved
OMB No. 0704-0188

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1. REPORT DATE (DD-MM-YYYY)		2. REPORT TYPE	3. DATES COVERED (From - To)		
4. TITLE AND SUBTITLE			5a. CONTRACT NUMBER		
			5b. GRANT NUMBER		
			5c. PROGRAM ELEMENT NUMBER		
6. AUTHOR(S)			5d. PROJECT NUMBER		
			5e. TASK NUMBER		
			5f. WORK UNIT NUMBER		
7. PERFORMING ORGANIZATION NAME(S) AND ADDRESS(ES)			8. PERFORMING ORGANIZATION REPORT NUMBER		
9. SPONSORING / MONITORING AGENCY NAME(S) AND ADDRESS(ES)			10. SPONSOR/MONITOR'S ACRONYM(S)		
			11. SPONSOR/MONITOR'S REPORT NUMBER(S)		
12. DISTRIBUTION / AVAILABILITY STATEMENT					
13. SUPPLEMENTARY NOTES					
14. ABSTRACT					
15. SUBJECT TERMS					
16. SECURITY CLASSIFICATION OF:			17. LIMITATION OF ABSTRACT	18. NUMBER OF PAGES	19a. NAME OF RESPONSIBLE PERSON
a. REPORT	b. ABSTRACT	c. THIS PAGE			19b. TELEPHONE NUMBER (include area code)

U.S. ARMY DEVELOPMENT COMMAND GROUND VEHICLE SYSTEMS CENTER

**Contrasting Intermediate-Temperature $\text{La}_{0.7}\text{Sr}_{0.3}\text{VO}_{3.86-5}$ (LSV) Catalyst
Elevated Sulfur Tolerance using Gaseous and Liquid Fuel Explored
through Experimental and Modeling Characterization over Time**

28 MAY 2023

Controlled by:	DEVCOM GVSC
Controlled by:	FPT Fuel's and Lubricant's Branch
CUI Category:	Controlled Technical Information
Distribution Statement:	A
POC:	Talia Marie Sebastian, PhD
POC:	Theodore Burye, PhD

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Unlimited. OPSEC #7546**

Motivation - SOFC Sulfur Contamination



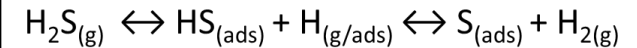
Fuel Flexibility and Anode Deactivation

- State-of-the-art (Ni/YSZ)
 - Nickel highly active toward electrochemical oxidation of sulfur, leading to sulfur poisoning and deactivation
 - Chemisorption (<50 ppm(v)), Sulfidation (>50 ppm(v))
 - Concentrations as low as 2 ppm(v) can cause irreversible damage.

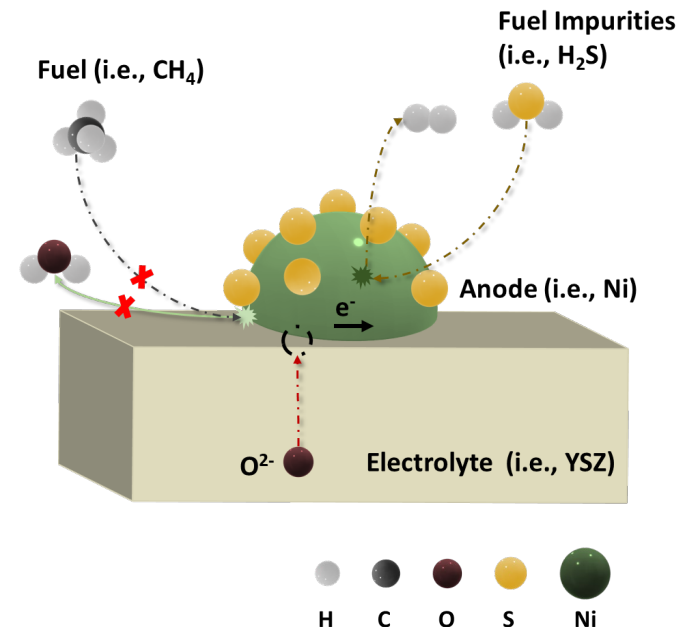
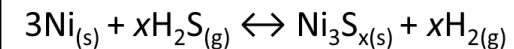
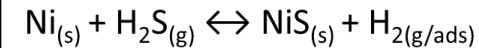
Material Strategies for Sulfur Tolerance

- Alloying nickel with noble or base metals
- Replacing nickel with base metals or nonmetal electronic conductors
- Replacing with mixed ionic-electronic conductors (i.e., Perovskite Oxides)

Mechanism of Chemisorption:

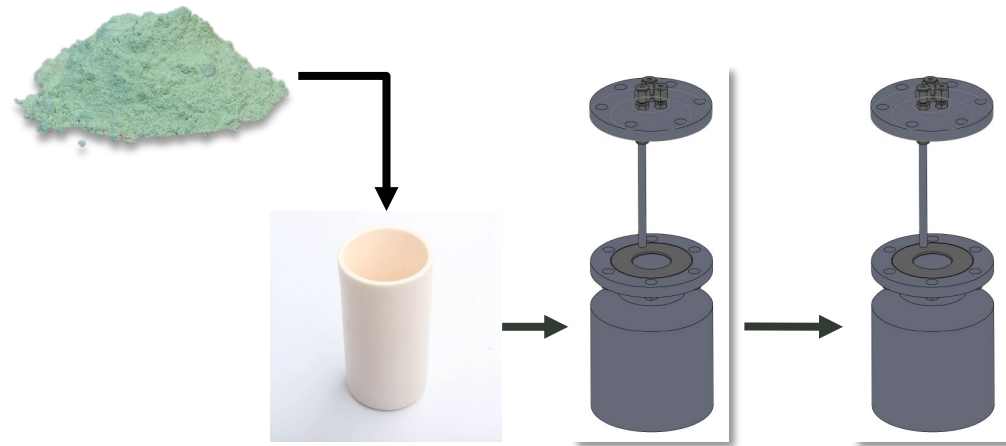
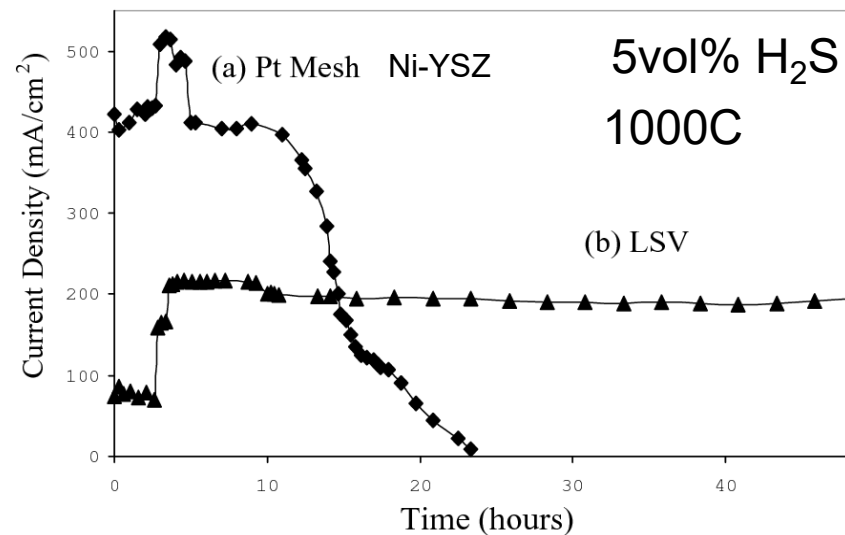


Mechanism of Sulfidation:



Adapted: DOI: 10.1016/j.jallcom.2017.11.381

Motivation – LSV Anode Catalyst Sulfur Tolerance



This study experimentally tested LSV powder:

- Heated under exposure to H₂S (hydrogen sulfide) and C₄H₄S (thiophene)
 - Up to 100 hours
- Changed atmosphere between H₂, CH₄ and CH₃OH
 - Investigated gaseous vs. liquid fuel impact
 - Investigated polar vs. non-polar fuel impact

This study characterized post-experimentation LSV samples:

- Sulfur adsorption characterized using SEM/EDS
- Sulfur adsorption characterized using XRD
- LSV interaction in different atmospheres modeled in parallel to experimentation

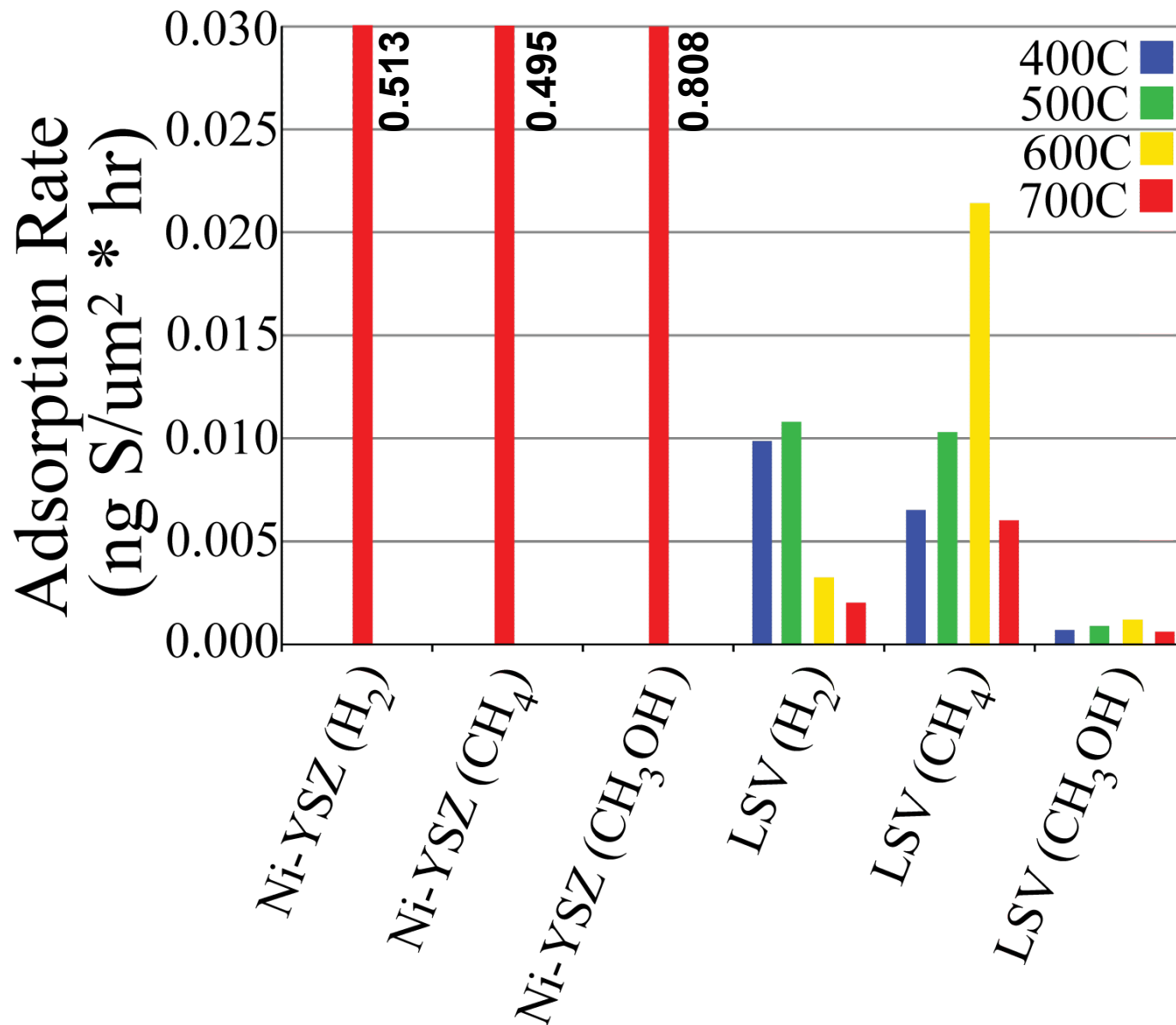
Experimental Results – Operating Parameters



Gas Pressure = 45 PSI Equivalent Flow Rate = 300 mL/min

Contaminant Concentration (ppm)	Mixture	Temperature (C)	Time (hours)
300	H ₂ S/H ₂	400	25-100 hours
300	H ₂ S/H ₂	500	25-100 hours
300	H ₂ S/H ₂	600	25-100 hours
300	H ₂ S/H ₂	700	25-100 hours
300	H ₂ S/CH ₄	400	25-100 hours
300	H ₂ S/CH ₄	500	25-100 hours
300	H ₂ S/CH ₄	600	25-100 hours
300	H ₂ S/CH ₄	700	25-100 hours
300	C ₄ H ₄ S/CH ₃ OH	400	25-100 hours
300	C ₄ H ₄ S/CH ₃ OH	500	25-100 hours
300	C ₄ H ₄ S/CH ₃ OH	600	25-100 hours
300	C ₄ H ₄ S/CH ₃ OH	700	25-100 hours

Experimental Results – Adsorption Rates



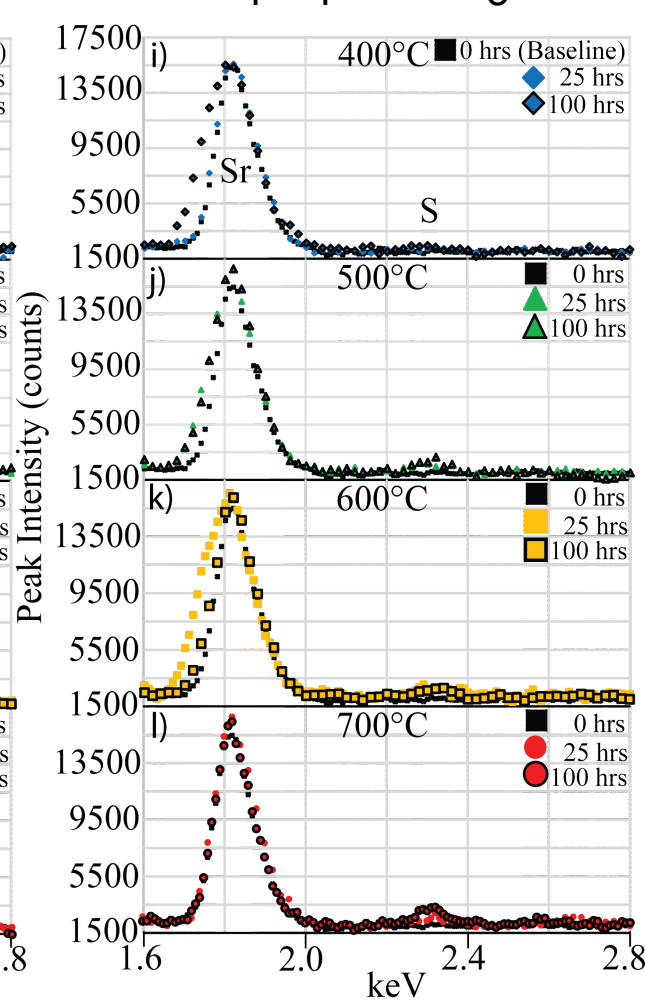
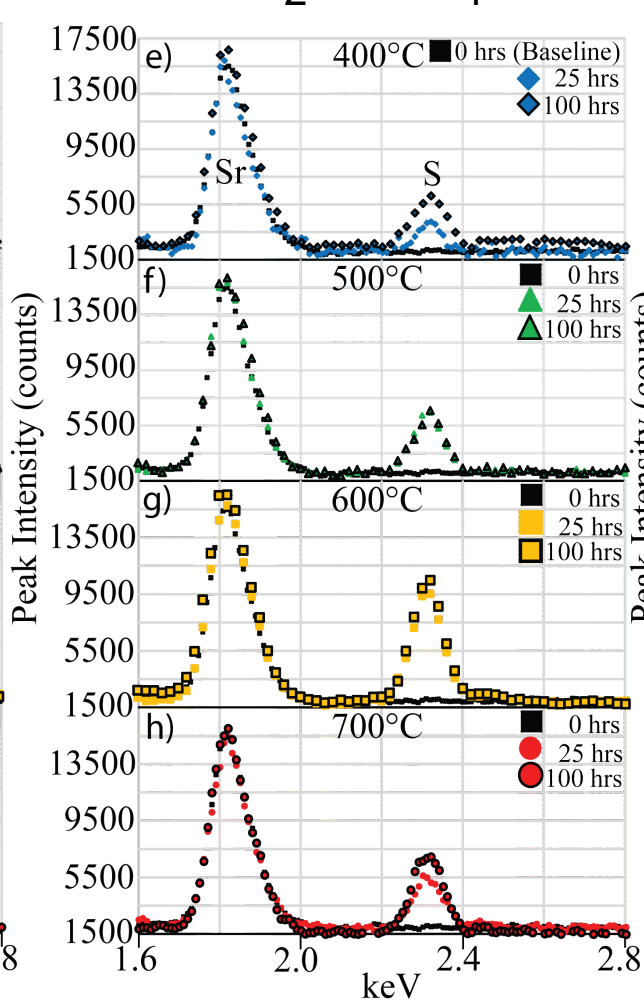
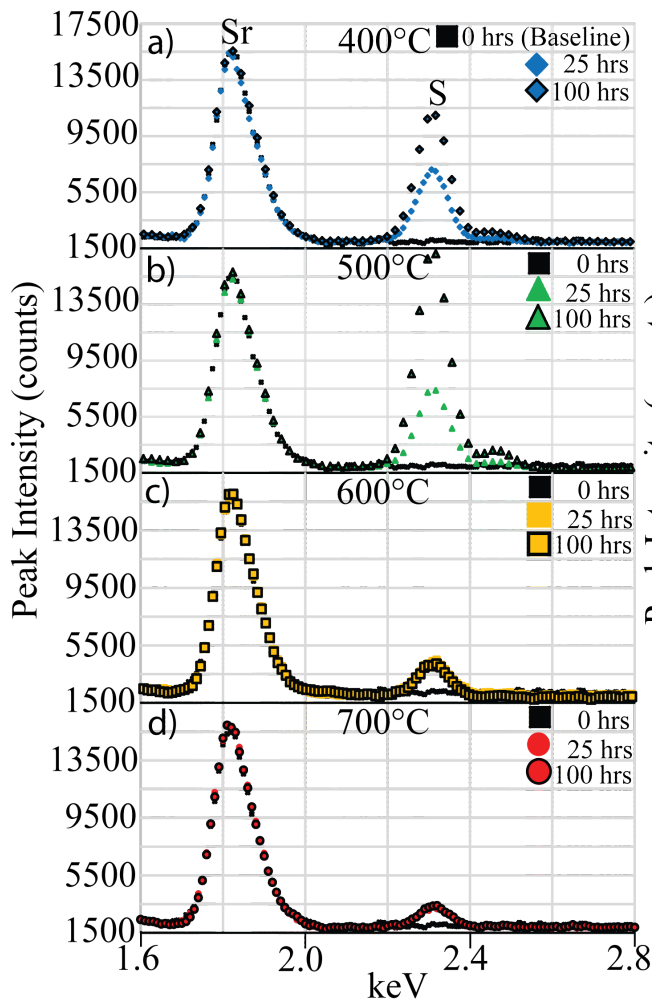
Experimental Results – 300ppm LSV Raw EDS



H_2S/H_2

H_2S/CH_4

C_4H_4S/CH_3OH



Experimental Results – 300ppm LSV Agglomerate Size

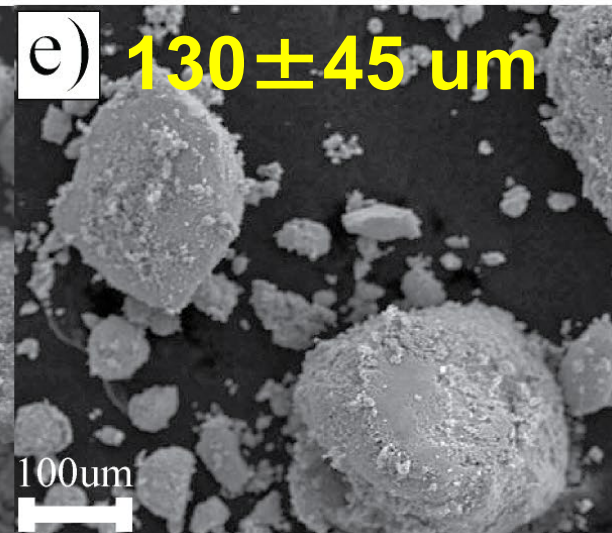
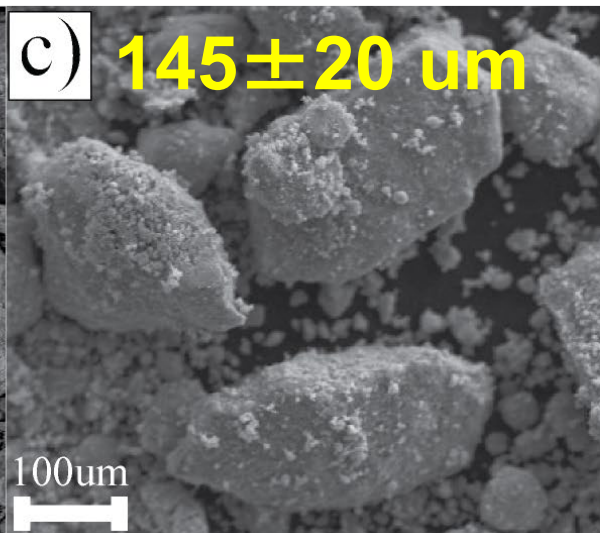
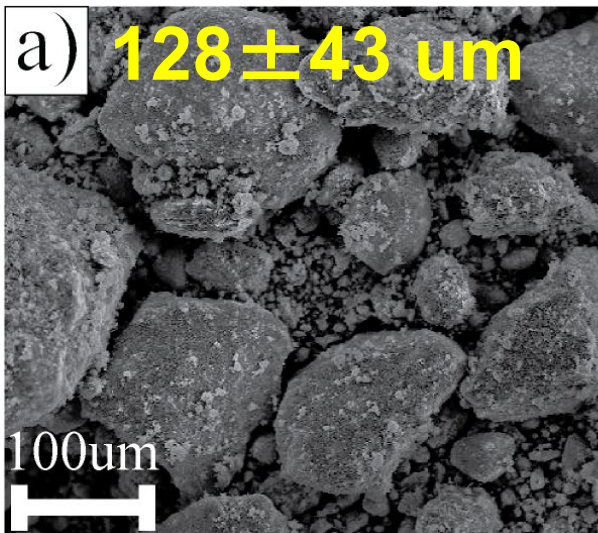


Hydrogen

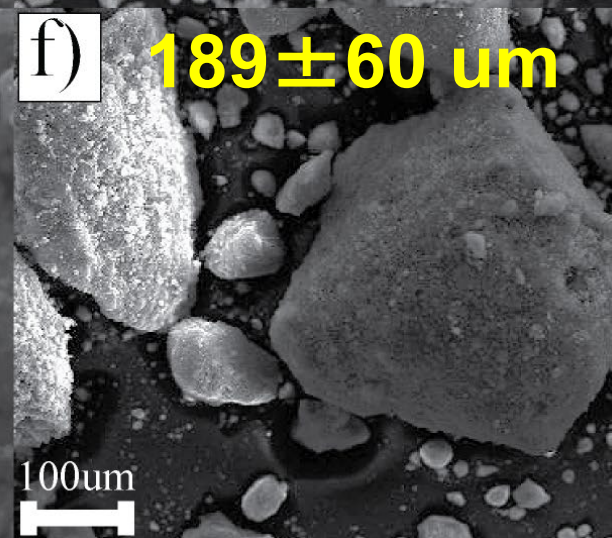
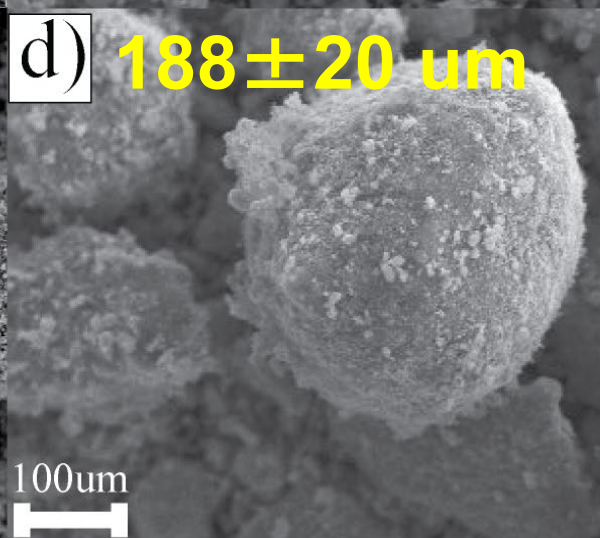
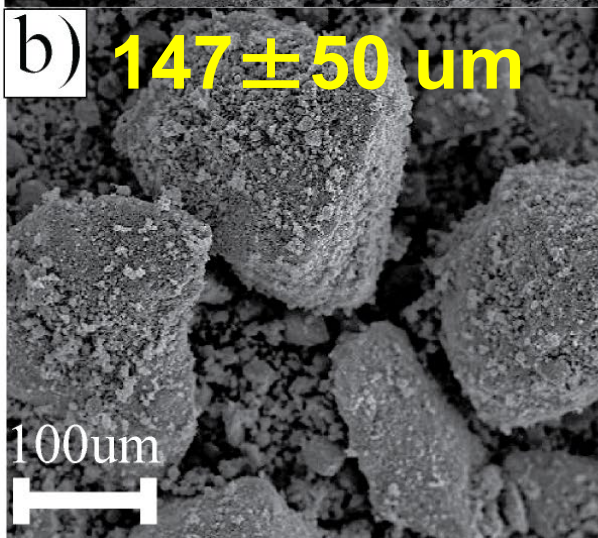
Methane

Methanol

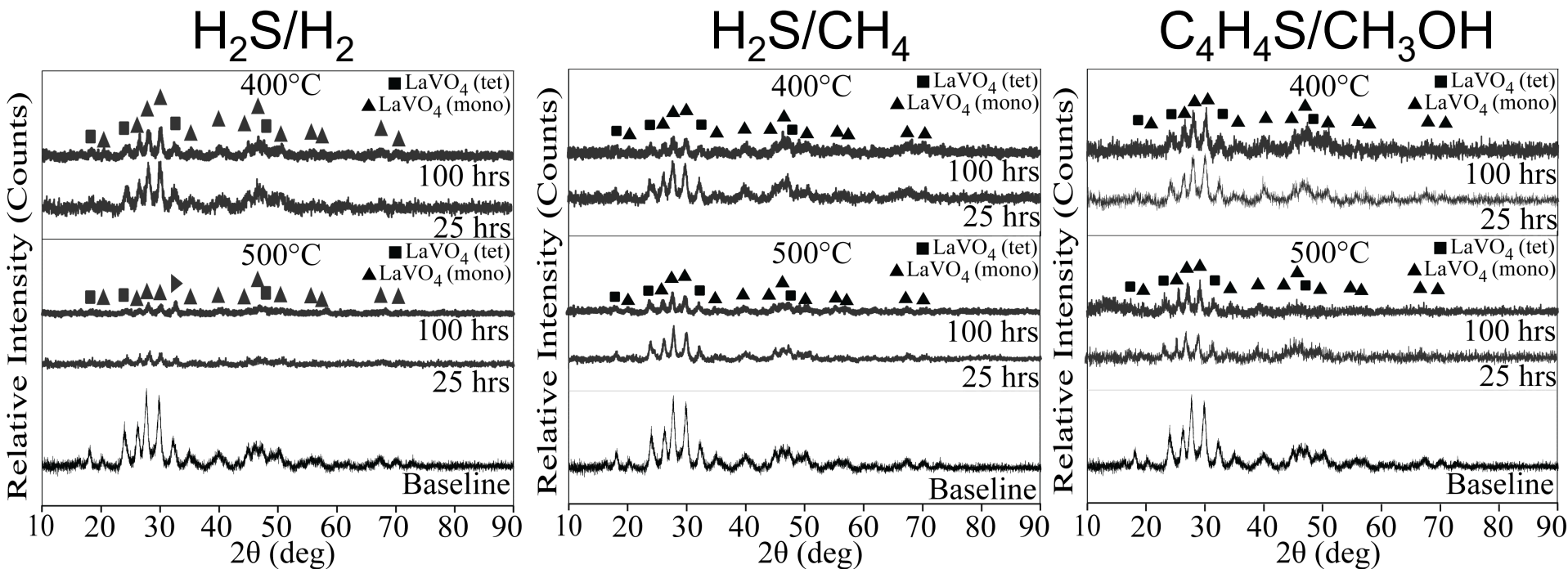
Smallest



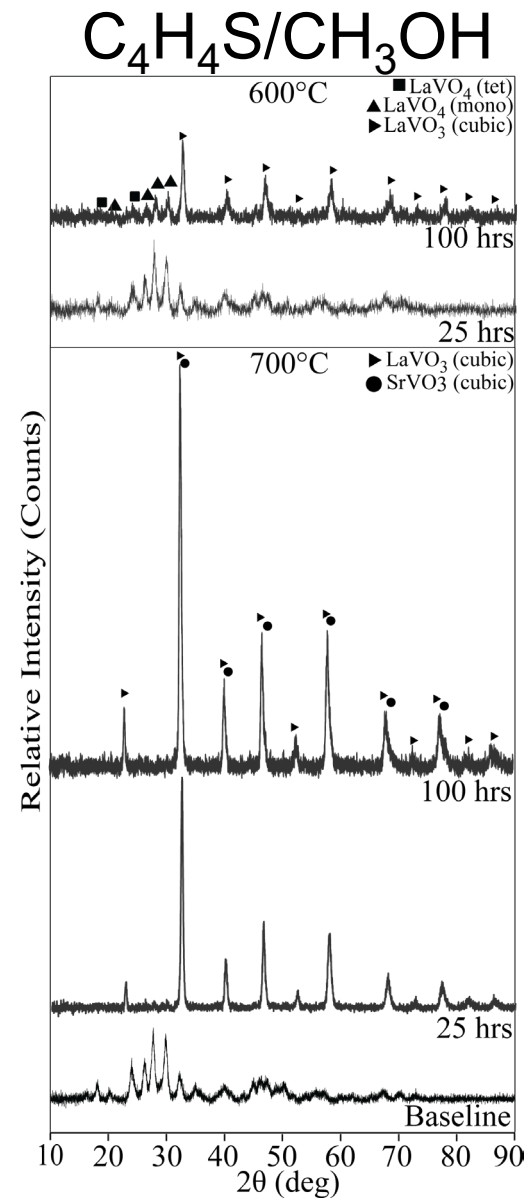
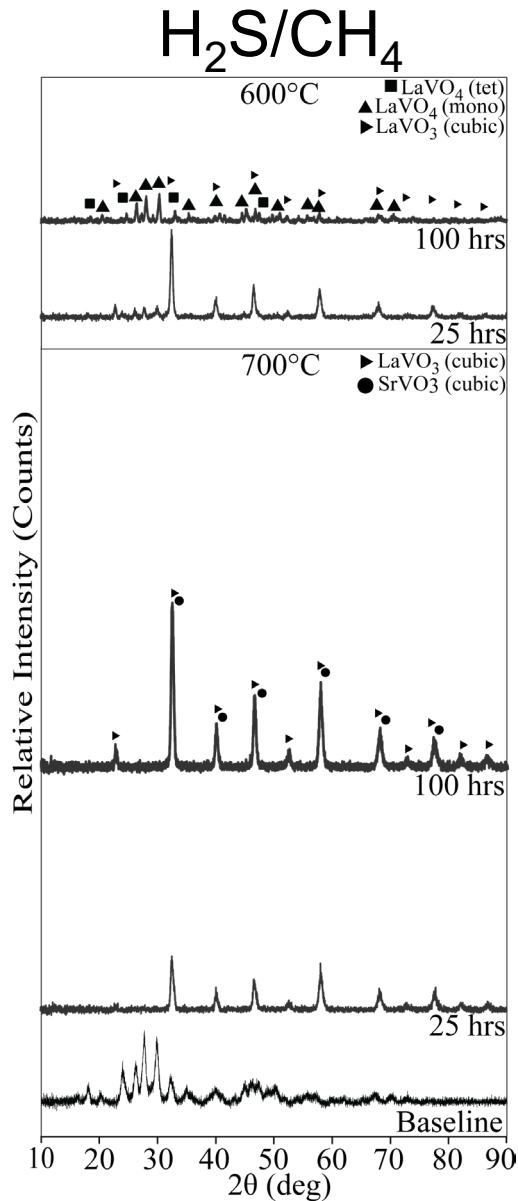
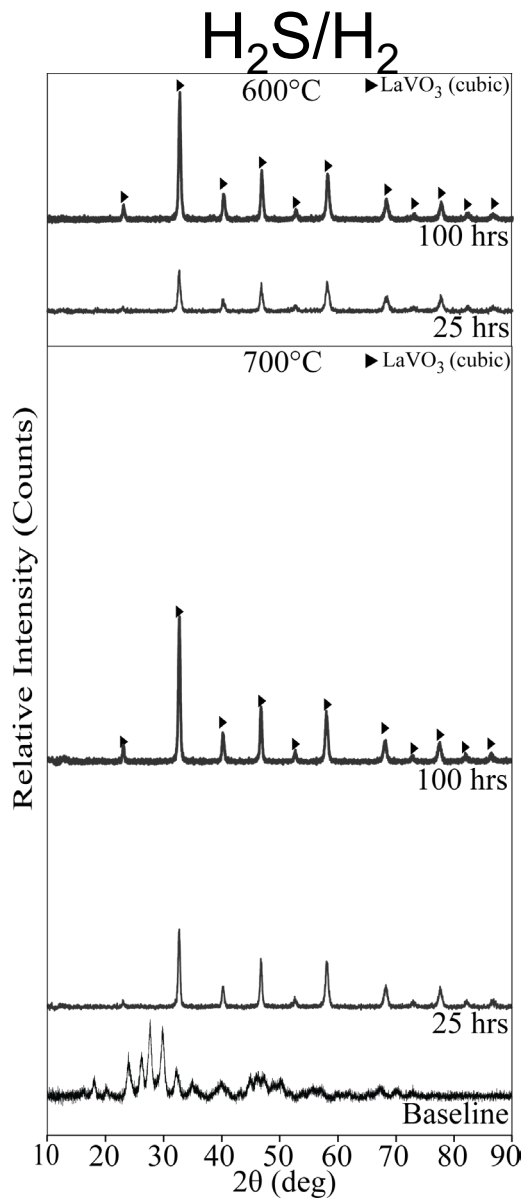
Largest



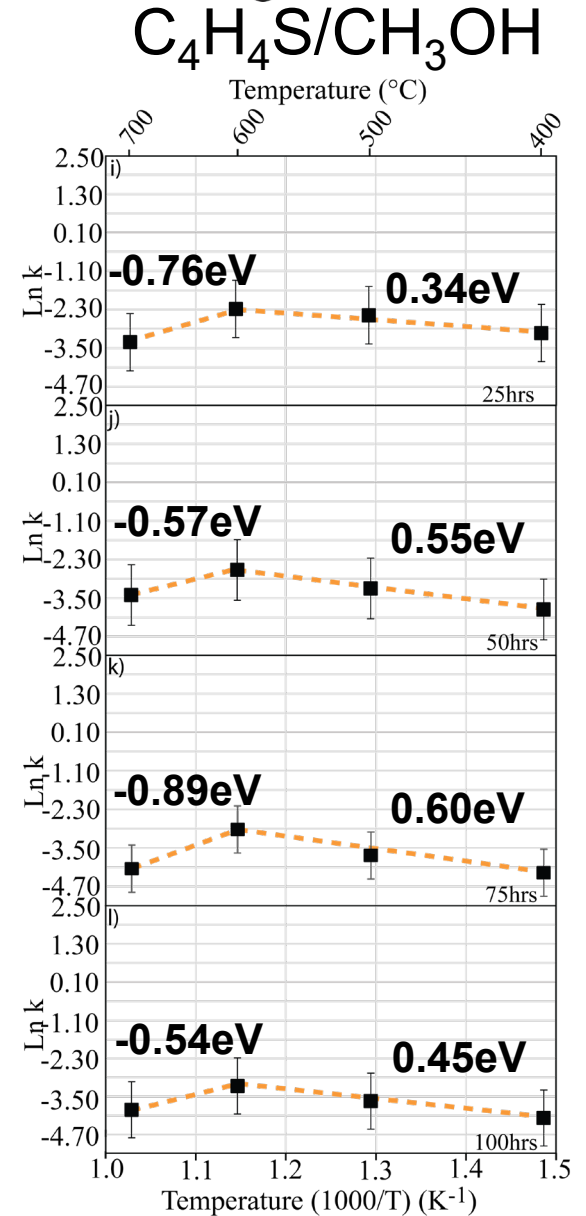
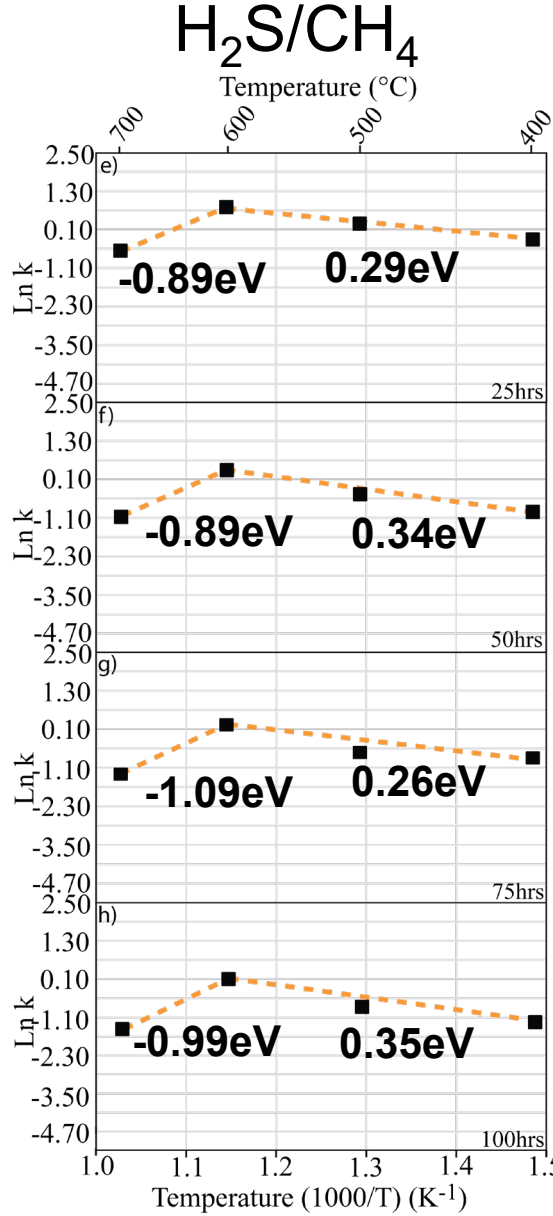
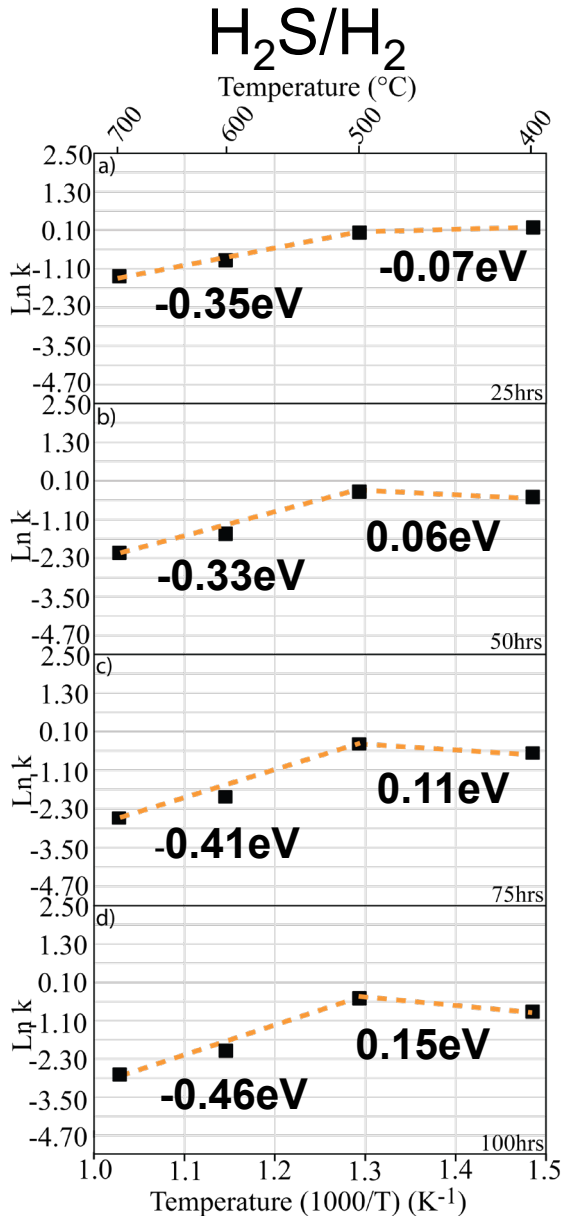
Experimental Results – 300ppm LSV Low-Temperature Raw XRD



Experimental Results – 300ppm LSV High-Temperature Raw XRD

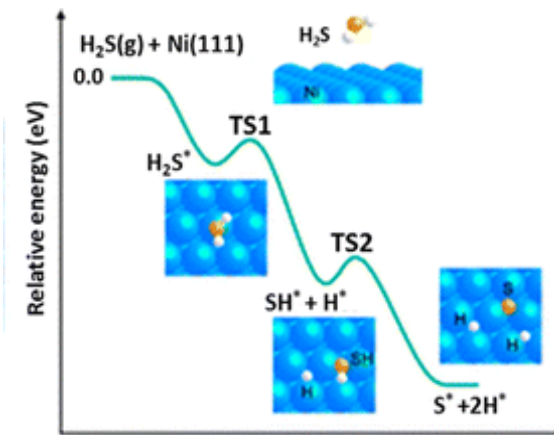
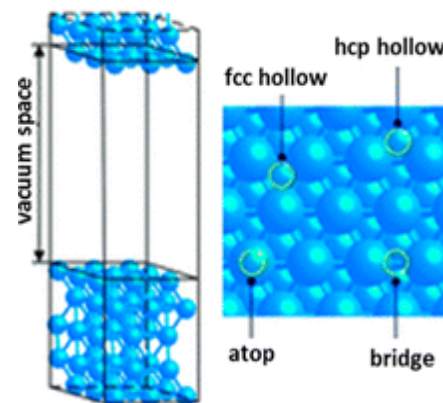
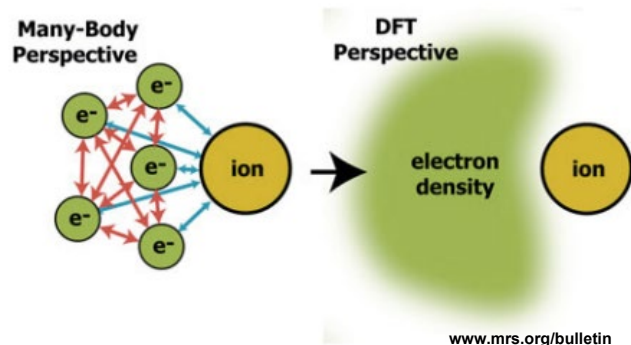


Experimental Results – 300ppm LSV Activation Energies



Theoretical Approach to Research Problem

Atomistic Modeling and Simulation



Density Functional Theory in Catalysis

- Atomic structures and surfaces
- Active sites and chemical states
- Adsorption and diffusion
- Electronic structure and distribution

Density Functional Theory Literature Ni/YSZ

- Adsorption of H₂S on nickel surfaces
- Two-step dissociative adsorption reaction
- Favorable reaction process

Density Functional Theory LSV Treatment

- VASP:DFT:GGA:PBEsol+U:520

Table 3. Activation Barriers (E_a) and Reaction Energies (ΔE) for the Elementary Steps in a H₂S Dissociative Adsorption Process and Adsorption Energies (E_{ads}) of Sulfur Species (S*, HS*, and H₂S*)^a

metal	E_{a1}^b	ΔE_1^b	E_{a2}^c	ΔE_2^c	$E_{\text{ads}}\text{S}^*$	$E_{\text{ads}}\text{HS}^*$	$E_{\text{ads}}\text{H}_2\text{S}^*$
Pt(111)(93)	0.02	-0.90	0.04	-1.19	5.14	3.00	0.90
Pd(111)(94)	0.37	-1.25	0.04	-0.73	5.15	3.02	0.71
Rh(211)(95)	0.01	-1.50	0.32	-1.50	6.0	3.69	1.00
Ni(100)(88)	0.29	-1.56	0.45	-1.05	5.96	3.72	0.83
Ni(111)(88)	0.15	-0.98	0.11	-0.86	5.14	2.95	0.67

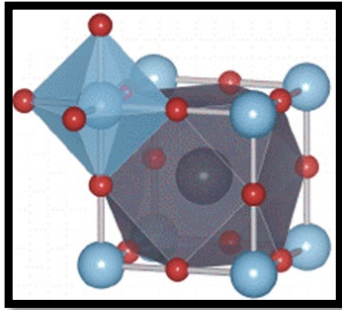
^aAll values in eV.

^b E_{a1} and ΔE_1 correspond to $\text{H}_2\text{S}^* \rightarrow \text{HS}^* + \text{H}^*$.

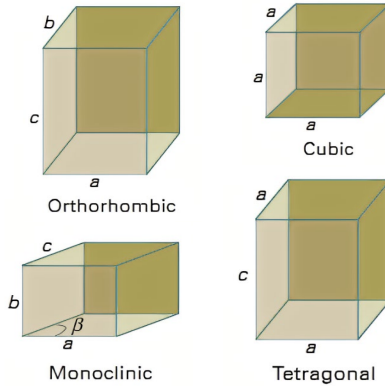
^c E_{a2} and ΔE_2 correspond to $\text{HS}^* \rightarrow \text{H}^* + \text{S}^*$.

DOI:10.1021/acs.chemrev.6b00284

Theoretical Details



DOI:10.1103/PhysRevB.89.134103



Lanthanum Vanadate (LaVO₃) - Reduced

- Orthorhombic: stable (Pnma)
 - $a = 5.677 \text{ \AA}$, $b = 7.942 \text{ \AA}$, $c = 5.591 \text{ \AA}$
 - $\alpha = 90.053^\circ$, $\beta = 90.115^\circ$, $\gamma = 90.003^\circ$
- Cubic: metastable (Pm $\bar{3}$ m)
 - $a = 3.950 \text{ \AA}$, $b = 3.950 \text{ \AA}$, $c = 3.950 \text{ \AA}$
 - $\alpha = 90.000^\circ$, $\beta = 90.000^\circ$, $\gamma = 90.000^\circ$
 - Decomposes to orthorhombic

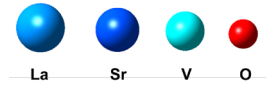
Lanthanum Orthovanadate (LaVO₄) - Oxidized

- Tetragonal: stable (I4₁/amd)
 - $a = 6.268 \text{ \AA}$, $b = 6.268 \text{ \AA}$, $c = 6.268 \text{ \AA}$
 - $\alpha = 106.091^\circ$, $\beta = 106.091^\circ$, $\gamma = 116.466^\circ$
- Monoclinic: metastable (P2₁/c)
 - $a = 7.353 \text{ \AA}$, $b = 6.804 \text{ \AA}$, $c = 8.463 \text{ \AA}$
 - $\alpha = 54.455^\circ$, $\beta = 90.000^\circ$, $\gamma = 90.000^\circ$
 - Decomposes to tetragonal

Lanthanum Vanadate (La_{0.7}Sr_{0.3}VO_{3±δ}) - Mixed

Hydrogen							
Temperature (C)	[H2S] (ppm)	Facet 1	Phase	Facet 2	Phase	Facet 3	Phase
400	30	(1,2,0)	Monoclinic	(0,1,2)	Monoclinic		
500	30	(1,1,0)	Cubic	(2,0,0)	Cubic		
600	30						
700	30	(1,1,0)	Cubic	(2,0,0)	Cubic		
400	300	(1,2,0)	Monoclinic	(0,1,2)	Monoclinic		
500	300	(1,2,0)	Monoclinic	(0,1,2)	Monoclinic		
600	300	(1,1,0)	Cubic	(2,0,0)	Cubic	(2,1,1)	Cubic
700	300	(1,1,0)	Cubic	(2,0,0)	Cubic	(2,1,1)	Cubic
Methane							
Temperature (C)	[H2S] (ppm)	Facet 1	Phase	Facet 2	Phase	Facet 3	Phase
400	30	(1,2,0)	Monoclinic	(0,1,2)	Monoclinic		
500	30	(1,2,0)	Monoclinic	(0,1,2)	Monoclinic		
600	30	(1,1,0)	Cubic	(2,0,0)	Cubic	(2,1,1)	Cubic
700	30	(1,1,0)	Cubic	(2,0,0)	Cubic	(2,1,1)	Cubic
400	300	(1,2,0)	Monoclinic	(0,1,2)	Monoclinic		
500	300	(1,2,0)	Monoclinic	(0,1,2)	Monoclinic		
600	300	(1,2,0)	Monoclinic	(0,1,2)	Monoclinic	(2,1,1)	Cubic
700	300	(1,1,0)	Cubic	(2,0,0)	Cubic	(2,1,1)	Cubic
Methanol							
Temperature (C)	[H2S] (ppm)	Facet 1	Phase	Facet 2	Phase	Facet 3	Phase
400	30						
500	30						
600	30						
700	30						
400	300	(1,2,0)	Monoclinic	(0,1,2)	Monoclinic		
500	300	(1,2,0)	Monoclinic	(0,1,2)	Monoclinic		
600	300	(1,1,0)	Cubic	(2,0,0)	Cubic	(2,1,1)	Cubic
700	300	(1,1,0)	Cubic	(2,0,0)	Cubic	(2,1,1)	Cubic

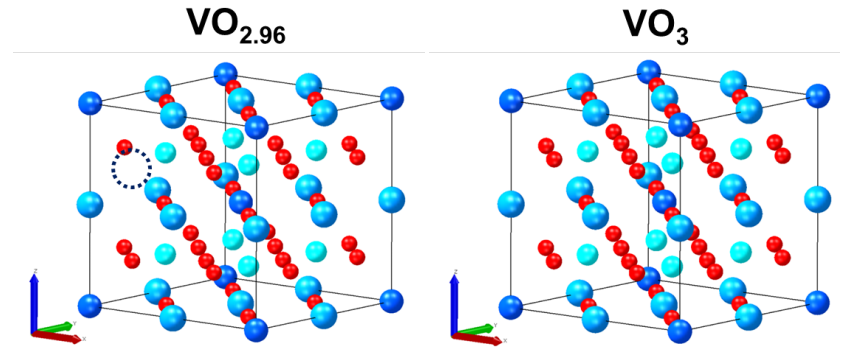
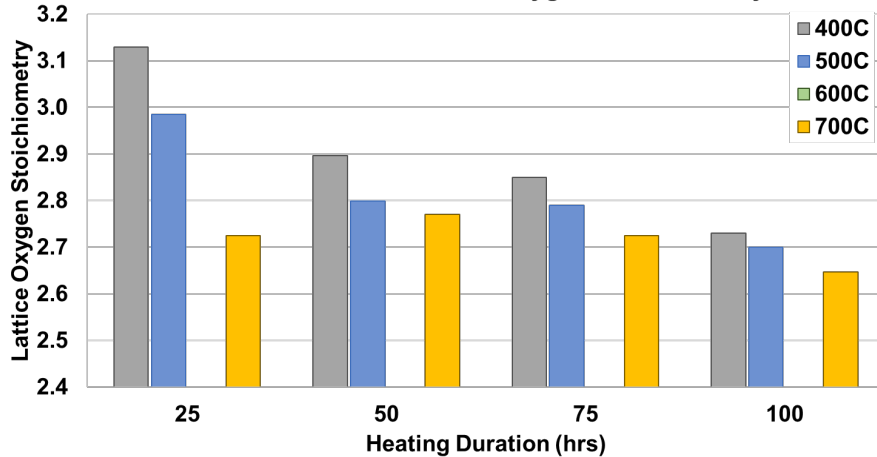
Theoretical Details Cont.



Lanthanum Strontium Vanadate ($\text{La}_{0.7}\text{Sr}_{0.3}\text{VO}_{3\pm\delta}$) – Mixed

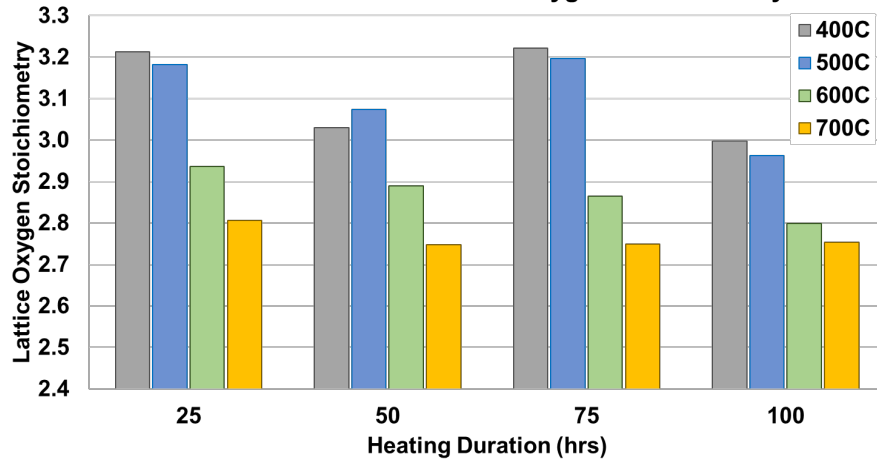
- Gas/temperature dependent oxygen stoichiometry
- Increased sulfur accumulation with increasing oxygen

LSV in H₂/H₂S Lattice Oxygen Stoichiometry

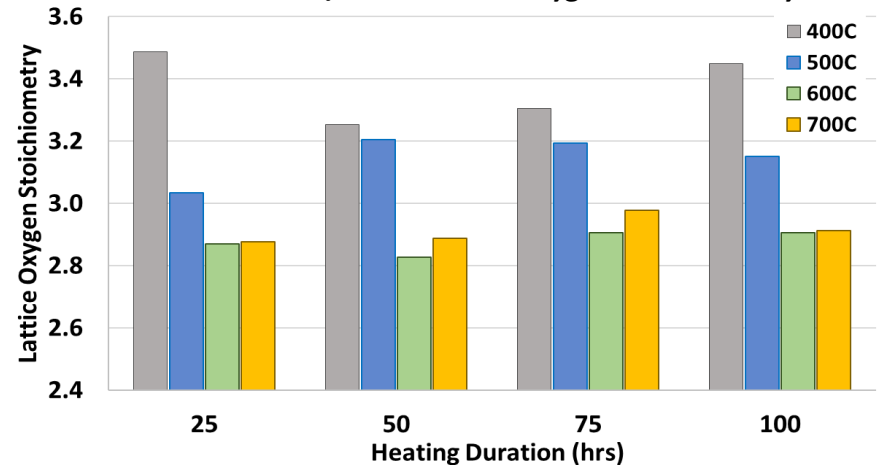


- Monoclinic → Tetragonal → **Cubic**

LSV in CH₄/H₂S Lattice Oxygen Stoichiometry



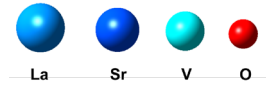
LSV in H₃COH/C₄H₄S Lattice Oxygen Stoichiometry



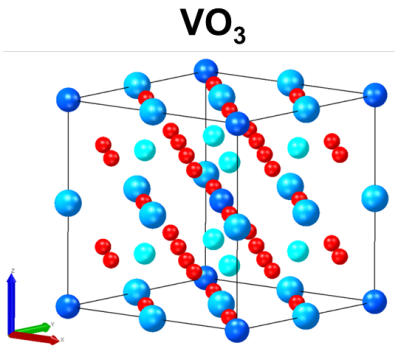
Theoretical Details Cont.



Lanthanum Strontium Vanadate ($\text{La}_{0.7}\text{Sr}_{0.3}\text{VO}_{3\pm\delta}$) – Cubic {200}, {110}, {211} Facets

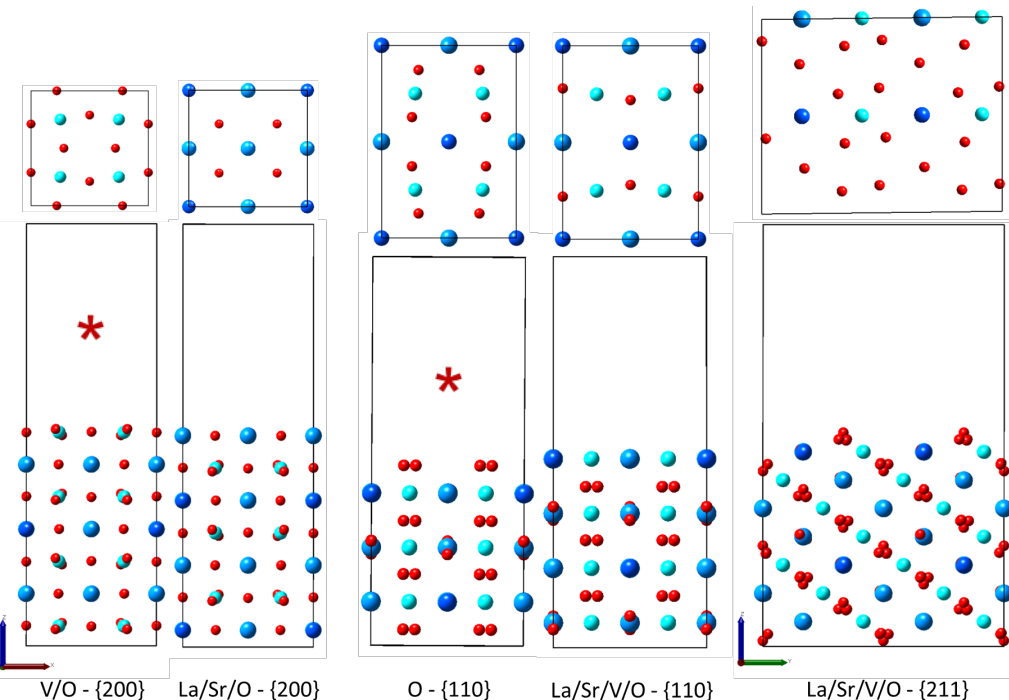
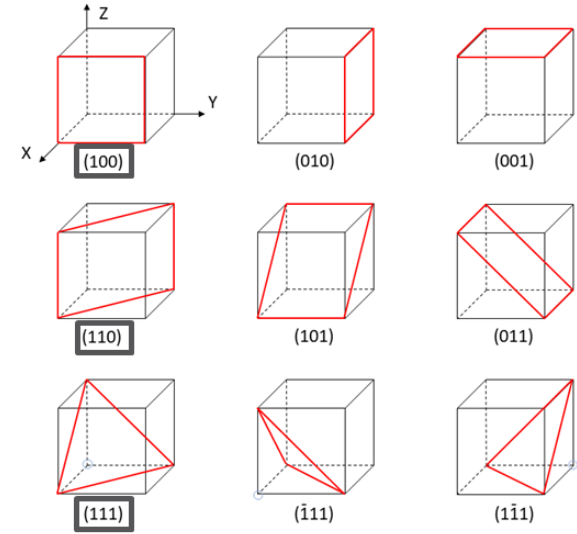


- Prominent cubic facets {110}, {200}, {211}

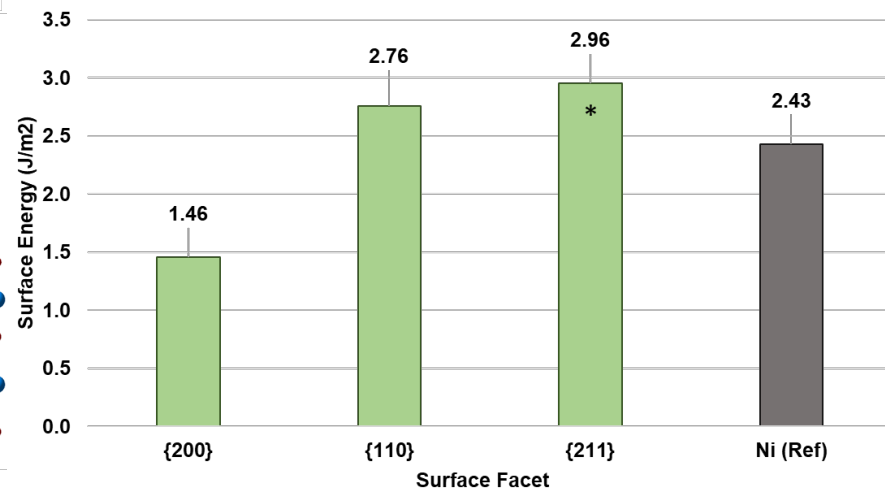


$$\sigma = \frac{E_{slab} - n(E_{bulk})}{2A}$$

$$\sigma = \frac{E_{slab-V/O} + E_{slab-La/Sr/O}}{2}$$



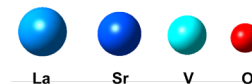
Theoretical Surface Energies of Prominent Oxygen Rich c-LSV



Theoretical Results



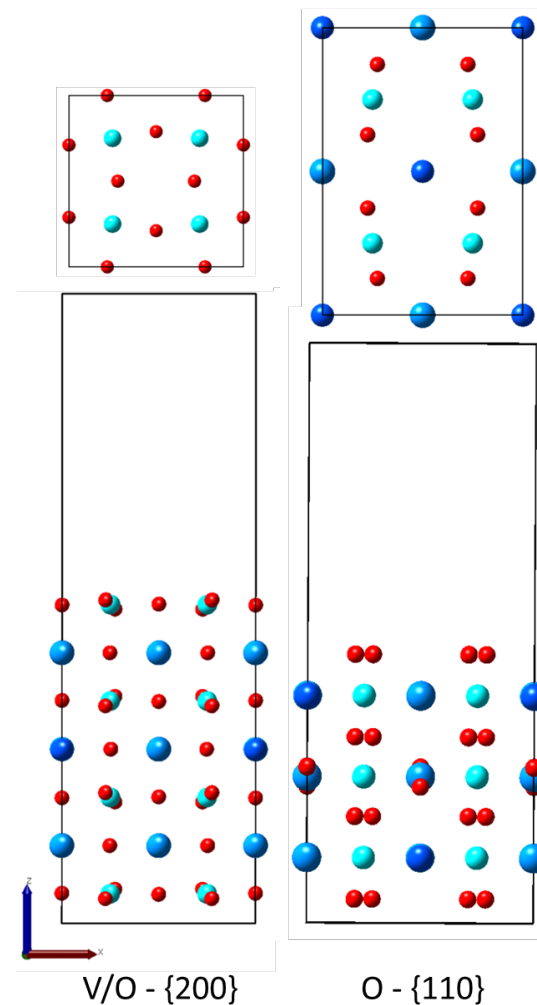
Lanthanum Strontium Vanadate ($\text{La}_{0.7}\text{Sr}_{0.3}\text{VO}_{3\pm\delta}$) – Cubic {200}, {110} Facets



$$E_{ads} = E_{slab + molecule} - (E_{slab} + E_{molecule})$$

Adsorption Energy (eV)

Termination	Ads Site	H ₂ S*	CH ₄ *	CH ₃ OH*
{200} V/O				
	Atop V	-0.45	-0.18	-0.83
	Atop O	-0.43	-0.02	-0.11
	Hollow	0.03	-0.03	-0.09
	Average	-0.28	-0.08	-0.34
{110} La/Sr/V/O				
	Atop La	-1.27	-1.15	-1.80
	Atop Sr	-1.16	-1.12	-1.67
	Bridge O	-0.83	-1.05	-1.63
	Hollow	-1.12	-1.07	-1.66
	Average	-1.10	-1.10	-1.69



Theoretical Results

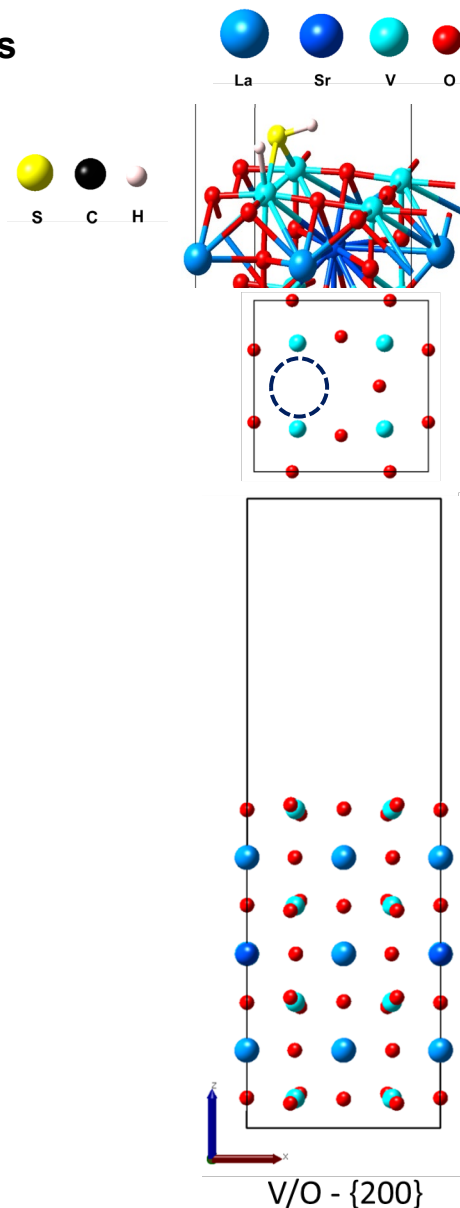


Lanthanum Strontium Vanadate ($\text{La}_{0.7}\text{Sr}_{0.3}\text{VO}_{3\pm\delta}$) – Cubic {200}, {110} Facets

$$E_{ads} = E_{slab + molecule} - (E_{slab} + E_{molecule})$$

Adsorption Energy (eV)

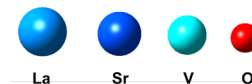
Termination	Ads Site	H2S*	HS*, H*	H*, S*, H*
{200} V/O	Atop V	-0.46		
	Atop O	-0.43		
	Atop V _o		-1.70	
	Hollow	0.01		
Termination	Ads Site	CH4*	H3C*, H*	CH2*, H*, H*
{200} V/O	Atop V	-0.23		
	Atop O	-0.03		
	Atop V _o	-0.46		
	Hollow	-0.04		
Termination	Ads Site	H3COH*	H3CO*, H*	H2C*, H*, O*
{200} V/O	Atop V	-0.85		
	Atop O*	-0.87		
	Atop V _o	-1.09		
	Hollow	-0.02		



Theoretical Results

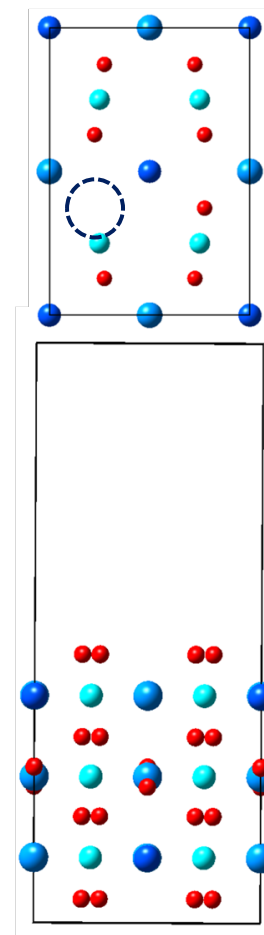


Lanthanum Strontium Vanadate ($\text{La}_{0.7}\text{Sr}_{0.3}\text{VO}_{3\pm\delta}$) – Cubic {200}, {110} Facets



$$E_{ads} = E_{slab + molecule} - (E_{slab} + E_{molecule})$$

Adsorption Energy (eV)					
Termination	Ads Site	H2S*	HS*, H*	H*, S*, H*	
{110} La/Sr/V/O					
	Hollow La	-0.30			
	Hollow Sr	-0.17			
	Bridge O	-0.20			
	Atop V_o	-0.45			
Termination	Ads Site	CH4*	H3C*, H*	CH2*, H*, H*	
{110} La/Sr/V/O					
	Hollow La	-0.12			
	Hollow Sr	-0.17			
	Bridge O	-0.06			
	Atop V_o	-0.18			
Termination	Ads Site	H3COH*	H3CO*, H*	H2C*, H*, O*	
{110} La/Sr/V/O					
	Hollow La	-0.69			
	Hollow Sr	-0.90			
	Bridge O	-0.80			
	Atop V_o	-1.15			



O - {110}

Theoretical Results



Lanthanum Vanadate ($\text{La}_{0.7}\text{Sr}_{0.3}\text{VO}_{3\pm\delta}$) – Mixed Cubic {200} H_2S Adsorption

- Higher surface energy with increasing oxygen deficit

$$E_f^O = E_{slab-O} - (E_{slab} + \mu_O)$$

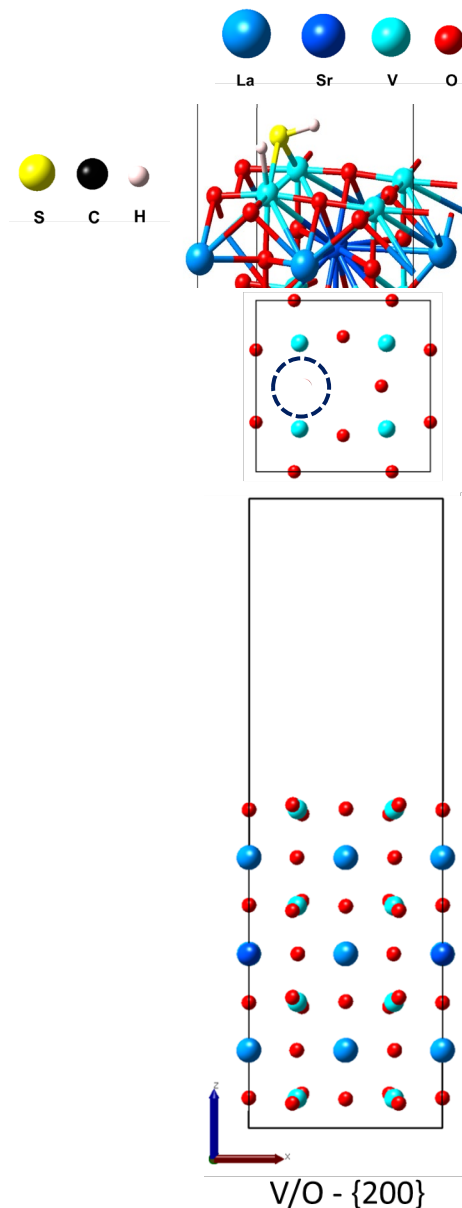
Surface Energy

Termination	Charge	σ (J/m ²)	Avg. σ (J/m ²)	E_f^O (eV/O atom)
{200} V/O	-7	-0.78	1.46	
	-5	0.62	2.16	5.52
	-3	1.94	2.82	4.95
	-1	3.30	3.50	5.23
	1	4.68	4.19	5.33
{200} Sr/La/O	0	3.70		

$$E_{ads} = E_{slab + molecule} - (E_{slab} + E_{molecule})$$

Adsorption Energy (eV)

Termination	Total Charge	Ads Site	H2S*	HS*, H*	H*, S*, H*
{200} V/O	-7	Atop V _o	-0.43		
	-5	Atop V _o		-1.70	
	-3	Atop V _o		-1.07	
	-1	Atop V _o		-1.06	
	1	Atop V _o		-1.06	



V/O - {200}

Current Conclusions



Experimental Results Conclusions

1. LSV shows significantly improved sulfur tolerance, compared to Ni-YSZ, across multiple fuel types (gaseous or liquid).
2. Methanol shows the most promise.
 1. Thiophene not as reactive.
 2. Methanol limiting sulfur interactions with LSV.
3. Generally, sulfur tolerance is lower $\leq 600\text{C}$.
 1. Cubic phase more sulfur tolerance. Occurs $\geq 600\text{C}$.
 2. Methanol is an exception.

Modeling Results Conclusions

1. LSV adsorbs H₂S, methane, and methanol through molecular adsorption on oxygen rich surfaces.
2. Slightly stronger adsorption of methanol than H₂S, likely due to higher dielectric constant of methanol.
3. Oxygen rich LSV can adsorb H₂S through barrierless one-step dissociative chemisorption, reacting with surface oxygen, leading to La/Sr-SH and V-OH bonds, in presence of oxygen vacancies.
4. LSV adsorbs H₂S on oxygen deficient surfaces through molecular adsorption, as well as with barrierless one-step dissociative chemisorption, reacting with surface La/Sr, leading to La/Sr-SH and La/Sr-OH bonds in the presence of oxygen vacancies.

Acknowledgements



Office of the Chief Scientist, GVSC

Fuel Cell Technologies Branch, GVSC

Fuels and Lubricants Branch, GVSC

Water Treatment and Handling Branch, GVSC

Characterization and Failure Analysis Branch, GVSC



Backup Slides

Contaminate Selection Parameters

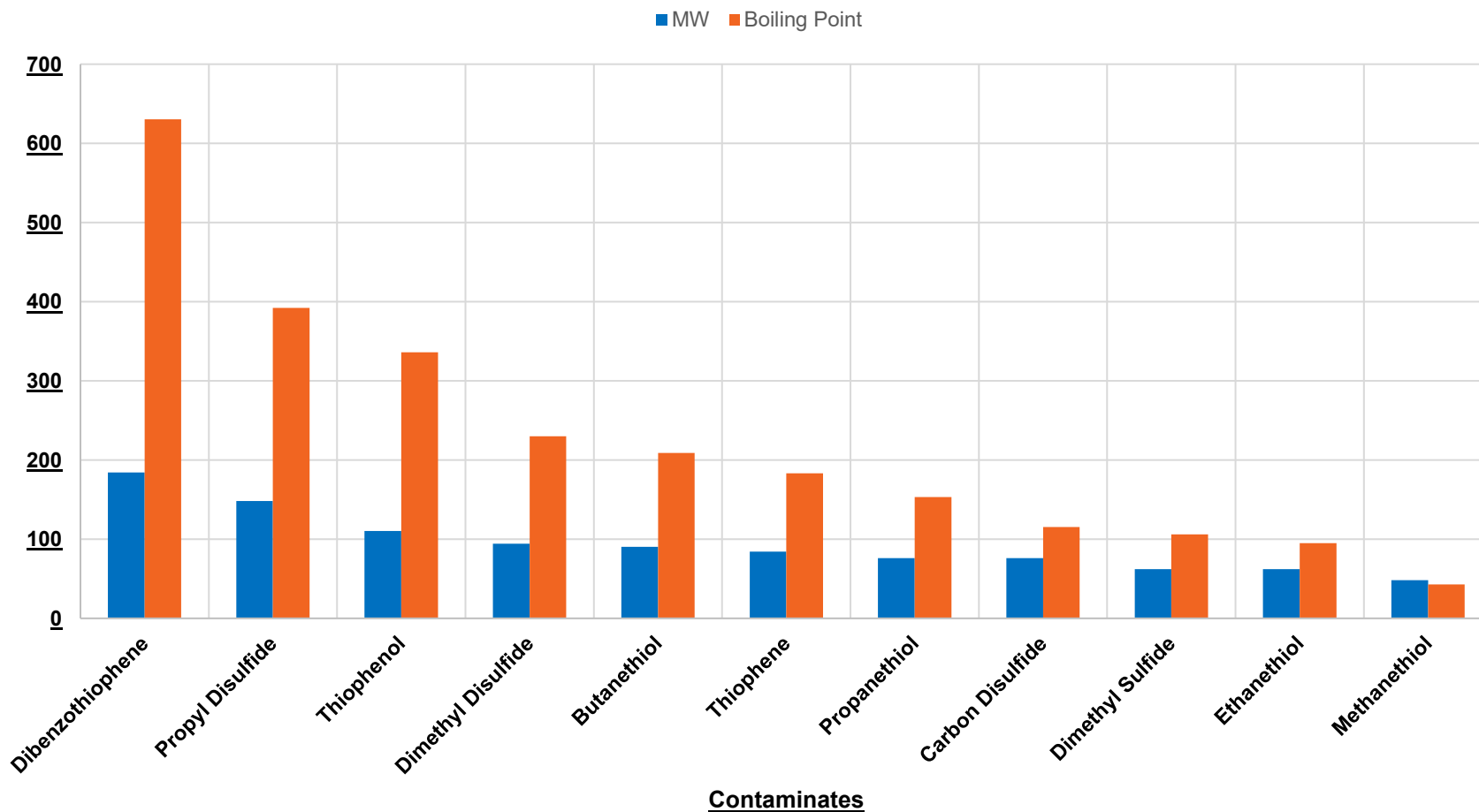


Contaminate Name	Room Temperature Phase	Boiling Temperature (°F)	Decomposition Temperature (°F)
Methanol	Liquid	148.5	1202-1382
Dibenzothiophene	Solid	630.5	
Allyl Propyl Disulfide	Liquid	392	
Dimethyl Disulfide	Liquid	230	1150 ²
Butanethiol	Liquid	208.8	
Thiophene	Liquid	183	2060
Propanethiol	Liquid	153	
Carbon Disulfide	Liquid	115.23	>1832
Dimethyl Sulfide	Liquid	106	1470
Ethanethiol	Liquid	95	1340-1880
Hydrogen Sulfide	Gas	-75.19	
Methanethiol	Gas	42.71	1349-1524

Contaminate Selection MW and Boiling Point Comparison



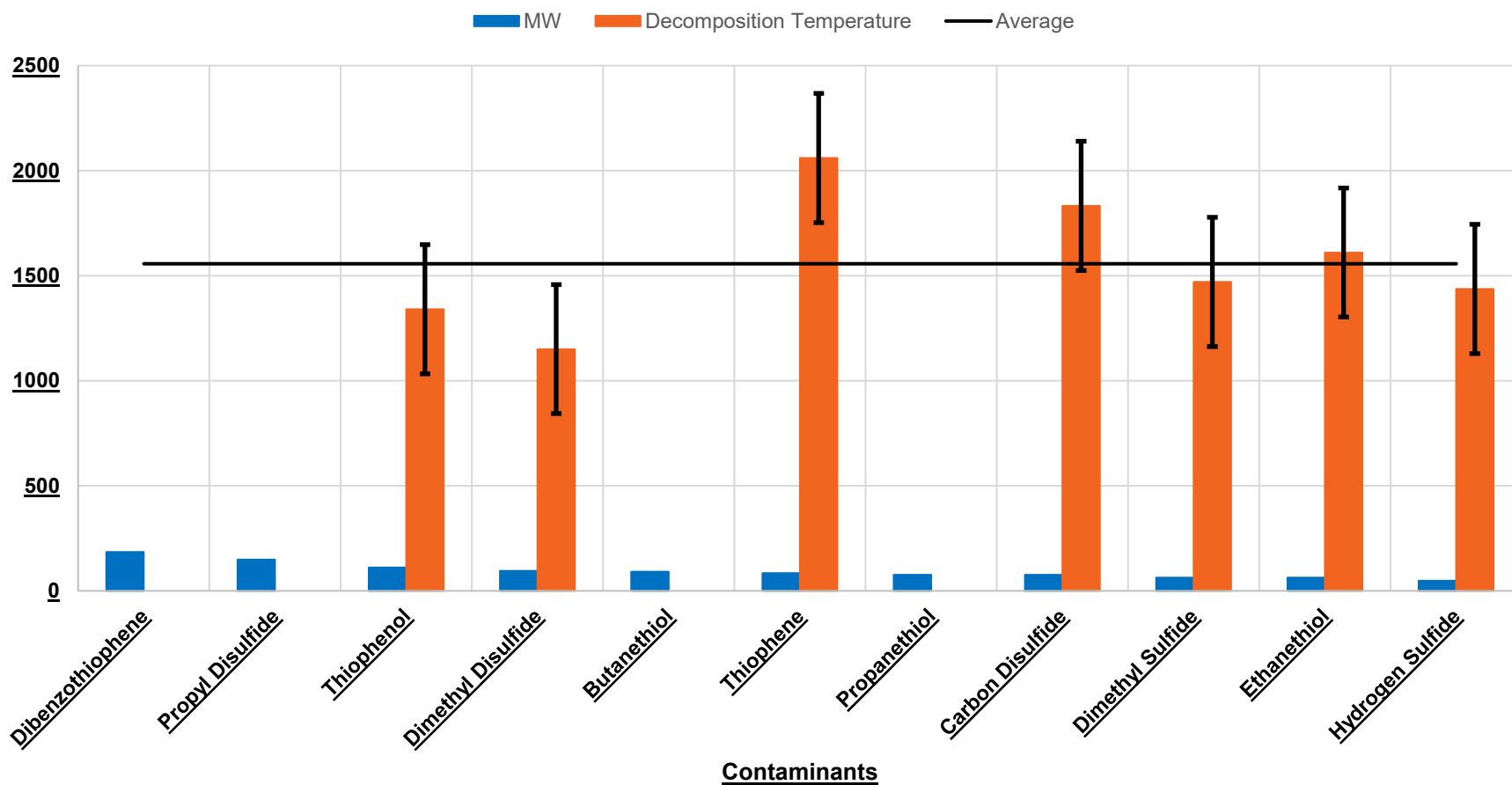
Sulfur Compound MW and Boiling Point (°F)



Contaminate Selection MW and Decomposition Temperature Comparison



Sulfur Compound MW and Decomposition Temperature (°F)



Experimental Results – Adsorption Rates 10vol% 700C



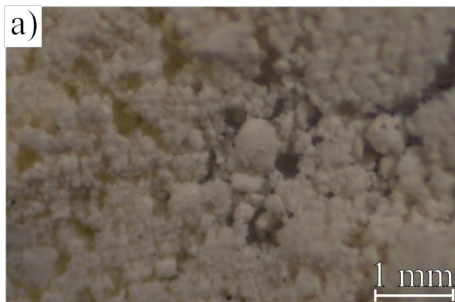
Experimental Results – Optical Microscopy



La = +3

Sr = +2

Untested
LSV Oxide
Powder



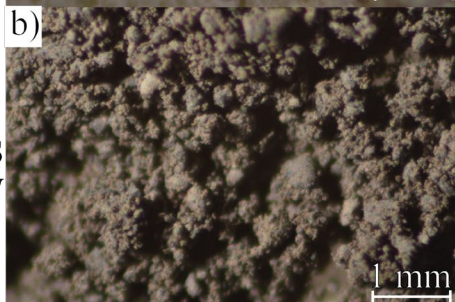
Cream



STANFORD
ADVANCED MATERIALS

V = +5

30ppm H₂S
400°C LSV
Oxide



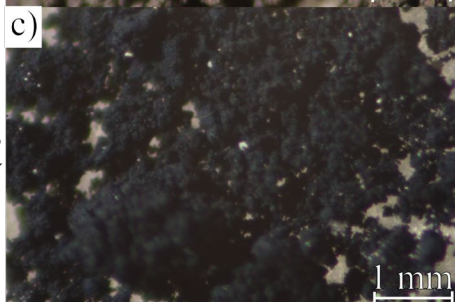
Brown/Yellow



STANFORD
ADVANCED MATERIALS

V = +5

30ppm H₂S
500°C LSV
Oxide



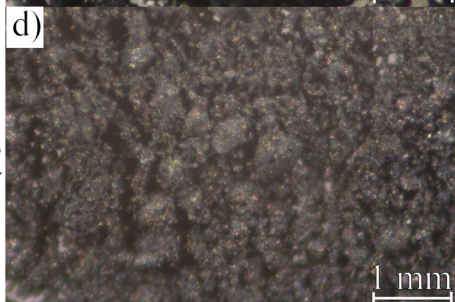
Dark Blue



STANFORD
ADVANCED MATERIALS

V = +4

30ppm H₂S
700°C LSV
Oxide



Black



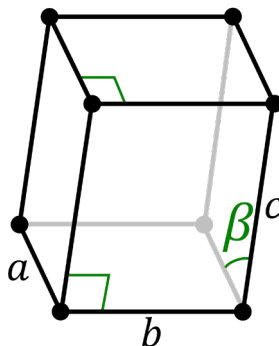
STANFORD
ADVANCED MATERIALS

V = +3

Experimental Results – Crystal Structures

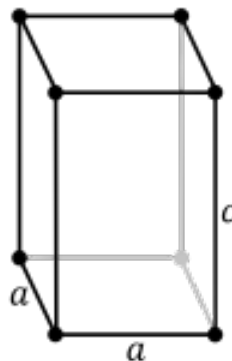


Monoclinic



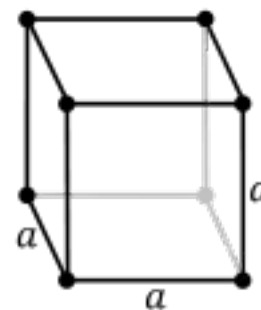
$$a \neq b \neq c$$
$$\alpha = \gamma = 90 \neq \beta$$

Tetragonal



$$a = b \neq c$$
$$\alpha = \gamma = \beta = 90$$

Cubic



$$a = b = c$$
$$\alpha = \gamma = \beta = 90$$

Experimental Results – Activation Energy Calculation



$$R_{ads,act} = k * P_{gas,partial}^x$$



$$P_{gas,partial} = P_{gas} * X_{H_2S}$$

$X = \text{kinetic order (assume 1)}$

$k = \text{kinetic rate constant}$

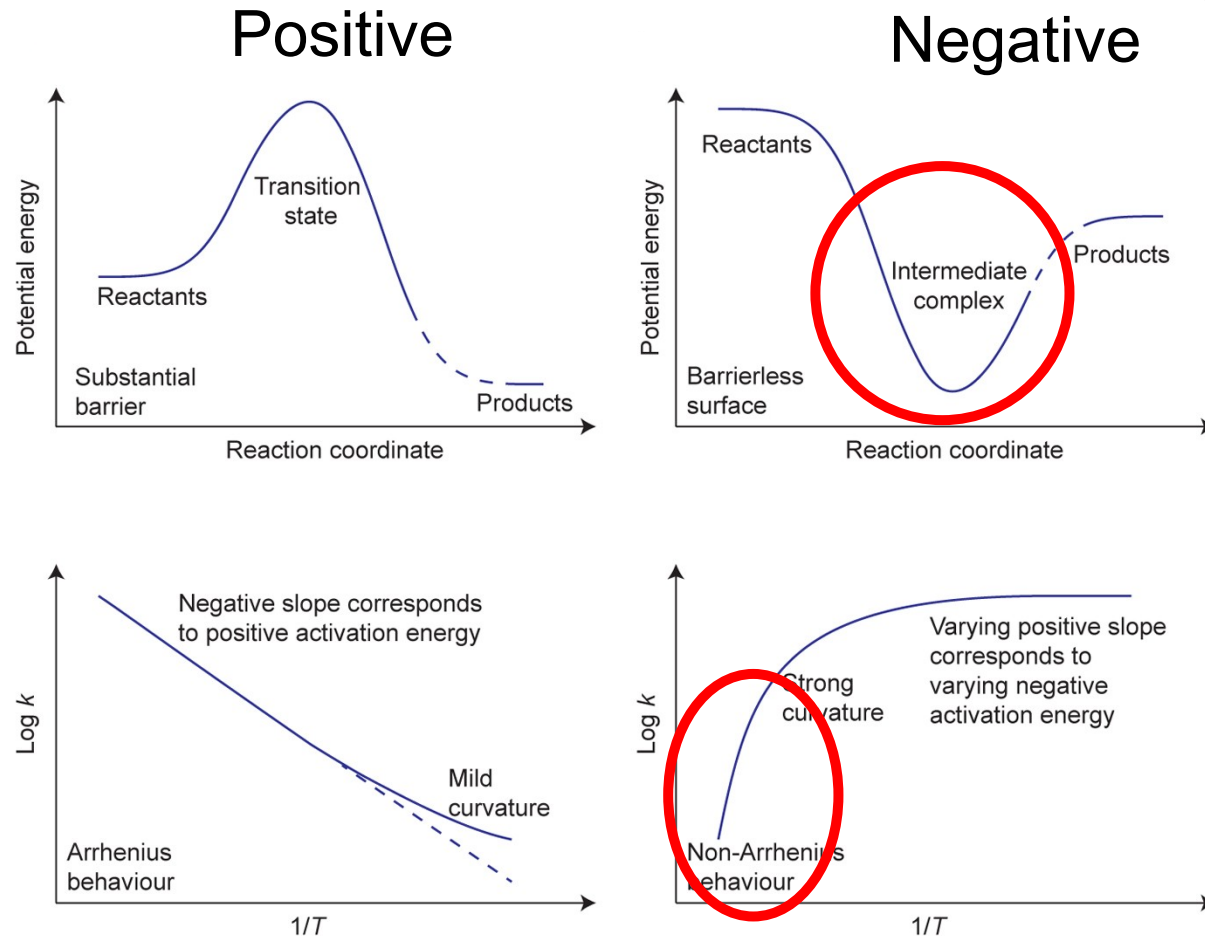


$X_{H_2S} = H_2S \text{ Mol Fraction}$

$P_{gas} = \text{Gas Pressure on Sample (45 PSI)}$

- Experimental and Kinetic Model Adsorption Rate Assumed Equal
- Kinetic Rate Constant Fitted to Match Experimental Adsorption Rate
 - Rate Constant Used to Determine Activation Energy

Experimental Results – Negative Activation Energy



- Negative Activation Energy
 - Barrierless Reaction
 - Capture of Molecules in a Potential Well
 - Higher Temperature Drives more Molecules from Well
 - Less Negative Value has Greater Reaction Barrier

Experimental Results – Activation Energy Calculation



$$k = A * e^{\frac{-E_a}{R * T}} \longrightarrow \ln(k) = \frac{-E_a}{R * T} + \ln(A)$$

R = Ideal Gas Constant

T = Temperature

E_a = Activation Energy (AE)
(Energy Barrier for Reaction to Occur)

A = Pre-Exponential Factor (PEF)
(Frequency of Collisions)

