

AD A117585

DTIC FILE COPY



(R)

ESL-TR-81-46

PREDICTIVE MODEL FOR JET ENGINE TEST CELL OPACITY

DR. GORDON A. LEWANDOWSKI
NEW JERSEY INSTITUTE OF TECHNOLOGY
323 HIGH STREET
NEWARK, NJ 07102

30 SEPTEMBER 1981

FINAL REPORT
1 JULY 1980 - 30 SEPTEMBER 1981

DTIC
ELECTE
S JUL 28 1982 D
A

APPROVED FOR PUBLIC RELEASE; DISTRIBUTION UNLIMITED



ENGINEERING AND SERVICES LABORATORY
AIR FORCE ENGINEERING AND SERVICES CENTER
TYNDALL AIR FORCE BASE, FLORIDA 32403, 15

82-07-37

NOTICE

PLEASE DO NOT REQUEST COPIES OF THIS REPORT FROM
HQ AFESC/RD (ENGINEERING AND SERVICES LABORATORY).

ADDITIONAL COPIES MAY BE PURCHASED FROM:

NATIONAL TECHNICAL INFORMATION SERVICE
5285 PORT ROYAL ROAD
SPRINGFIELD, VIRGINIA 22161

FEDERAL GOVERNMENT AGENCIES AND THEIR CONTRACTORS
REGISTERED WITH DEFENSE TECHNICAL INFORMATION CENTER
SHOULD DIRECT REQUESTS FOR COPIES OF THIS REPORT TO:

DEFENSE TECHNICAL INFORMATION CENTER
CAMERON STATION
ALEXANDRIA, VIRGINIA 22314

Unclassified

SECURITY CLASSIFICATION OF THIS PAGE (When Data Entered)

REPORT DOCUMENTATION PAGE		READ INSTRUCTIONS BEFORE COMPLETING FORM
1. REPORT NUMBER ESL-TR-81-46	2. GOVT ACCESSION NO. AD-A117585	3. RECIPIENT'S CATALOG NUMBER
4. TITLE (and Subtitle) PREDICTIVE MODEL FOR JET ENGINE TEST CELL OPACITY		5. TYPE OF REPORT & PERIOD COVERED FINAL REPORT July 1 1980-Sept. 30, 1981
		6. PERFORMING ORG. REPORT NUMBER
7. AUTHOR(s) DR. GORDON A. LEWANDOWSKI		8. CONTRACT OR GRANT NUMBER(s) FO 8635-80-C0222
9. PERFORMING ORGANIZATION NAME AND ADDRESS New Jersey Institute of Technology 323 High Street Newark, NJ 07102		10. PROGRAM ELEMENT, PROJECT, TASK AREA & WORK UNIT NUMBERS P.E. 62601 F JON: 1900-90-11
11. CONTROLLING OFFICE NAME AND ADDRESS AFESC/RDVS Tyndall AFB, Florida 32403		12. REPORT DATE September 30, 1981
		13. NUMBER OF PAGES 72
14. MONITORING AGENCY NAME & ADDRESS (if different from Controlling Office)		15. SECURITY CLASS. (of this report) UNCLASSIFIED
		15a. DECLASSIFICATION/DOWNGRADING SCHEDULE
16. DISTRIBUTION STATEMENT (of this Report) Approved for public release; distribution unlimited		
17. DISTRIBUTION STATEMENT (of the abstract entered in Block 20, if different from Report)		
18. SUPPLEMENTARY NOTES Availability of this report is specified on verso of front cover.		
19. KEY WORDS (Continue on reverse side if necessary and identify by block number) Computer Program Test Cell Jet Engine Test Cell Visibility Light Scattering Opacity		
20. ABSTRACT (Continue on reverse side if necessary and identify by block number) A computer program (written in FORTRAN for a CDC 6600) was developed to predict the plume opacity of jet engine test cells. The data input required for the model includes: the particle density, concentration, and size distribution in the exhaust gas, and the effective stack diameter. Previous data obtained for J-57 engines were used to test the model, and the difference		

Unclassified

SECURITY CLASSIFICATION OF THIS PAGE (When Data Entered)

Unclassified

SECURITY CLASSIFICATION OF THIS PAGE(When Data Entered)

between the theoretical and measured transmittance was generally within one percent.

The program also predicts the theoretical effect of using electrostatic precipitators or venturi scrubbers to treat the exhaust emissions. These predictions indicate that control devices larger than the test cells would have to be installed to even achieve a minimal effect on the observed visibility.

Section For	
SECRET	☒
CONFIDENTIAL	☐
Unannounced	☐
Justification	
By	
Distribution/	
Availability Codes	
Dist	Avail and/or Special
A	



Unclassified

SECURITY CLASSIFICATION OF THIS PAGE(When Data Entered)

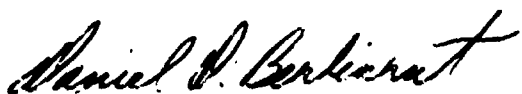
PREFACE

This report was prepared at the Department of Chemical Engineering, New Jersey Institute of Technology, 323 High Street, Newark, New Jersey 07102, under contract No. FO 8635-80-CO222 with the Air Force Engineering and Services Center, Tyndall Air Force Base, Florida 32403. Capt. D. Berlinrut managed the program for the Air Force Engineering and Services Center. The work was begun July 1, 1980 and completed September 30, 1981.

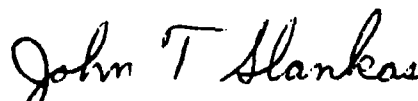
The author, Dr. Gordon A. Lewandowski, is indebted to the following individuals and organizations: Dr. W. Wong of New Jersey Institute of Technology for his valuable suggestions regarding stable generation of the complex Riccati-Bessel functions; Exxon Research & Engineering Co. (ERE) for release of their opacity computer program which was used to check the results of the program presented in this report; and S. Shaw of ERE for her efforts to obtain the release of their program and for guidance in its use.

This report has been reviewed by the Public Affairs Office and may be released to the National Technical Information Service (NTIS), where it will be available to the general public, including foreign nations.

This technical report has been reviewed and is approved for publication.



Daniel D. Berlinrut, Capt, USAF, BSC
Air Quality Research Engineer



John T. Slankas, Maj, USAF
Chief, Environmental Sciences
Branch



Michael J. Ryan, Lt Col, USAF, BSC
Chief, Environics Division



Francis B. Crowley, III, Col, USAF
Director, Engineering & Services
Laboratory

TABLE OF CONTENTS

Section	Page
I Introduction	1
II Smoke Number	4
III Visibility Equations	7
IV Electrostatic Precipitator Equations	14
V Scrubber Equations	16
VI Results & Discussion	19
References	24
Appendices	
A Computer Input Data Format	27
B Output Format	36
C FORTRAN Listing	49
D Computer Program Nomenclature	63

LIST OF FIGURES

Figure		Page
1	Generalized Test Cell Schematic	2
2	Relationship Between SAE Smoke Number & Sooty Density	5
3	SAE Smoke Number vs. Ringelmann Reading	6
4	Visibility	8
5	Black Plume Ringelmann Number Correlation with Transmittance	13
6	Log-Normal Plot of Size Distribution from Grems' Data	20

LIST OF TABLES

Table		Page
1	Comparison of Computer Predictions with Grems' Data for J57 Engine	21
2	Comparisons of Controlled and Uncontrolled Emissions	22

SECTION I

INTRODUCTION

A generalized schematic of a jet engine test cell is shown in Figure 1. Generally, the width of a plume issuing from a test cell is approximated by the stack dimension. The stacks are usually square; however, they contain acoustical baffles which considerably reduce the open area. For the calculations made in this report, the plume width was assumed to be the square root of the net open stack area.

Dimensions can vary considerably, depending upon the particular cell design, but the principle of operation is always the same. An engine that has been repaired, or otherwise maintained, is placed in the cell to test it under flight conditions before being remounted on the aircraft. The engine is considered a mobile emission source which is governed by Federal rather than state regulations. However, the test cell is immobile, and on that basis a U.S. District Court upheld the right of the State of California to regulate test cell emissions (Reference 1) which occasionally violate state visibility requirements of Ringelmann 1 (20% opacity). Since the U.S. Air Force has a large number of test cells in California, this court ruling can have a significant impact on Air Force operations and capital expenditures.

In order to satisfy state regulations, there are three possible alternatives: (1) design smokeless engines and install them on all existing aircraft; (2) introduce fuel additives to minimize soot formation; (3) use particulate control devices to treat the test cell exhaust.

The first of these alternatives is already being pursued as a result of the military incentive to reduce visibility of in-flight aircraft. However, replacement is very costly and time consuming, due to the variety and number of existing aircraft and aircraft engines.

The second alternative can be effective. However, fuel additives are organo-metallic compounds (e.g., Ferrocene), which deposit metallic oxides on engine surfaces. Considering the cost of the engine and its maintenance, and the cost of the aircraft, anything that may permanently alter engine parts is considered highly undesirable.

The third alternative does not affect the engine. Because of this, it is the only alternative which state regulatory authorities can impose. Nevertheless, particulate control

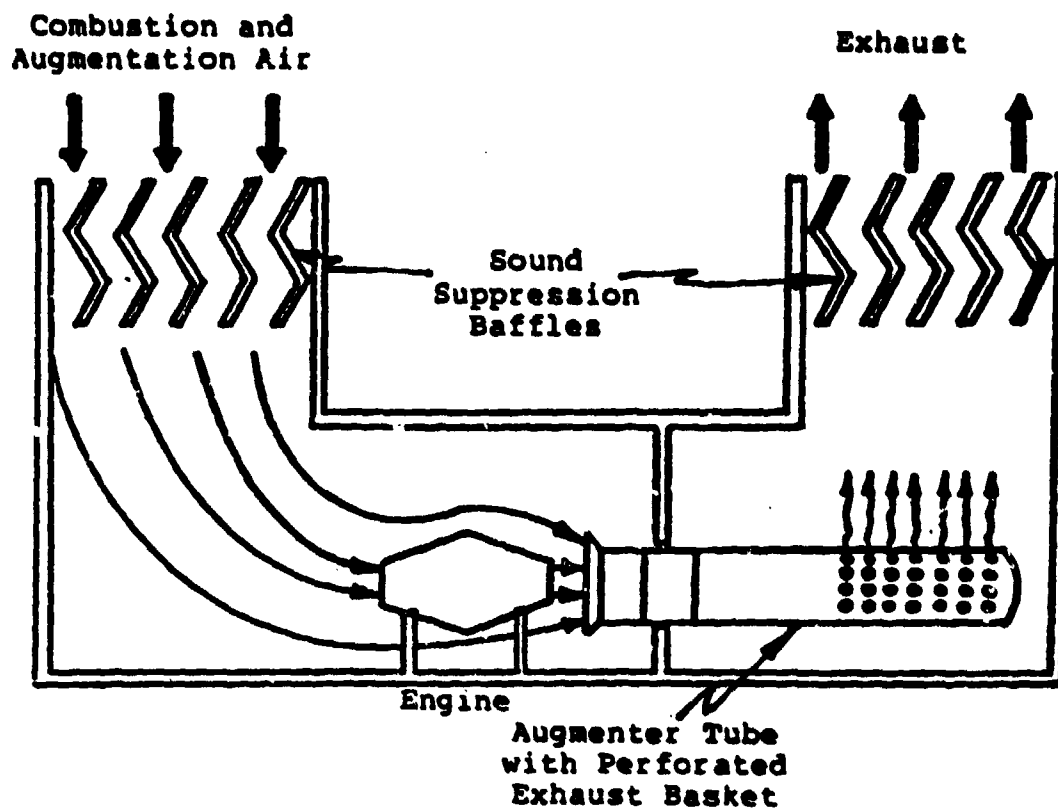


Figure 1. Generalized Test Cell Schematic

devices cannot be designed to meet an opacity requirement, only a specified degree of particulate removal.

The purpose of this study was to establish the connection between test cell particulate emissions and plume visibility as a basis for specifying control devices that could be mounted on the test cell exhaust stack. In addition, theoretical calculations were made to see under what conditions electrostatic precipitators or venturi scrubbers might satisfy opacity regulations.

SECTION II

SMOKE NUMBER

Much data on jet engine particulate emissions are in the form of SAE smoke numbers (SN), which measure the relative contrast of a standard filter paper exposed to the exhaust emissions for a standard period of time. A few investigators (References 2-6) have taken simultaneous measurements of particle loading ("soot density") and smoke number. Fewer studies (References 6-8) have determined plume opacity as a function of smoke number. These data, which are generally of poor quality, are plotted in Figures 2 and 3 for various engines.

Also presented in Figures 2 and 3 are empirical correlations based on Reference 9. The correlation in Figure 3 includes the results of Connor and Hodgkinson's work (References 10, 11) relating observed visibility to plume transmittance.

As can be seen, there is about as much error in predicting the Ringelmann number directly from the smoke number, as there is in predicting mass loading. However, in order to determine opacity from loading, the particle size distribution must be known (involving an additional error), and a computer program used to make the calculation. In either case, the use of smoke numbers is a very unreliable tool in predicting test cell plume opacity.

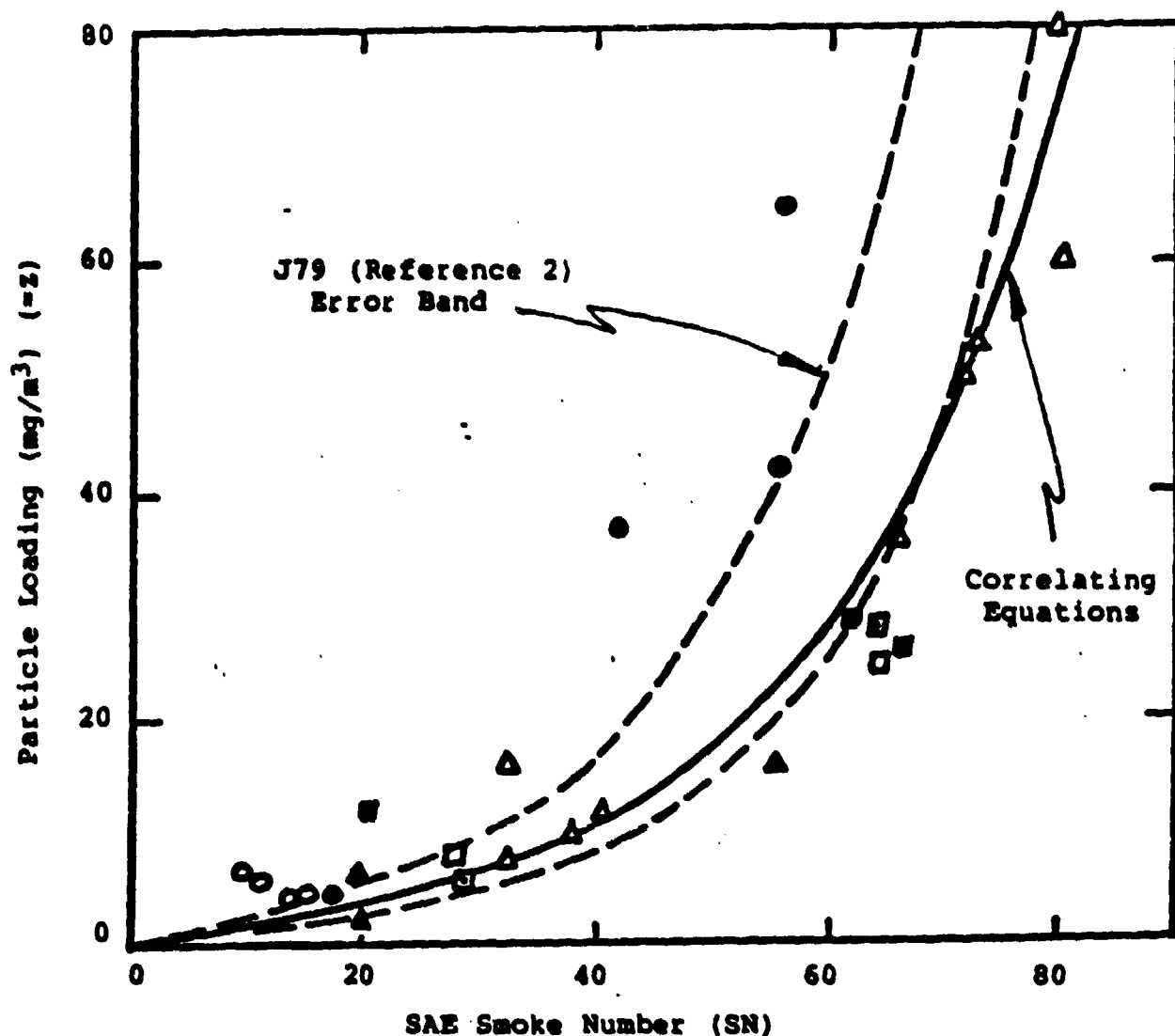


Figure 2. Relationship Between SAE Smoke Number and
Soot Density (Reference 6)

- JT8D & J52-P-6A
- J57-P-10 (Reference 4)
- J57-P-8
- ◆ T56 (501)
- T58-GE-10
- ▲ T64-GE-413
- △ TF30 (Reference 5)
- ▲ T400 (at Max. Power)
- TPE331-5-X21 (Reference 3)

Correlating Equations:

$$\ln\left(1 - \frac{SN}{100}\right) = -(.04682)^{0.9} \quad SN < 40$$

$$\ln\left(1 - \frac{SN}{100}\right) = -(.03162)^{0.6} \quad SN \geq 40$$

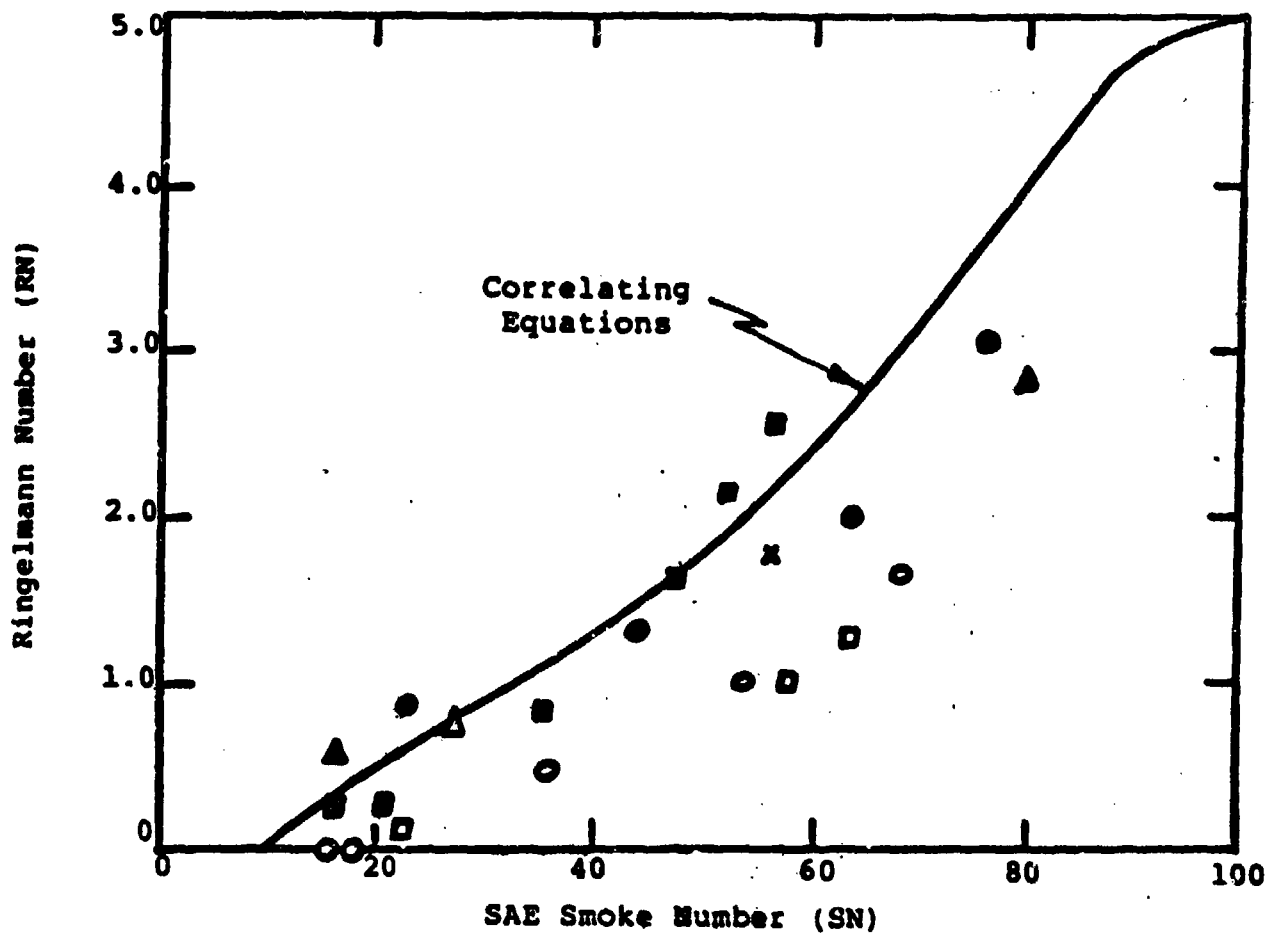


Figure 3. SAE Smoke Number vs. Ringelmann Reading (Reference 6)

Correlating Equations:

- | | |
|---------------------------|---|
| ○ J79 (Reference 2) | $\ln\left(\frac{T}{100}\right) = -(0.194L)\left[-\ln\left(1-\frac{SN}{100}\right)\right]^{2.08} \quad SN \geq 30$
$(L = \text{plume width} = 3.5 \text{ m})$ |
| ● J79-GE-10 (Reference 8) | |
| □ J65 (clean) | $\ln\left(\frac{T}{100}\right) = -(0.0617L)\left[-\ln\left(1-\frac{SN}{100}\right)\right], \quad SN \leq 30$ |
| ■ J57-P-8 | |
| □ J57 (Reference 7) | $RN = -.0375T + 4.5, \quad 15 \leq T \leq 85$
$RN = -.0800T + 8.1, \quad 95 \geq T > 85$
$RN = -.0667T + 5.0, \quad T < 15$ |
| ● J52-P-6A | |
| △ J52-P-6A (Smokeless) | |
| △ TF30-P-8 | |
| △ TF30-P-6 (Smokeless) | |
| × T56-A-10 | |

SECTION III

VISIBILITY EQUATIONS

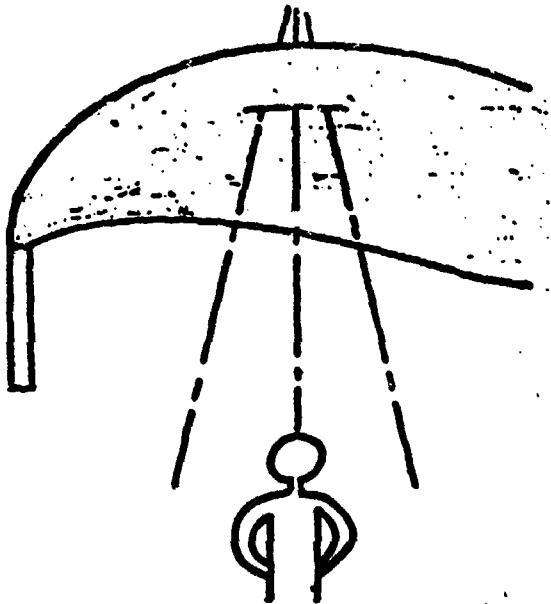
Jet engine exhaust emissions largely consist of fine particles of unburned carbon. Because they are black, and therefore absorb much of the incident light intensity, carbon particles will exhibit very little back-scattering of ambient light. The visibility of black plumes is almost entirely a function of the relative contrast between the background sky-light and the amount of such light transmitted through the plume (Figure 4). This relative contrast is independent of observer position and can be calculated by the following equation (Reference 11):

$$T = \frac{B_T}{B_0} = \exp \left[\left(\frac{-3WD}{2\rho_p} \right) \frac{1}{I} \sum_i \left(\frac{Q_{ext}}{d_p} \right)_i \right]$$

where: T = transmittance, or relative plume brightness
 B_T = brightness of light transmitted through the plume
 B_0 = background sky brightness
 W = particle loading
 D = plume diameter
 ρ_p = particle density
 I = total number of particle sizes
 d_p = particle size
 Q_{ext} = extinction coefficient, or ability of a given particle to reduce the intensity of the transmitted light

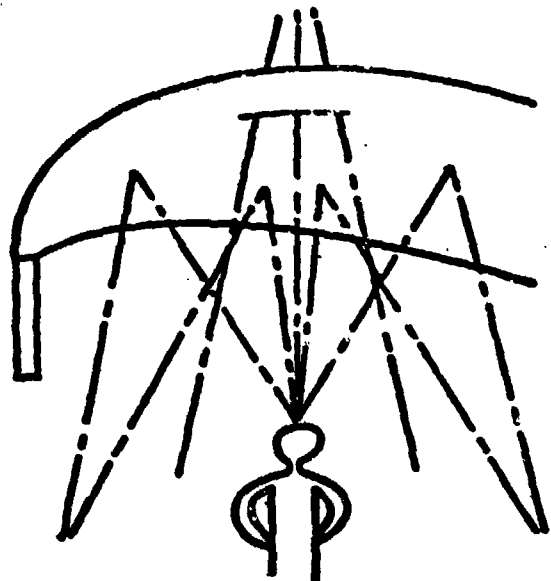
subscript i = i th particle size in the distribution

The extinction coefficient for any given particle is determined by the following equation (References 11 and 12):



Black Plumes

For transmitted light, the observer sees only relative contrast with background sky brightness.



White Plumes

Scattered light originates from both in front and behind the observer. Therefore, the relative position of the sun is significant.

Figure 4. Visibility

$$Q_{\text{ext}} = \frac{2}{x^2} \sum_n (2n + 1) \text{Real}(a_n + b_n)$$

where: $x = \pi d_p / \lambda$

λ = wavelength of light in which the plume is viewed (the computer program allows this value to be input, or if left blank assumes an average value for skylight of 0.550 microns)

a_n & b_n are complex Riccati-Bessel function of order " n ":

$$a_n = \frac{\psi_n'(y)\psi_n(x) - m\psi_n(y)\psi_n'(x)}{\psi_n'(y)\xi_n(x) - m\psi_n(y)\xi_n'(x)}$$

$$b_n = \frac{m\psi_n'(y)\psi_n(x) - \psi_n(y)\psi_n'(x)}{m\psi_n'(y)\xi_n(x) - \psi_n(y)\xi_n'(x)}$$

$y = mx$

m = complex refractive index. This is a function of the wavelength of light (λ) at which it is measured, and also the method of generating the soot particles. The computer program allows this value to be input, or if left blank assumes a value for amorphous carbon at 0.550 microns of: $1.96 - 0.66i$ (References 13, 14). (Note: Because the transmitted light is altered both in phase and magnitude, a vector is needed to express the effect of the particles. As in electrical engineering, a vector can be expressed as a complex number with real and imaginary parts. This is the case for the particle refractive index.)

Since these equations involve series functions of complex numbers, their solution is not simple. Instabilities can easily arise (particularly with large values of x), which cause the extinction coefficient to oscillate wildly and even produce negative values. In order to generate stable functions, the

following method is used (References 12, 15):

$$P_n(z) = \frac{d[\ln \psi_n(z)]}{dz} = \frac{\psi_n'(z)}{\psi_n(z)}$$

$$Q_n(z) = \frac{d[\ln \xi_n(z)]}{dz} = \frac{\xi_n'(z)}{\xi_n(z)}$$

(where $z = y$ or x)

Therefore:
$$a_n = \frac{\psi_n(x)}{\xi_n(x)} \left[\frac{P_n(y) - mP_n(x)}{P_n(y) - mQ_n(x)} \right]$$

$$b_n = \frac{\psi_n(x)}{\xi_n(x)} \left[\frac{mP_n(y) - P_n(x)}{mP_n(y) - Q_n(x)} \right]$$

$$\psi_n'(z) = \psi_{n-1}(z) - \frac{n}{z} \psi_n(z)$$

$$\xi_n'(x) = \xi_{n-1}(x) - \frac{n}{x} \xi_n(x)$$

Therefore:
$$P_n(z) = \frac{\psi_{n-1}(z) - \frac{n}{z} \psi_n(z)}{\psi_n(z)} = \frac{\psi_{n-1}(z)}{\psi_n(z)} - \frac{n}{z}$$

$$= \frac{J_{\nu-1}(z)}{J_{\nu}(z)} - \frac{(\nu - 1/2)}{z}$$

where $J =$ Bessel function

$$\nu - 1/2 = n$$

Using Lentz's continued fraction method⁽¹⁵⁾:

$$\frac{J_{\nu-1}}{J_{\nu}} = \frac{|w_1|w_2, w_1| |w_3, w_2, w_1| \dots}{|w_2| |w_3, w_2| \dots}$$

$$w_p = (-1)^{p+1} \frac{2(v + p - 1)}{z}$$

$$|w_p, w_{p-1}, \dots, w_1| = w_p + \frac{1}{w_{p-1} + \frac{1}{w_{p-2} + \frac{1}{\dots}}}$$

Convergence is reached for J_{v-1}/J_v when $|w_p, \dots, w_1|$ in the numerator equals $|w_p, \dots, w_2|$ in the denominator.

$Q_n(x)$ is generated by the following recursion formula:

$$Q_n(x) = \frac{1}{\frac{n}{x} - Q_{n-1}(x)} - \frac{n}{x}$$

(where $Q_0(x) = -i$)

Since

$$\frac{\psi_{n-1}(x)}{\psi_n(x)} = \frac{J_{v-1}(x)}{J_v(x)}$$

$$\psi_n(x) = \psi_{n-1}(x) \left[\frac{J_v(x)}{J_{v-1}(x)} \right]$$

(where $\psi_0(x) = \sin x$)

Finally,

$$\xi_n(x) = \psi_n(x) + i\beta_n(x)$$

$$\beta_n(x) = \left(\frac{2n-1}{x} \right) \beta_{n-1}(x) - \beta_{n-2}(x)$$

(where $\beta_0(x) = \cos x$, and $\beta_1(x) = \frac{\cos x}{x} + \sin x$)

Following Wiscombe (Reference 12) the order (n) of these functions varies from 1 to N, where:

$$N = x + 4x^{1/3} + 2, \quad x \geq 4200$$

$$N = x + 4.05x^{1/3} + 2, \quad 8 < x < 4200$$

$$N = x + 4x^{1/3} + 1, \quad x \leq 8$$

These equations can be used to generate the requisite Riccati-Bessel functions, the extinction coefficient, and finally the transmittance.

Once the transmittance (T) is calculated, the Ringelmann number may be obtained from the empirical correlation of Connor and Hodgkinson (References 10, 11), Figure 5.

A computer program was written to perform these calculations. The FORTRAN listing and sample runs are given in the Appendices.

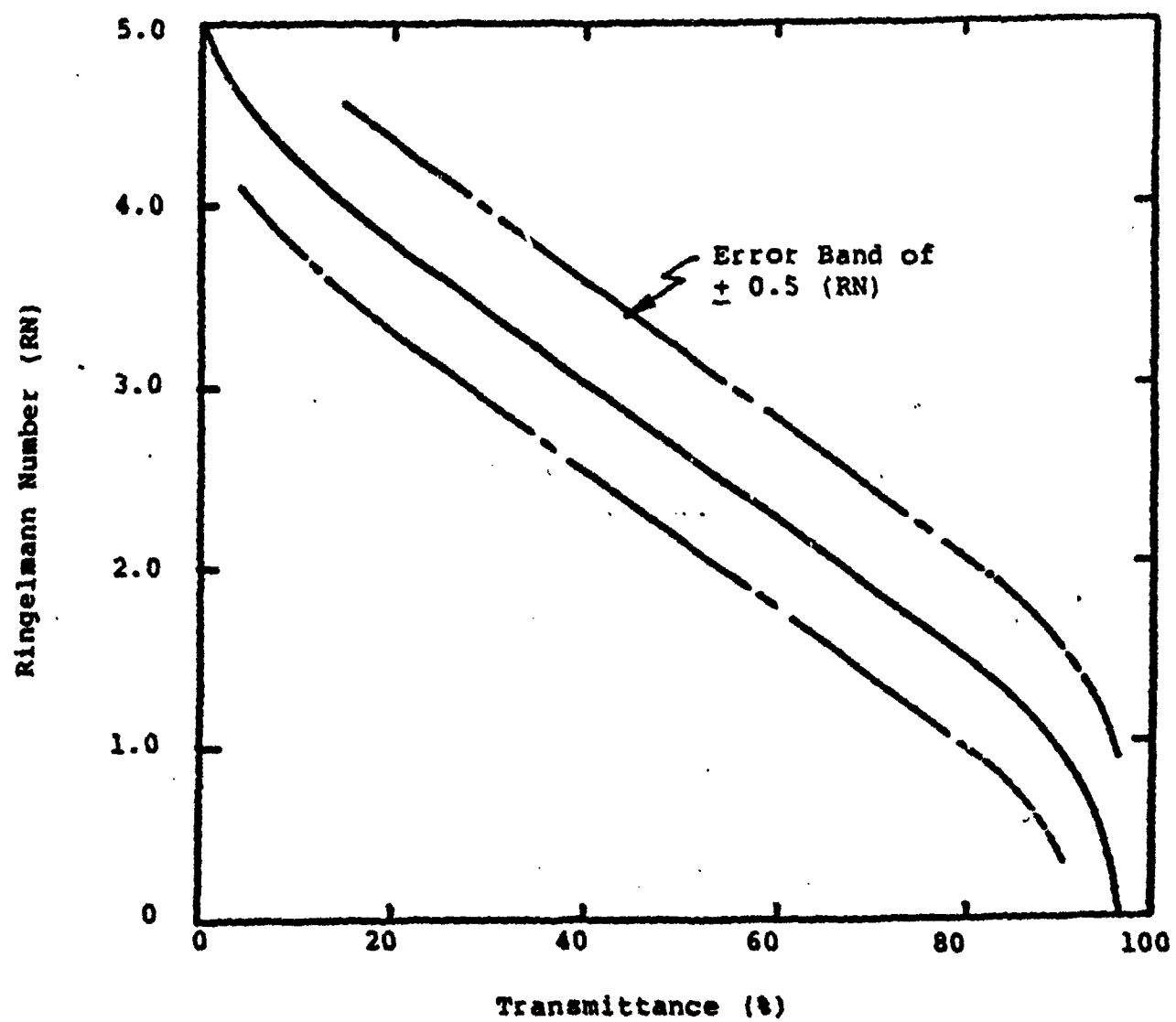


Figure 5. Black Plume Ringelmann Number Correlation with Transmittance (References 10, 11)

SECTION IV

ELECTROSTATIC PRECIPITATOR (ESP) EQUATIONS

A standard mathematical model (Reference 16) was used for predicting the ability of a wire-and-plate ESP to operate as a particle control device:

$$w_i = \frac{8.85 \times 10^{-5} E_c E_p d_{pi}}{\mu} \left(\frac{\xi}{\xi + 2} \right)$$

$$\eta_i = 1 - \exp\left(\frac{-A_p w_i K}{Q}\right)$$

$$\eta = \sum_i \eta_i m_i$$

where: η = overall fractional collection efficiency

η_i = fractional collection efficiency for particles of size d_{pi}

m_i = inlet mass fraction of particles of size d_{pi}

A_p/Q = specific collection area of the ESP (A_p = total collection surface in m^2 ; and Q = gas flow in m^3/sec)

w_i = theoretical migration velocity of particles of size d_{pi} , in m/sec

K = empirical constant

ξ = dielectric constant of the particles (dimensionless)

μ = gas viscosity, in cp

E_c = electric field strength near the discharge electrodes, in kV/cm

E_p = electric field strength near the collecting plates, in kV/cm

d_p = particles size, in microns

This model is based on a field-charging mechanism and is valid for particles larger than 0.5 microns.

If the collection efficiency for an ESP is plotted against the particle size, the resulting curve will exhibit a minimum in the range of 0.2 to 0.7 microns. Above that range, a field-charging mechanism predominates and the efficiency declines with particle size. Below that range, a diffusion-charging mechanism predominates and the efficiency increases with decreasing particle size. Since most of the particles emitted from a test cell are smaller than 0.2 μm , a large K value of 600 was used in order to compensate for the lack of a diffusion-charging mechanism in the model equations.

In order to reduce the amount of input data needed to run the computer program and avoid a prior design of the ESP, the following values were assumed:

$$\xi = 3, \text{ for carbon}$$

$$\mu = 0.024 \text{ cp, for air at } 350^{\circ}\text{F and } 1 \text{ atm}$$

$$E_c = E_p = \frac{40 \text{ kV}}{(4.5 \text{ inches})(2.54 \text{ cm/inch})} = 3.50 \text{ kV/cm}$$

(where 9 inches is generally used as the plate-to-plate spacing in utility-type ESP's, with a secondary voltage of 40 kV).

The computer program takes the uncontrolled test cell emission data, calculates the fractional efficiencies, and then determines the outlet particle size distribution and loading. This information then goes to the visibility portion of the program where the outlet Ringelmann number is calculated.

SECTION V

SCRUBBER EQUATIONS

A standard mathematical model (Reference 17) was used to describe the particle collection efficiency of a high energy venturi scrubber. As with the ESP model, this also required an empirical factor (f) to make the model agree approximately with actual data:

$$\ln(1 - \eta_i) = -\left(\frac{18}{55}\right) \left(\frac{\rho_l}{\rho_p}\right) \left(\frac{Q_l}{Q_g}\right) \left(\frac{d_d}{d_{pi}}\right)^2 \frac{1}{C_i} \{ (k_i f + 0.7) - 1.4 \ln \left(\frac{k_i f + 0.7}{0.7} \right) - \left(\frac{0.49}{k_i f + 0.7} \right) \}$$

This equation is written in dimensionless form, and therefore any consistent set of units may be used:

η_i = fractional collection efficiency for particles of size d_{pi}

ρ_l = liquid density

ρ_p = particle density

Q_l = liquid flow rate

Q_g = gas flow rate

C_i = Cunningham correction factor for gas viscosity; for particles that are the same size or smaller than the mean free path of the gas molecules (λ)

$$= 1 + \frac{2\lambda}{d_{pi}} \left[1.23 + 0.41 \exp \left(\frac{-0.44 d_{pi}}{\lambda} \right) \right] \text{ (dimensionless)}$$

k_i = Stokes' parameter = $\frac{C_i \rho_p d_{pi}^2}{9\mu_g d_d} V_{gT}$ (dimensionless)

f ~ 0.5 (dimensionless empirical factor based on the author's experience)

V_{gT} = gas velocity in the venturi throat

$$= \sqrt{\frac{\Delta P_T}{\rho_L} \frac{Q_g}{Q_L}} g_c$$

ΔP_T = pressure drop across the venturi throat

g_c = Newton's Law conversion factor

The following equations require specific units:

d_d = mean drop size in the venturi throat (Reference 18), in microns

$$= \frac{1920}{V_{gT}} \sqrt{\frac{\sigma_L}{\rho_L}} + 3.69 \left(\frac{\mu_L}{\sigma_L \rho_L} \right)^{0.45} \left(\frac{1000 Q_L}{Q_g} \right)^{1.5}$$

σ_L = surface tension of scrubbing liquid, in dynes/cm

ρ_L = density of scrubbing liquid, in g/cc

μ_L = viscosity of scrubbing liquid, in cp

Q_L = flow rate of scrubbing liquid, in gpm

Q_g = gas flow rate, in cfm

V_{gT} in ft/sec

λ = mean free path of gas molecules, in microns

$$= \frac{3.78 \mu_g}{\sqrt{P_g \rho_g}}$$

μ_g = gas viscosity, in cp

P_g = gas pressure, in psia

ρ_g = gas density, in lbm/ft³

Again, in order to minimize the input data requirements, the following operating conditions were assumed:

(1) water is the scrubbing liquid at 70°F

(2) gas properties are those of air at 350°F and 1 atm pressure.

For venturi scrubbers, Q_l/Q_g (the liquid-to-gas ratio) is generally 5 to 30 gpm/1000 cfm, and ΔP_T is 10 to 70 inches of water.

The computer program takes the uncontrolled test cell emission data, calculates the fractional efficiencies, and then determines the outlet particle size distribution and loading. This information then goes to the visibility portion of the program where the outlet Ringelmann number is calculated.

As with electrostatic precipitators, the primary collection mechanism for venturi scrubbers should theoretically change in the range 1.0 to 0.1 μm . Above 1 μm , the particles are collected by an inertial mechanism, while below 0.1 μm a diffusional mechanism should prevail. Again, this would imply a trough in the fractional efficiency curve for particles in the 1.0 to 0.1 μm range. However, in practice, the collection efficiency of venturi scrubbers continues to decline below 0.1 μm , indicating that the predominant mechanism remains inertial. This means that standard venturi scrubbers are inherently less efficient than ESP's in collecting particles smaller than 0.5 μm . One method of overcoming this deficiency has been to induce condensation in the gas stream, either before the scrubber (by quenching), or afterward (by utilizing a two-phase ejector). However, these methods cannot as yet be mathematically modelled with any confidence and have not been included in the computer program.

SECTION VI

RESULTS & DISCUSSION

Grems (Reference 19) measured the particle size distribution, loading, and transmittance from a test cell at McClellan Air Force Base. However, the particle density was unknown. In the present study, this density was used as an empirical parameter to fit the computer results to Grems' data. Excellent agreement was obtained for a particle density of 0.92 g/cc (Table 1). For comparison, computer results are also shown for a particle density of 1.0 g/cc.

Soot particles are porous spheres of carbon, having a high void fraction. Solid carbon has a density of 1.8 to 2.1 g/cc. Therefore, a particle density of 0.92 g/cc implies a void fraction of about 0.53.

Although Grems' data indicated a bimodal particle size distribution, a straight-line log-normal fit was made by the computer program (see Figure 6).

Table 2 shows computer predictions of plume visibility when an electrostatic precipitator or venturi scrubber is used. For the ESP, a specific collection surface of $3281/\text{m}^2$ per 1000 m^3/min of gas ($1000 \text{ ft}^2/1000 \text{ cfm}$) corresponds to an upper limit in commercial applications. Since the gas flow from a test cell is on the order of 200,000 scfm, 200,000 ft^2 of collecting plate would be required. However, even such a large ESP has only a small effect on the Ringelmann number because of the small particle size. The size range which has the greatest effect on visibility matches the wavelength of visible light--i.e., 0.2 to 0.7 microns. This is precisely the range in which an ESP or any other control device, is least efficient. Therefore, purchase of an electrostatic precipitator larger than the test cell would only have a marginal effect on plume visibility during the few hours per week the test cell is in use.

Similarly, a venturi scrubber designed for the limit of its range of operability would also have a marginal effect on test cell plume visibility. At a liquid-to-gas ratio of 30 gpm/1000 cfm ($4.01 \text{ m}^3/\text{min}$ water per 1000 m^3/min gas) the scrubber would produce 6000 gpm of waste water for a typical installation; and at a pressure drop of 70 inches of water (131 mm mercury) a 2400 hp tail fan would be required. Under these conditions, the computer predicts an overall particle collection efficiency of 49% with a visibility improvement of 0.5

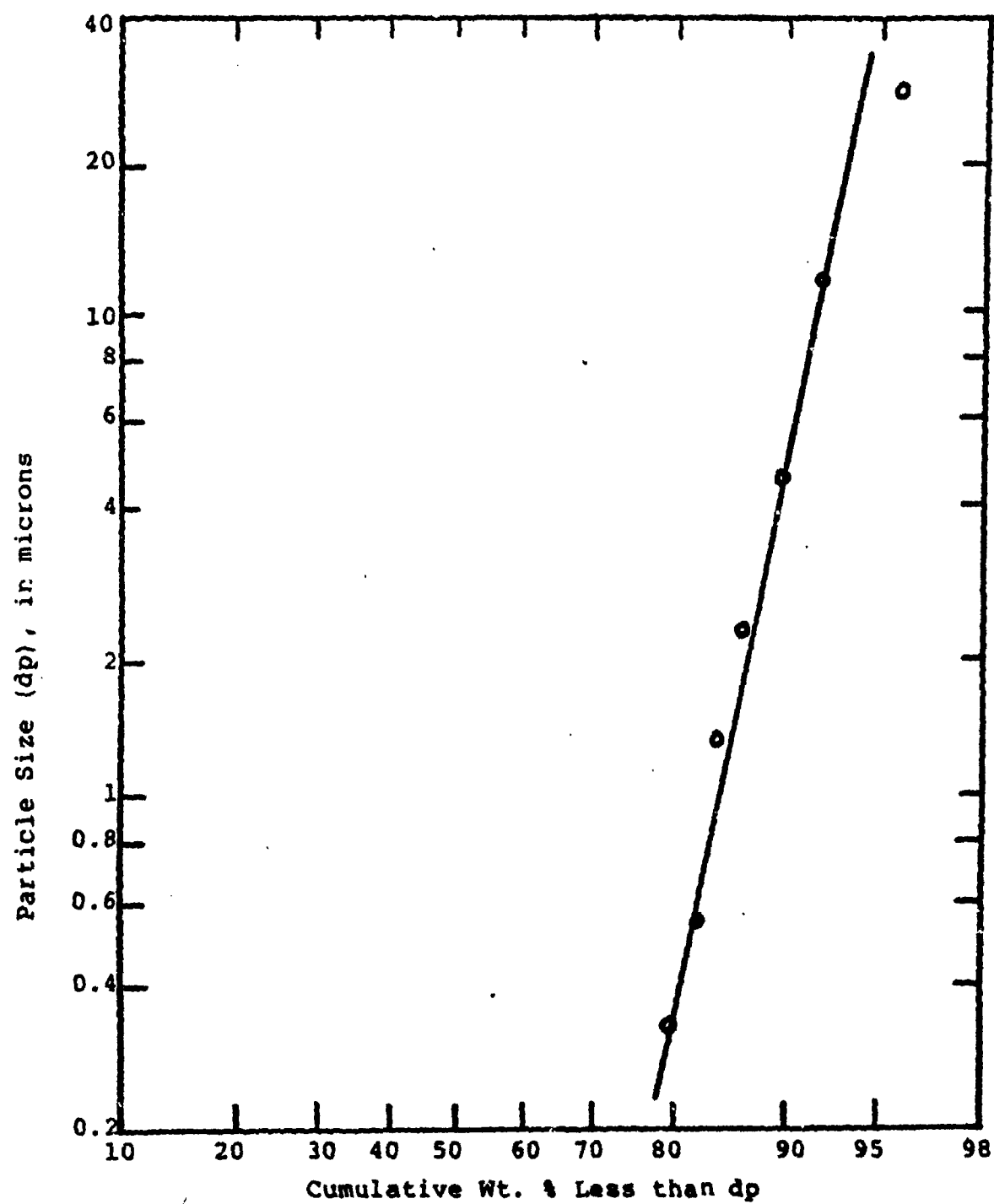


Figure 6. Log-Normal Plot of Size Distribution from Grems' Data (Reference 19)

TABLE 1. COMPARISON OF COMPUTER PREDICTIONS WITH GRENS' DATA FOR J57 ENGINE (Reference 19).

Fuel Firing Rate (lbm/hr)	Particle Loading (mg/m ³)	Measured Cum Mt less than	Particle Size Distribution Aerodynamic Diameter* (d _p for ρ _p = 1.0 g/cc)	Measured Transmittance	Predicted Transmittance (for ρ _p = 1.0 g/cc)	d _p * (for ρ _p = 0.92 g/cc)	Predicted Transmittance (for ρ _p = 0.92 g/cc)
1000	2.16	93.5	23 μ	960	88.30	24.0 μ	87.40
		91.4	10.5			10.9	
		91.4	4			4.2	
		87.8	2			2.1	
		84.9	1.1			1.15	
		79.9	0.57			0.59	
		73.5	0.33			0.34	
2500	1.95	95.7	20	88	89.4	29.2	88.6
		92.1	11.5			12.0	
		89.7	4.5			4.69	
		86.6	2.2			2.29	
		84.5	1.3			1.36	
		82.7	0.54			0.56	
		79.3	0.33			0.34	
8620	6.00	98.6	22	66	67.9	22.9	65.6
		96.8	9.3			9.78	
		95.1	3.5			3.65	
		92.8	1.7			1.77	
		90.5	0.94			0.98	
		83.8	0.47			0.49	
		77.4	0.23			0.24	
8620	6.34	97.7	21	66	68.4	21.9	66.2
		97.7	9.4			9.80	
		97.4	3.5			3.65	
		95.8	1.7			1.77	
		94.8	0.92			0.96	
		94.2	0.46			0.48	
		88.2	0.22			0.23	

Net open exhaust area = 700 ft² (700 = 26.5 ft, or 8 meters); refractive index for amorphous carbon at 550 nm = 1.96-0.66i

*For a cascade injector, $d_{p1}/\sqrt{\rho_{p1}} = d_{p2}/\sqrt{\rho_{p2}}$

TABLE 2. COMPARISONS OF CONTROLLED AND UNCONTROLLED EMISSIONS.

UNCONTROLLED EMISSIONS: (Plume Width = 8 Meters)

Particle Loading (mg/m ³)	Particle Density (g/cc)	Particle Size (μm)	Cum.Wt. % Less Than	Transmittance (%)	Ringelmann Number
6.34	0.92	21.9	97.7	66.2	1.5-2.5
		9.80	97.7		
		3.65	97.4		
		1.77	95.8		
		0.96	94.8		
		0.48	94.2		
		0.23	88.2		

CONTROLLED EMISSIONS:

(1) with ESP: SCA = 3281 m² /1000 m³/min

Outlet Particle Loading (mg/m ³)	Collection Efficiency (%)	Transmittance (%)	Ringelmann Number
2.93	53.8	82.8	0.9-1.9

(2) with Venturi Scrubber: L/G = 4.01 m³/min water per 1000 m³/min Gas
ΔP = 131 mm Hg

Outlet Particle Loading (mg/m ³)	Collection Efficiency (%)	Transmittance (%)	Ringelmann Number
3.26	48.6	81.0	1.0-2.0

Ringelmann number. Operating data with a scrubber (not a venturi) at the Jacksonville Naval Air Station (Reference 20) indicate an average particle collection efficiency of about 75%. However, there was considerable uncertainty in the accuracy of the data. Stockham, et al. (Reference 21) also report an average collection efficiency of 48% with water injection into the augmentor tube. Again, this is not venturi scrubber data, but it does indicate the validity of the order of magnitude of the predicted results. It should be noted that opacity measurement with a scrubber operating is virtually impossible, since the scrubber will emit a large and obscuring steam plume of its own.

REFERENCES

- (1) Morse, H.N., "Legal Briefs," JAPCA, Vol. 31, p. 323. March 1981.
- (2) Shaffernocker, W.M. and Stanforth, C.M., "Smoke Abatement Techniques," SAE Transactions, Vol. 77, pp. 1059-1079. 1968.
- (3) Johansen, K.M. and Kumm, E.L., Determination of Aircraft Turbine Engine Particulates, EPA-650/2-75-055. May 1975.
- (4) Grems, B.C., Smoke Abatement for POD Test Cells, CEEDO-TR-77-40. July 1977.
- (5) Fenton, D.L., Nordstrom, E.W., Luebcke, E.H., Turbine Engine Particulate Emission Characterization, FAA-RD-77-165. October 1977.
- (6) Lindenhofen, H.E., A Survey of the Air Pollution Potential of Jet Engine Test Facilities, NAPTC-PE-3. October 1972.
- (7) Stockham, J. and Bétz, H., "Study of Visible Exhaust Smoke from Aircraft Jet Engines," SAE paper No. 710428. May 1971.
- (8) Klarman, A.F., Rollo, A.J. and Scott, H.C., Evaluation of Water/Fuel Emulsion Concept for Test Cell Smoke Abatement, NAPC-PE-7. March 1978.
- (9) Wood, A.D., "Correlation Between Smoke Measurements and the Optical Properties of Jet Engine Smoke," paper No. 751119, presented at SAE National Aerospace Engineering & Manufacturing Meeting, Los Angeles, CA. 17-20 Nov. 1975.
- (10) Conner, W.A. and Hodgkinson, J.R., PHS Report No. 999-AP-30. 1967.
- (11) Halow, J.S. and Zeek, S.J., "Predicting Ringelmann number and Optical Characteristics of Plumes," JAPCA, Vol. 23, pp. 676-684. August 1973.
- (12) Wiscombe, W.J., "Improved Mie Scattering Algorithms," Applied Optics, Vol. 19, pp. 1505-1509. May 1980.

- (13) Ensor, D.S. and Pilat, M.J., "Calculation of Smoke Plume Opacity from Particulate Air Pollutant Properties," JAPCA, Vol. 21, pp. 496-501. 1971.
- (14) McDonald, J.E., "Visibility Reduction Due to Jet Exhaust Carbon Particles," J. Appl. Meteorology, Vol. 1, pp. 391-398. 1962.
- (15) Lentz, W.J., "Generating Bessel Functions in Mie Scattering Calculations Using Continued Fractions," Applied Optics, Vol. 15, pp. 668-671. March 1976.
- (16) Stern, A.C., ed. Air Pollution, 3rd ed., Vol. IV. New York: Academic Press. 1977.
- (17) Calvert, S., et al., Scrubber Handbook, NTIS Publication No. PB 213 016. August 1972.
- (18) Nukiyama, S. and Tanasawa, Y., Trans. Soc. Mech. Engrs. (Japan), Vol. 4, p. 86. 1938.
- (19) Grems, B.C., Plume Opacity and Particulate Emissions from a Jet Engine Test Facility, Masters Thesis, U. of California (Davis). 1976.
- (20) Kelly, J., and Chu, E., Jet Engine Test Cells-Emissions and Control Measures: Phase 2, EPA-340/1-78-001 b. April 1978.
- (21) Stockham, J.D., Lannis, M.D., MacNaughton, M.G., and Tarquinio, J.J., "Control of Particulate Emissions from Turbine Engine Test Cells by Cooling Water Injection," JAPCA, Vol. 31, pp. 675-678. June 1981.

APPENDIX A
COMPUTER INPUT DATA FORMAT

The following pages give the format for the input data needed to run the computer program. The particle loading should be determined by EPA Method 5, and the particle size distribution by cascade impactor (Reference 19). The plume width can be approximated by the square root of the net open stack area (the actual stack cross-section minus the area occupied by acoustical baffles). For soot particles, the refractive index is $1.96-0.66i$ at a wavelength of 550 nm, and the particle density was estimated empirically as 0.92 g/cc.

Examples are given for:

- (1) Grems' data(19)
- (2) an electrostatic precipitator with a specific collection area of 1000 ft²/1000 cfm (3281 m² of collecting plate per 1000 m³/min of gas)
- (3) a venturi scrubber with a liquid-to-gas ratio of 30 gpm/1000 cfm (4.01 m³/min of water per 1000 m³/min of gas) at a pressure drop of 70 inches of water (131 mm Hg).

CARD #1

This card contains the title of the case being run, inserted between columns 9 and 10.

CARD #2

This card contains the number of data pairs in the particle size distribution. The minimum number is 2, and the maximum is 100, inserted as an integer between columns 11 and 15 (right justified).

CARD #3 a, b, c, etc.

This card(s) contains the data pairs for the particle size distribution. Columns 1-10, 21-30, 41-50, and 61-70 contain values of the cumulative weight percent less than particle size d_p ; while columns 11-20, 31-40, 51-60, and 71-80 contain the corresponding values of d_p . Therefore, a maximum of four data pairs can fit on one card. If there are more data pairs (as per CARD #2), these are put on subsequent cards, until the total number of data pairs (cumulative weight percent less than d_p , and d_p) is equal to the number specified in CARD #2. All values are floating point numbers, with four digits (or blanks) to the right of the decimal point (right justified).

CARD #4

This card contains the following physical parameters:
columns 11-15--the effective stack diameter in meters
(based on the net open area) expressed as a floating
point number, with two digits (or blanks) to the right
of the decimal point (right justified)

columns 16-22--the particle loading in mg/m^3 , as a floating point number, with two digits (or blanks) to the right of the decimal point (right justified)

columns 23-28--the particle density in g/cm^3 , as a floating point number, with two digits (or blanks) to the right of the decimal point (right justified)

columns 29-46--the particle refractive index. Columns 29-37 contain the real part, and 38-46 the imaginary part; both as floating point numbers with two digits (or blanks) to the right of the decimal point (right justified). If these columns are left completely blank, a value for amorphous carbon of $1.96-0.66i$ is assumed by the program. Note that the refractive index and the wavelength that follows must be consistent

columns 47-53--the wavelength of light (in microns) at which the refractive index was measured, and at which the plume is presumed to be viewed. This must be expressed as a floating point number with three digits (or blanks) to the right of the decimal point (right justified). If columns 29-46 were left blank, these columns should also be left completely blank, in which case the program assumes a value of 0.550 microns.

CARD #5

This card contains (in column 2) an integer number which

indicates whether or not a particulate control device (electrostatic precipitator or venturi scrubber) has been installed on the test cell exhaust:

- zero (0) means no control device
- 1 means an electrostatic precipitator
- 2 means a venturi scrubber

These are the only permissible cases.

CARD #6

This card depends on the code given in CARD #5.

- (a) If there is no control device (0 in column 2 of CARD #5), CARD #6 does not exist.
- (b) If an electrostatic precipitator is indicated by CARD #5, CARD #6 must contain the specific collection area (in m^2 of plate area per 1000 m^3/min of exhaust gas) in columns 11-17 as a floating point number with one digit (or blank) to the right of the decimal point (right justified).
- (c) If a venturi scrubber is indicated by CARD #5, CARD #6 must contain the liquid-to-gas ratio (in m^3/min water per 1000 m^3/min exhaust gas) in columns 11-15; and the scrubber pressure drop (in mm mercury) in columns 16-23; both expressed as floating point numbers, with two digits (or blanks) to the right of the decimal point (right justified).

CARD #7

This card contains (in column 2) a code which tells the computer if more cases are to follow:

zero (0) signifies no more cases

1 means an additional case follows

For each additional case, CARDS #1 to 7 must be repeated, even if some of the data remain the same.

FORM 5-64
 FORM 5-64
 DATE

Page 2

STATION		FOR EACH STATION		STATION	
NAME	NO.	NAME	NO.	NAME	NO.
NJIT1					
88.2	0.22	94.2	0.46	94.8	0.92
97.4	3.5	97.7	9.4	97.7	21.0
8.0	6.34	0.92			
NJIT2					
77.4	0.23	83.8	0.47	90.5	0.94
95.1	3.5	96.0	9.3	98.6	22.0
8.0	6.08	0.92			
NJIT3					
73.5	0.33	79.9	0.57	84.9	1.1
91.4	1.9	91.4	10.5	93.5	23.0
8.0	2.16	0.92			

Figure A-1. Computer Input Data Format

33

Figure A-1. Continued. Computer Input Data Format

PROJECT		PERIOD		DATE		PAGE	
ESP CASE						1-1	
TESTING NUMBER		TESTING DATE		TESTING TIME		TESTING LOCATION	
1		7		97.2		97.7	
0		3.5		97.7		97.7	
		8.0		6.34		0.92	
		3200.8					
		0.22		0.46		0.92	
		95.8		21.0		95.8	
		1.7					

Figure 1-A. Continued. Computer Input Data Format

35

Figure A-1. Continued. Computer Input Data Format

APPENDIX B
OUTPUT FORMAT

Example outputs are given on the next few pages for the input data shown in the previous section (i.e. Grems' data, an ESP, and a venturi scrubber).

Figure B-1. Output Format

PLUME WIDTH (IN METERS) = 6.88 PARTICLE DENSITY (IN G/CC) = .92
 OUTLET LOADING (IN MG/M3) = 6.34 REFRACTIVE INDEX: REAL PART = 1.96
 LIGHT WAVELENGTH (IN MICRONS) = 1.55 IMAGINARY PART = .166

OUTLET PARTICLE SIZE DISTRIBUTION
 CUMULATIVE WEIGHT PERCENT
 LESS THAN STATED PARTICLE SIZE PARTICLE SIZE
 (MICRONS)

1.0	1.000
2.0	.000
3.0	.000
4.0	.000
5.0	.000
6.0	.000
7.0	.000
8.0	.000
9.0	.000
10.0	.000
12.0	.000
15.0	.000
18.0	.000
20.0	.000
25.0	.000
30.0	.000
35.0	.000
40.0	.000
45.0	.000
50.0	.000
55.0	.000
60.0	.000
65.0	.000
70.0	.000
75.0	.000
80.0	.000
85.0	.000
90.0	.000
95.0	.000
99.0	.000
100.0	.000
1.0	.000
2.0	.000
3.0	.000
4.0	.000
5.0	.000
6.0	.000
7.0	.000
8.0	.000
9.0	.000
10.0	.000
12.0	.000
15.0	.000
18.0	.000
20.0	.000
25.0	.000
30.0	.000
35.0	.000
40.0	.000
45.0	.000
50.0	.000
55.0	.000
60.0	.000
65.0	.000
70.0	.000
75.0	.000
80.0	.000
85.0	.000
90.0	.000
95.0	.000
99.0	.000
100.0	.000

RINGELMANN NUMBER RANGE

1.5 - 2.5

PERCENT LIGHT TRANSMITTED = 66.15

Figure B-1. Continued. Output Format

.....
NJ172
.....

Figure E-1. Continued. Output Format

PIPE WIDTH (IN REVERSI) =	8.88	PARTICLE DENSITY (IN G/CC) =	.62
OUTLET LOADING (IN MG/M3) =	6.98	REFRACTIVE INDEX: REAL PART	1.96
TIME SAMPLE LENGTH (IN MICRON) =	.550	IMAGINARY PART	-.66

OUTLET PARTICLE SIZE DISTRIBUTION	
CUMULATIVE WEIGHT PERCENT LESS THAN STATED PARTICLE SIZE	PARTICLE SIZE (MICRON)
1.0	1.0
2.0	2.0
3.0	3.0
4.0	4.0
5.0	5.0
6.0	6.0
7.0	7.0
8.0	8.0
9.0	9.0
10.0	10.0
11.0	11.0
12.0	12.0
13.0	13.0
14.0	14.0
15.0	15.0
16.0	16.0
17.0	17.0
18.0	18.0
19.0	19.0
20.0	20.0
21.0	21.0
22.0	22.0
23.0	23.0
24.0	24.0
25.0	25.0
26.0	26.0
27.0	27.0
28.0	28.0
29.0	29.0
30.0	30.0
31.0	31.0
32.0	32.0
33.0	33.0
34.0	34.0
35.0	35.0
36.0	36.0
37.0	37.0
38.0	38.0
39.0	39.0
40.0	40.0
41.0	41.0
42.0	42.0
43.0	43.0
44.0	44.0
45.0	45.0
46.0	46.0
47.0	47.0
48.0	48.0
49.0	49.0
50.0	50.0
51.0	51.0
52.0	52.0
53.0	53.0
54.0	54.0
55.0	55.0
56.0	56.0
57.0	57.0
58.0	58.0
59.0	59.0
60.0	60.0
61.0	61.0
62.0	62.0
63.0	63.0
64.0	64.0
65.0	65.0
66.0	66.0
67.0	67.0
68.0	68.0
69.0	69.0
70.0	70.0
71.0	71.0
72.0	72.0
73.0	73.0
74.0	74.0
75.0	75.0
76.0	76.0
77.0	77.0
78.0	78.0
79.0	79.0
80.0	80.0
81.0	81.0
82.0	82.0
83.0	83.0
84.0	84.0
85.0	85.0
86.0	86.0
87.0	87.0
88.0	88.0
89.0	89.0
90.0	90.0
91.0	91.0
92.0	92.0
93.0	93.0
94.0	94.0
95.0	95.0
96.0	96.0
97.0	97.0
98.0	98.0
99.0	99.0
100.0	100.0

RINGELMANN NUMBER RANGE
1.5 - 2.5
PERCENT LIGHT TRANSMITTED = 65.63

Figure B-1. Continued. Output Format

.....
M-1113
.....

Figure B-1. Continued, Output Format

NJ174

Figure B-1. Continued. Output Format

INLET DUSTY (IN WT%) = 0.00 PARTICLE DENSITY (G/CC) = 0.92
 INLET LOADING (IN MG/M) = 1.00 REFRACTIVE INDEX: REAL PART = 1.96
 INLET WAVELENGTH (IN MICRON) = 0.550 IMAGINARY PART = 0.00

WILEY PARTICLE SIZE DISTRIBUTION
 CUMULATIVE WEIGHT PERCENT PARTICLE SIZE
 LESS THAN STATED PARTICLE SIZE (MICRON)

1.0	0.000
2.0	0.000
3.0	0.000
4.0	0.000
5.0	0.000
6.0	0.000
7.0	0.000
8.0	0.000
9.0	0.000
10.0	0.000
12.0	0.000
15.0	0.000
18.0	0.000
20.0	0.000
25.0	0.000
30.0	0.000
35.0	0.000
40.0	0.000
45.0	0.000
50.0	0.000
55.0	0.000
60.0	0.000
65.0	0.000
70.0	0.000
75.0	0.000
80.0	0.000
85.0	0.000
90.0	0.000
95.0	0.000
100.0	0.000

WINGELMANN NUMBER RANGE

0.5 - 1.0

PERCENT LIGHT TRANSMITTED = 88.59

Figure B-1. Continued. Output Format

 NJTS

*** AN ELECTROSTATIC PRECIPITATOR HAS BEEN ASSUMED AS A CONTROL DEVICE ***
 THE SPECIFIC COLLECTION SURFACE IS 3280.8 M² PER 1000 M³/MIN
 WHICH PRODUCES AN OVERALL COLLECTION EFFICIENCY OF 53.77 %

ESP INLET LOADING = 6.34 MG/M³

INLET PARTICLE SIZE DISTRIBUTION

CUM.WT.%	MICRONS
1.0	0.030
2.0	0.330
3.0	0.000
4.7	0.000
5.0	0.000
10.0	0.030
15.0	0.000
25.0	0.000
30.0	0.000
40.0	0.000
50.0	0.000
60.0	0.001
70.0	0.004
80.0	0.022
85.0	0.040
90.0	0.213
95.0	1.382
96.7	2.381
97.0	4.650
98.0	11.317
99.0	45.977

Figure B-1. Continued. Output Format

PLUME WIDTH (IN METERS) =	0.00	PARTICLE DENSITY (IN G/CM ³) =	0.92
OUTLET LOADING (IN MG/M ³) =	2.03	REFRACTIVE INDEX: REAL PART	1.94
LIGHT WAVELENGTH (IN MICRONS) =	0.550	IMAGINARY PART	-0.04

OUTLET PARTICLE SIZE DISTRIBUTION

CUMULATIVE WEIGHT PERCENT LESS THAN STATED PARTICLE SIZE	PARTICLE SIZE (MICRON)
---	---------------------------

1.0	0.000
2.0	0.000
3.0	0.000
4.0	0.000
5.0	0.000
10.0	0.000
15.0	0.000
20.0	0.000
30.0	0.000
40.0	0.000
50.0	0.000
60.0	0.000
70.0	0.000
80.0	0.000
85.0	0.000
90.0	0.000
95.0	0.000
96.0	0.000
97.0	0.000
98.0	0.000
99.0	0.000

RINGELMANN NUMBER RANGE

0.9 - 1.9

PERCENT LIGHT TRANSMITTED = 82.00

Figure B-1. Continued. Output Format

PLUME WIDTH (IN METERS) =	0.00	PARTICLE DENSITY (IN G/CC) =	0.02
OUTLET LOADING (IN MG/M3) =	3.24	REFRACTIVE INDEX: REAL PART	1.06
LIGHT WAVELENGTH (IN MICRONS) =	0.550	IMAGINARY PART	-0.66

OUTLET PARTICLE SIZE DISTRIBUTION

CUMULATIVE WEIGHT PERCENT LESS THAN STATED PARTICLE SIZE	PARTICLE SIZE (MICRON)
---	---------------------------

1.0	0.000
7.0	0.000
3.0	0.000
4.0	0.000
5.0	0.000
10.0	0.000
15.0	0.000
20.0	0.000
30.0	0.000
40.0	0.000
50.0	0.000
60.0	0.000
70.0	0.001
80.0	0.003
85.0	0.005
90.0	0.009
95.0	0.024
96.0	0.035
97.0	0.051
98.0	0.084
99.0	0.182

SINGELMAN NUMBER RANGE

1.0 - 2.0

PERCENT LIGHT TRANSMITTED = 80.00

Figure B-1. Continued. Output Format

PLUME WIDTH (IN METERS) =	0.00	PARTICLE DENSITY (IN G/CC) =	0.02
OUTLET LOADING (IN KG/H3) =	3.26	REFRACTIVE INDEX: REAL PART	1.06
LIGHT WAVELENGTH (IN MICRONS) =	0.550	IMAGINARY PART	-0.66

OUTLET PARTICLE SIZE DISTRIBUTION

CUMULATIVE WEIGHT PERCENT LESS THAN STATED PARTICLE SIZE	PARTICLE SIZE (MICRON)
---	---------------------------

1.0	0.000
2.0	0.000
3.0	0.000
4.0	0.000
5.0	0.000
10.0	0.000
15.0	0.000
20.0	0.000
30.0	0.000
40.0	0.000
50.0	0.000
60.0	0.000
70.0	0.001
80.0	0.003
85.0	0.005
90.0	0.009
95.0	0.026
96.0	0.035
97.0	0.051
98.0	0.084
99.0	0.182

SINGELMAN NUMBER RANGE

1.0 - 2.0

PERCENT LIGHT TRANSMITTED = 80.99

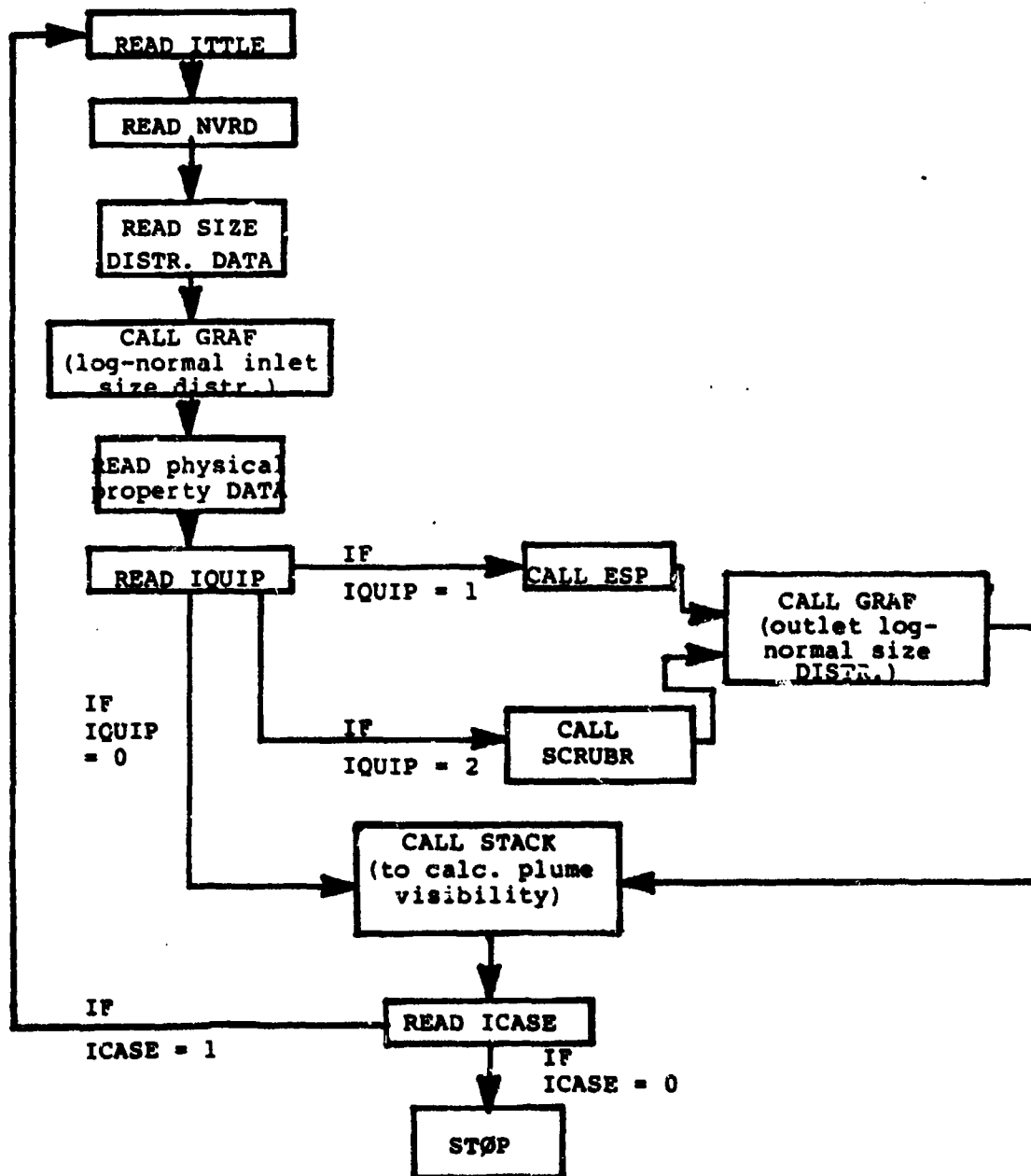
Figure B-1. Continued. Output Format

APPENDIX C
FORTRAN LISTING

The following FORTRAN program performs the various visibility and control calculations. It was originally written on a UNIVAC 90/80-3, and later converted for use on a CDC 6600. The version shown here is for the CDC 6600.

COMPUTER PROGRAM FLOW CHART

Figure C-1.



```

1      PROGRAM NJITZ (INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT)
2      .....
3      THIS PROGRAM WAS WRITTEN IN 1981 BY GORDON A. LEWANDOWSKI
4      OF THE NEW JERSEY INSTITUTE OF TECHNOLOGY
5      UNDER AIN FINCE. CONTRACT NO. F08635-80-C0222
6      .....
7      COMMON/ANDRD/INUM0,CLCW(101)
8      COMMON/ASCHIN/ALB,PD,EFFS,NS
9      COMMON/RESP/EFPS,SCATIN
10     COMMON/ACHAR/ALAM,PATH,REFRAC
11     COMMON/ALON/ZI,NMOP
12
13     *** COMMON BLOCKS ARE USED TO TRANSFER DATA BETWEEN THE
14     MAIN PROGRAM AND SUBROUTINE4
15     ANDRD,ASCHIN,DE-P,ACHAR,ALON,AND NMOUT ARE THE
16     NAMES OF THE COMMON BLOCKS. *****
17
18     COMPLEX REFRAC
19     DIMENSION ON DPC(101),DEND(101),CWRD(101)
20     DIMENSION ON DPC(101),CWRD(101),PTLN(101)
21     CLCW(1) = 0.0
22     CLCW(2) = 1.00
23     CLCW(101) = 40.94
24     DO 9 J=3,100
25     CLCW(J) = CLCW(J-1) + 1.00
26     9 CONTINUE
27
28     *** CLCW IS A FUNCTION THAT DIVIDES THE CUMULATIVE WEIGHT
29     DISTRIBUTION INTO EQUAL INCREMENTS OF 10. *****
30
31     1 CONTINUE
32     INUM0=0
33
34     C *** READ AND PRINT TITLE ****
35     C
36     READ(5,1010)ITITLE
37     FORMAT(1X,A10)
38     WRITE(6,5)
39     4 FORMAT(11H,1010,32(10H))
40     WRITE(6,ITITLE)
41     FORMAT(10X,A10)
42     5 FORMAT(10X,32(10H))
43     WRITE(6,5)
44
45     C *** HEAD SIZE DISTRIBUTION AS CUMULATIVE WEIGHT & LESS THAN (CWRD)
46     C PARTICLE SIZE (INPRD) IN MICRONS *****
47     C
48     READ(5,1020)NPRD
49     1020 FORMAT(1X,10)
50     HEAD(1:1020) = (CWRD(J),NPRD(J),J = 1,NPRD)
51     1015 FORMAT(1X,10)
52     IF (INPRD(1).EQ.0.0) DPRD(1) = 0.0001
53     IF (CWRD(1).EQ.0.0) CWRD(1) = 0.0001
54
55     C *** SUBROUTINE NGAFF FITS THE HEAD DISTRIBUTION DATA TO A
56     C SINGLE-LINE LOG-NORMAL EQUATION. THAT EQUATION IS THEN
57     C USED TO INTERPOLATE OR EXTRAPOLATE THE SIZE DISTRIBUTION AS NEEDED
58     C
59     CALL NGAFF (INPRD,CWRD,NPRD,OM)
60

```

Figure C-2. Computer Source Code Listing

	C	*** HEAD-CLINE CHARACTERISTICS: PLUME WIDTH (PATH) IN METERS.	00011200
	C	PARTICLE LOADING (L) IN MG/M3, PARTICLE DENSITY (RHO)	00011300
62	C	IN G/CC, COMPLEX REFRACTIVE INDEX OF PARTICLES (REFRAC), AND	00011400
	C	WAVELENGTH OF LIGHT (ELAM) IN WHICH THE PLUME IS OBSERVED	00011500
	C	(IN MICRONS) **000	00011600
	C		00011700
70	C	HEADLINE: (L) PATH: (L) RHO: (L) REFRAC: (L) ELAM	00011800
	C	1000 FORM: (L) (L) (L) (L) (L) (L) (L) (L) (L) (L) (L) (L) (L) (L) (L) (L)	00011900
	C	*** IF NO VALUE IS GIVEN FOR REFRAC, THE VALUE FOR AMNPHOUS	00012000
	C	CANONIC AT 540 N IS ASSUMED (1.00 - 0.001).	00012100
74	C	IF NO VALUE IS GIVEN FOR ELAM, AN AVERAGE WAVELENGTH FOR	00012200
	C		00012300

Figure C-2. Continued. Computer Source Code Listing

PROGRAM NJ172		7/17/74 OPT=1	FIN 4.0520	30707/RI 13.02.14	PAGE 2
	C	VISIBLE LIGHT IS ASSUMED OF 0.550 MICRONS. *****			00012500
		WLN = WLN (REFRACT)		00012500	
		WLN = WLN (REFRACT)		00012500	
80		IF (WLN, EQ, 0.0) GO TO 0000		00012500	
		GO TO 0000		00012500	
		0000 IF (WLN, EQ, 0.0) GO TO 0007		00012500	
		GO TO 0007		00012500	
85		0007 WLNAC = 11.00 - 0.001		00012500	
		WLN = REAL (WLNAC)		00012500	
		WLN = REAL (WLNAC)		00012500	
		0008 IF (WLN, EQ, 0.0) WLN = 0.550		00012500	
		WLN = 0.550		00012500	
90		1070 READ (1, 1070) WLN		00012500	
		FORMAT (1, 1070)		00012500	
		IF (WLN, EQ, 0.0) GO TO 6		00012500	
		IF (WLN, EQ, 0.0) GO TO 7		00012500	
		GO TO 8		00012500	
95		0000 READ ESP SPECIFIC COLLECTION AREA (SCA) AS WZ OF PLATE AREA		00012500	
		FOR 1000 M3/MIN OF GAS *****		00012500	
		READ (1, 1050) SCA		00012500	
		1050 FORMAT (1, 1050) SCA		00012500	
		CALL ESP (INPE, CWDZ)		00012500	
100		0000 SUBROUTINE "ESP" CALCULATES THE OUTLET PARTICLE SIZE		00012500	
		DISTRIBUTION AND LOADING FROM AN ELECTROSTATIC PRECIPITATOR.		00012500	
		THIS DISTRIBUTION IS THEN NORMALIZED BY CALLING "GRAPH". ***		00012500	
105		IF (INDRO, EQ, 1) GO TO 11		00012500	
		CALL GRAPH (INPE, CWDZ, NE, DP)		00012500	
		GO TO 6		00012500	
110		0000 READ SCRAMMER D-TA: LIQUID/GAS RATIO (ALSO AS M3/MIN LIQUID		00012500	
		FOR 1000 M3/MIN GAS AND PRESSURE DROP (PD) AS MM. MERCURY **		00012500	
		D, AD (1, 1060) ALB, PD		00012500	
		1060 FORMAT (1, 1060) ALB, PD		00012500	
115		0000 SUBROUTINE "SCRAM" CALCULATES THE OUTLET PARTICLE SIZE		00012500	
		DISTRIBUTION AND LOADING FROM A HIGH ENERGY VENTURI SCRAMMER.		00012500	
		THIS DISTRIBUTION IS THEN NORMALIZED BY CALLING "GRAPH". ***		00012500	
120		CALL SCRAM (INPE, CWDZ)		00012500	
		IF (INDRO, EQ, 1) GO TO 11		00012500	
		CALL GRAPH (INPE, CWDZ, NE, DP)		00012500	
		GO TO 6		00012500	
125		0000 SUBROUTINE "STACK" PERFORMS THE VISIBILITY CALCULATIONS. ****		00012500	
		CALL STACK (INPE)		00012500	
		1070 READ (1, 1070) SCALF		00012500	
		1070 FORMAT (1, 1070) SCALF		00012500	
130		IF (SCALF, EQ, 0.0) GO TO 2		00012500	
		GO TO 1		00012500	
		2 STOP		00012500	
		END		00012500	

Figure C-2. Continued. Computer Source Code Listing

SUMMIT[NE ANAF 76/76 001-1

FIN 4,8-528

30767/01 13.02.14

PAGE

1

```

1      SUMMIT[NE ANAF (UPND,CURD,NVND,DP)
2      C
3      C
4      C
5      C
6      C
7      C
8      C
9      C
10     C
11     C
12     C
13     C
14     C
15     C
16     C
17     C
18     C
19     C
20     C
21     C
22     C
23     C
24     C
25     C
26     C
27     C
28     C
29     C
30     C
31     C
32     C
33     C
34     C
35     C
36     C
37     C
38     C
39     C
40     C
41     C
42     C
43     C
44     C
45     C
46     C
47     C
48     C
49     C
50     C
51     C
52     C
53     C
54     C
55     C
56     C
57     C
58     C
59     C
60     C
61     C
62     C
63     C
64     C
65     C
66     C
67     C
68     C
69     C
70     C
71     C
72     C
73     C
74     C
75     C
76     C
77     C
78     C
79     C
80     C
81     C
82     C
83     C
84     C
85     C
86     C
87     C
88     C
89     C
90     C
91     C
92     C
93     C
94     C
95     C
96     C
97     C
98     C
99     C
100    C

```

Figure C-2. Continued. Computer Source Code Listing

```

1      SUMROUTINE ESP(IMP,DPE,CODE)
2      *** PROGRAM CALCULATES THE INLET PARTICLE SIZE DISTRIBUTION AND LOADING
3      FROM AN ELECTROSTATIC PRECIPITATOR WITH SPECIFIC COLLECTION SURFACE
4
5      COMMON/RESP/FF,SCA,NE
6      COMMON/ANNO/INNO,CLCW(101)
7      COMMON/ACON/PP,MMOP
8      DIMENSION DP(101),DPE(101),CODE(101),SUME(101)
9
10     *** EQUATIONS USED TO CALCULATE ESP EFFICIENCY
11
12     FRACTIONAL EFFICIENCY = 1 - EXP(-SCA*MMOP)
13     V = MIGRATION VELOCITY (IN/SEC) = 8.05E-05*E*E*E*E*E*(CD/(CD+2))/V
14     F = 40 KV DISCHARGE VOLTAGE AND 4 INCH PLATE-TO-PLATE SPACING
15     EC = E*E = FIELD STRENGTH = 3.50 KV/CM
16     DP = INLET PARTICLE SIZE IN MICRONS
17     CD = DIELECTRIC CONSTANT OF PARTICULATE, WHICH FOR CARBON IS ABOUT
18     FOR AIR AT 750 F
19     V = GAS VISCOSITY = 1.024 CP
20     K = FUDGE FACTOR, SINCE THE MODEL EQUATION FOR THE
21     MIGRATION VELOCITY APPLIES TO PARTICLES LARGER THAN
22     100 MICRONS (WHICH IS LARGER THAN MOST OF THE PARTICLES
23     ENTERED BY THE TEST CELL), A "K" VALUE OF 600 WAS USED
24     IN THE PROGRAM
25     CONTINUED EQUATIONS
26     FRACTIONAL EFFICIENCY = 1 - EXP(-0.750*SCA*DP)
27     WHERE SCA IS IN M2 OF COLLECTION PLATE PER 1000 M3/MIN OF GAS FLOW
28     DP IS IN MICRONS
29     THUS, EACH PARTICLE SIZE HAS ITS OWN EFFICIENCY. THE OVERALL
30     EFFICIENCY IS THE SUM OF THE EFFICIENCIES FOR EACH PARTICLE SIZE
31     TIMES THE WEIGHT FRACTION FOR EACH SIZE, SINCE BY SUBROUTINE GRAP
32     (AND CLCW), THERE ARE 100 INCREMENTS, ALL OF THE SAME
33     WEIGHT PERCENT. THE OVERALL EFFICIENCY IS SIMPLY THE SUM
34     OF THE FRACTIONAL EFFICIENCIES.
35
36     SUM = 0.0
37     A = 0.0750*SCA
38     DO 10 I = 1,100
39     DPE(I) = (DP(I)**A) * DPE(I)/(2.0)
40     SUM = SUM + DPE(I)
41
42     3 CONTINUE
43     EFF = 100.0*SUM
44     WRITE(10,1001)
45     1001 FORMAT(17.14,'AN ELECTROSTATIC PRECIPITATOR HAS BEEN ASSUMED
46     1002 CONTROL DEVICE 0000)
47     WRITE(10,1011)SCA
48     1011 FORMAT(17.14,'THE SPECIFIC COLLECTION SURFACE IS')
49     1012 FORMAT(17.14,'M2 PER 1000 M3/MIN')
50     1013 FORMAT(17.14,'WHICH PRODUCES AN OVERALL COLLECTION EFFICIENCY OF')
51     1014 FORMAT(17.14,'%')
52     WRITE(10,1015)
53     1015 FORMAT(17.14,'INLET LOADING =',F5.2,'M3/M3')
54     1016 FORMAT(17.14,'INLET PARTICLE SIZE DISTRIBUTION')
55     WRITE(10,1017)
56     1017 FORMAT(17.14,'')

```

Figure C-2. Continued. Computer Source Code Listing


```

1      SIMHMITIME STACK (DPI)
2      *** SYSTEM DEPENDENT THE VISIBILITY CALCULATIONS BASICALLY USING
3      THE METHOD OF HALOW & ZEIN (JAPCO) VOL. 23, PP. 914-915.
4      AUGUST 1973. HOWEVER, THERE HAVE BEEN A NUMBER OF IMPORTANT
5      MODIFICATIONS AS DESCRIBED BELOW. *****
6
7      COMMON/ACHAR/ELAM,PATH,REFRAC
8      COMMON/ACOM/71,NMOP
9      COMMON/AROOT/1,MIND,CICU(10)
10     DIMENSION NO(1:1000),ENT(1000),NO(1000),NO(1000)
11     COMPLEX YV,REFRAC,NM,NJC,PNT(2,4),R2(4),AM,RH
12     COMPLEX Q(1000),UNC(1000),UNC(1000),UNC(1000)
13     COMPLEX NIMAR
14     NIMAR = (0.0,1.0)
15     RIFPR = 0.0
16     DO 100 K=1,100
17     OP1 = (DP(K),OP(K))/2.0
18     IF (INT(PT(5,K)) .GT. 24)
19
20     *** PARTICLES LARGER THAN 50 MICRONS HAVE A NEGOTIABLE EFFECT
21     ON VISIBILITY, AND THEREFORE, HAVE BEEN EXCLUDED FROM THE
22     CALCULATIONS IN ORDER TO SAVE COMPUTATION TIME. *****
23
24     IV = 3.1415927*DP1/RLAM
25     YV = 0.0*MAC*YV
26     USON = 0.0
27     NM(1) = SIN(IV)
28     NM(2) = -SIN(IV)
29     NM(3) = COS(IV)
30     NM(4) = -COS(IV)
31     Q(1) = NIMAR
32     Q(2) = -1.0*Q(1)
33
34     *** MAXIMUM VALUES (NMAX) OF THE ORDER (N) OF THE RICCATI-BESSEL
35     FUNCTIONS ARE GENERATED BY THE FOLLOWING THREE EQUATIONS
36     ACCORDING TO U. J. COMBE, U.J., APPLIED OPTICS, VOL. 19, PP. 1505-
37     1508, MAY 1980. *****
38
39     IF (IV.GE.4200.0) NMAX=IV+4.0*(IV**E3)**.2
40     IF (IV.LT.4200.0) NMAX=IV+4.0*(IV**E3)**.2
41     IF (IV.LT.4.0) NMAX=IV+4.0*(IV**E3)**.1
42     DO 99 N=1,NMAX
43
44     *** THE NEXT 14 LINES GENERATE BESSEL FUNCTIONS OF THE ARGUMENT
45     IV, ACCORDING TO THE METHOD OF LENTZ, U.J., APPLIED OPTICS,
46     VOL. 19, PP. 640-671 (MARCH 1976). *****
47
48     UP(1) = 1.0*(FLOAT(N)+0.5)/IV
49     UN(1) = 0.0
50     UP(2) = -2.0*(FLOAT(N+1)+0.5)/IV
51     UN(2) = 0.0
52     UP(3) = 0.0
53     UN(3) = 0.0
54     IF (N.EQ.1)
55     UP(4) = 2.0*(FLOAT(N+1)+0.5)/IV
56     UN(4) = 0.0
57     IF (N.EQ.2)
58     UP(5) = 0.0
59     UN(5) = 0.0
60     IF (N.EQ.3)
61     UP(6) = 0.0
62     UN(6) = 0.0
63     IF (N.EQ.4)
64     UP(7) = 0.0
65     UN(7) = 0.0
66     IF (N.EQ.5)
67     UP(8) = 0.0
68     UN(8) = 0.0
69
70     *** PNR AND Q ARE LOGARITHMIC DERIVATIVE FUNCTIONS USED
71     TO CALCULATE AN & NM.

```

Figure C-2. Continued. Computer Source Code Listing

APPENDIX D COMPUTER PROGRAM NOMENCLATURE

A1	= real part of a_n denominator
A2	= a_n numerator/A1
A3	= a_n denominator/A1
AN	= a_n
AK	= Stokes' parameter (k) in Calvert's scrubber equations (dimensionless)
AKF	= $AK(f) + 0.7$, where $f = 0.5$
ALG	= liquid/gas ratio
B	= intercept of straight-line log-normal equation (in GRAF)
BIMAG	= i
B1	= real part of b_n denominator
B2	= b_n numerator/B1
B3	= b_n denominator/B1
BJ	= J_{v-1}/J_v (with real argument)
BJC	= J_{v-1}/J_v (with complex argument)
BN	= b_n
CC	= Cunningham correction factor in scrubber equations (dimensionless)
CLCW	= cum. wt. % in 1% increments
CN	= n/x
CWDE	= outlet cumulative wt. % from ESP
CWDS	= outlet cumulative wt. % from scrubber
CWRD	= raw cum. wt. % input data

DD = scrubber drop size (by Nukiyama-Tanasawa equation), in microns

DHUN is defined by line 7 of function EINV

DP = normalized particle size from subroutine GRAF (in microns)

DPE = outlet particle size from ESP (in microns)

DPRD = raw particle size data (in microns)

DPS = outlet particle size from scrubber (in microns)

DPI = average value of DP in interval (microns)

EFF = calculated ESP efficiency (%)

EFFS = calculated scrubber efficiency (%)

EINV(RCW) = inverse normal distribution function (RCW = variable)

ETA is defined by line 17 of function EINV

ETASQ is defined by line 16 of EINV

E3 = $1/3$

EF2 is defined by line 15 of function EINV

FND = FLOAT(NVRD)

G is defined by line 37 of subroutine ESP

GRAF is a subroutine that uses the method of least squares to fit the raw particle size distribution data to a straight-line equation

I, IJ, IK, IL are all counters

ICASE = 0, when there are no further cases, and = 1 when another set of data cards (i.e. another case) follows

INOGO = 1 if the electrostatic precipitator, or scrubber, has such a high efficiency that virtually all of the original particle size distribution is collected. Otherwise, it is 0.

IP = p (in generating values of w)
 IQUIP = 0, if there is no particle collection device; = 1, if there is an electrostatic precipitator; = 2, if there is a venturi scrubber
 ITTLE = alphanumeric variable (maximum of 10 letters) corresponding to the case title.
 J,JI are counters
 K = counter
 L = $(-1)^{P+1}$ (in generating values of w)
 N = n (order of Riccati-Bessel functions)
 NE = number of data pairs for outlet distribution from ESP
 NMAX = max. value of n
 NS = number of data pairs for outlet distribution from scrubber
 NVRD = number of raw data pairs for inlet size distribution
 PATH = plume width = effective stack diameter (in meters)
 PD = pressure drop across scrubber (in mm. mercury)
 PN_X = $P_n(x) = \psi_n'(x)/\psi_n(x)$
 PN_Y = $P_n(y) = \psi_n'(y)/\psi_n(y)$
 PTLN = natural log of scrubber penetration
 Q = $Q_n(x) = \xi_n'(x)/\xi_n(x)$
 QEXT = extinction coefficient = $-\frac{2}{x^2} \Sigma(2n+1) \text{real}(a_n+b_n)$
 QSUM = $\Sigma(2n+1) \text{real}(a_n+b_n)$
 RB1X = $\psi_n(x)$
 RB2 = $\beta_n(x)$
 RB3 = $\xi_n(x)$

REFRAC = complex refractive index of particle (dimensionless)
 RHOP = particle density (in g/cc)
 RIIM = imaginary part of refractive index
 RIRL = real part of refractive index
 RNM = calculated Ringelmann number
 RNMAX = upper estimate of Ringelmann number (=RNM+0.5)
 RNMIN = lower estimate of RNM
 S = fractional penetration
 SCA = specific collection area of ESP (in m² per 1000 m³/min of gas)
 SGN is defined by lines 11 and 14 of EINV
 SLOPE = slope of straight-line log-normal equation (in GRAF)
 STACK is the subroutine that calculates plume visibility
 STEPB = $\sum_i \left(\frac{Q_{ext}}{d_p} \right)_i$
 SUM = % penetration
 SUME = cumulative wt % penetration for particles of size DPE
 SUMS = cumulative wt % penetration for particles of size DPS
 SUMX = EX
 SUMXY = EXY
 SUMX2 = $\sum (X^2)$
 SUMY = EY
 TRANS = calculated fractional transmittance =

$$\exp\left(\frac{-3WD}{2\rho p}\right) \frac{1}{100} \sum_{i=1}^{100} \left(\frac{Q_{ext}}{d_p} \right)_i$$

TRANSW = % transmittance
 VGT = gas velocity in venturi scrubber throat (in meters/sec)
 WD = $|w_p, \dots, w_2|$, with real arguments
 WDC = $|w_p, \dots, w_2|$, with complex arguments
 WI = IMAG(WNC-WDC)
 WN = $|w_p, \dots, w_1|$, with real arguments
 WNC = $|w_p, \dots, w_1|$, with complex arguments
 WP = $w_p = (-1)^{p+1} \frac{2(v+p-1)}{x}$
 WPC = $(-1)^{p+1} \frac{2(v+p-1)}{y}$
 WR = real (WNC-WDC)
 X = EINV(CWRD)
 X1 = EINV(CLCW)
 X2 = x^2
 XLAM = wavelength of light used to view the plume (λ) (in microns)
 XV = $\pi d_p / \lambda$ (dimensionless)
 Y = $\log_{10} \text{DPRD}$
 YV = $m \pi d_p / \lambda$ (dimensionless)
 ZI = particle loading (in mg/m^3)