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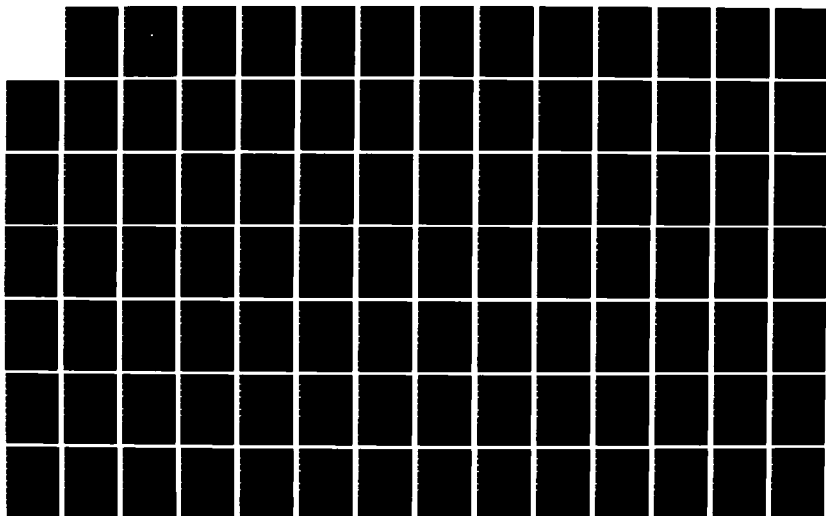
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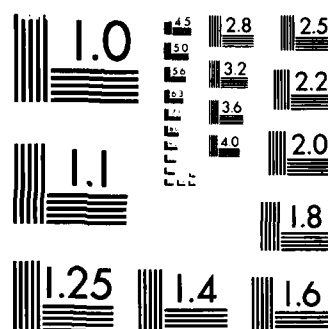
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NAVAL POSTGRADUATE SCHOOL
Monterey, California



THESIS

THE EFFECTIVENESS OF HEAT EXCHANGERS
WITH ONE SHELL PASS AND
FIVE TUBE PASSES

by

Lawrence E. Hess

September 1985

Thesis Advisor:

Allan D. Kraus

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REPORT DOCUMENTATION PAGE		READ INSTRUCTIONS BEFORE COMPLETING FORM
1. REPORT NUMBER	2. GOVT ACCESSION NO. AD-A161019	3. RECIPIENT'S CATALOG NUMBER
4. TITLE (and Subtitle) The Effectiveness of Heat Exchangers with One Shell Pass and Five Tube Passes		5. TYPE OF REPORT & PERIOD COVERED Master's Thesis; September 1985
7. AUTHOR(s) Lawrence E. Hess		6. PERFORMING ORG. REPORT NUMBER
9. PERFORMING ORGANIZATION NAME AND ADDRESS Naval Postgraduate School Monterey, California 93943-5100		8. CONTRACT OR GRANT NUMBER(s)
11. CONTROLLING OFFICE NAME AND ADDRESS Naval Postgraduate School Monterey, California 93943-5100		10. PROGRAM ELEMENT, PROJECT, TASK AREA & WORK UNIT NUMBERS
14. MONITORING AGENCY NAME & ADDRESS (if different from Controlling Office)		12. REPORT DATE September 1985
		13. NUMBER OF PAGES 121
		15. SECURITY CLASS. (of this report) Unclassified
		15a. DECLASSIFICATION/DOWNGRADING SCHEDULE
16. DISTRIBUTION STATEMENT (of this Report) Approved for public release; distribution is unlimited		
17. DISTRIBUTION STATEMENT (of the abstract entered in Block 20, if different from Report)		
18. SUPPLEMENTARY NOTES		
19. KEY WORDS (Continue on reverse side if necessary and identify by block number) Heat Exchanger Effectiveness N_{tu} Method Five Tube Pass		
20. ABSTRACT (Continue on reverse side if necessary and identify by block number) Heat exchangers with one shell pass and n tube passes are often referred to as 1-n exchangers. The heat transfer literature contains many references to studies of 1-n exchangers when n is even but apparently, other than a single study and some work pertaining to the 1-3 exchanger at the Naval Postgraduate School, little work has been done with respect to the 1-n exchanger when n is odd. This thesis expands upon the study of 1-n exchangers with n being odd.		

20. (Continued)

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The Effectiveness of Heat Exchangers
With One Shell Pass and
Five Tube Passes

by

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Lieutenant Commander, United States Navy
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Submitted in partial fulfillment of the
requirements for the degree of

MASTER OF SCIENCE IN MECHANICAL ENGINEERING

from the

NAVAL POSTGRADUATE SCHOOL
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ABSTRACT

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While a completely closed form solution was found to be unfeasible, a polynomial approximation has been developed that yields the effectiveness (ϵ) of the two possible arrangements of the 1-5 exchanger as a function of the capacity rate ratio (R) and the number of transfer units (N_{tu}). This will enable the analyst to consider exchangers where the inlet to and outlet from the tubes are at opposite ends of the exchanger.

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NOMENCLATURE

English Letter Symbols

- A = Exchanger heat-transfer surface, sq m
- A_m = Coefficient of the mth value dimensionless
- A_0 = Coefficient, dimensionless
- A_1 = 1st order coefficient to be multiplied by N_{tu} , dimensionless
- A_2 = 2nd order coefficient to be multiplied by N_{tu}^2 , dimensionless
- A_3 = 3rd order coefficient to be multiplied by N_{tu}^3 , dimensionless
- A_4 = 4th order coefficient to be multiplied by N_{tu}^4 , dimensionless
- A_5 = 5th order coefficient to be multiplied by N_{tu}^5 , dimensionless
- a = Exchanger heat-transfer surface, sq m/m
- C = Capacity rate, W/°K. Also designates dimensionless arbitrary constant
- C_{pc} = Specific heat at constant pressure of cold fluid, J/kg°K
- C_{ph} = Specific heat at constant pressure of hot fluid, J/kg°K
- D = Empirical value of effectiveness (computer generated), dimensionless
- e = Error. Also used as the exponential function
- F = Logarithmic mean temperature difference correction factor, dimensionless
- L = Exchanger length, m
- N = Number of effectiveness empirical data points used to determine a curve for R, dimensionless

n = Number of tube passes, dimensionless. Also number of equations, dimensionless
 n_c = A related N_{tu} per unit length cold side, m^{-1}
 n_h = A related N_{tu} per unit length hot side, m^{-1}
 N_{tu} = Number of transfer units, dimensionless
 P = Temperature group, dimensionless
 q = Total rate of heat transfer, W
 q_{max} = Maximum total rate of heat transfer, W
 R = Capacity rate ratio, dimensionless
 S = Temperature group, dimensionless
 S_r = Sum of the squares of the residuals, dimensionless
 T = Hot fluid temperature, °C
 T_{pi} = Particular integral, dimensionless
 T_1 = Hot fluid temperature in, °C
 T_2 = Hot fluid temperature out, °C
 t_1 = Cold fluid temperature in, °C
 t_2 = Cold fluid temperature out, °C
 t_a = Cold fluid temperature 1st pass, °C
 t_{ab} = Cold fluid temperature between 1st and 2nd passes
 t_b = Cold fluid temperature 2nd pass, °C
 t_{bc} = Cold fluid temperature between 2nd and 3rd passes
 t_c = Cold fluid temperature 3rd pass, °C
 t_{cd} = Cold fluid temperature between 3rd and 4th passes
 t_d = Cold fluid temperature 4th pass, °C
 t_{de} = Cold fluid temperature between 4th and 5th passes
 t_e = Cold fluid temperature 5th pass, °C

- U = Overall heat transfer coefficient, $W/m^2 - ^\circ C$
 W = Mass flow, kg/sec.
 x = length coordinate, m. Also used to represent a constant value in a sequence
 y = Sum of m th degree polynomial, defined by eq. (5.1), dimensionless

Greek Letter Symbols

- α = Root of auxiliary differential equation, $1/m$
 ϵ = Exchanger effectiveness, dimensionless
 λ = Combination of variables defined by equation (3.12), dimensionless
 Σ = Summation, dimensionless
 σ^2 = Variance, dimensionless
 θ_m = Mean temperature difference for exchanger, $^\circ C$
 ∂ = Indicates partial derivative, dimensionless
 β = A combination of terms defined by eq. (3.23)

Subscripts

- c = Cold fluid
 h = Hot fluid
 i, j, k = Values in a sequence
 m = Degree or order, an exponent
 1 = inlet
 2 = outlet

ACKNOWLEDGEMENT

I wish to thank my wife, Cheri, who has been a sustaining influence from the beginning and to my parents who launched my career. Also my sincere gratitude to Dr. Allan D. Kraus for his time, guidance and patience. Without his assistance and encouragement this thesis would not have been possible.

Finally, I wish to thank Uncle Sam who made one of my life-long goals possible.

I. INTRODUCTION

In many engineering applications, it is desirable to transfer thermal energy between fluids at different temperatures. This action may be economically accomplished with the aid of a heat exchanger.

The primary function of a non-direct contact heat exchanger is to provide two paths of flow, one for the hot fluid and one for the cold, by means of which heat can be transferred through walls separating the fluids.

The quantity of heat transferred is governed by three factors: 1) the amount and nature of the heat transfer surface to which the two fluids are exposed, 2) the overall heat transfer coefficient, and 3) the mean temperature difference across the intervening wall from one fluid to the other.

Numerous flow arrangements and geometric designs are possible. One of the most common types of heat exchangers is the shell and tube type. Here one fluid flows through the tubes. The tubes are enclosed in a shell with provisions for the other fluid to flow through the spaces between and exterior to the tubes. Overall flow may be either parallel or counter, but in most cases, the latter is preferred. The reason for this will be seen later. One of the most common flow arrangements used in the shell and tube

heat exchangers is a combination of the two, the parallel-counterflow exchanger. Heat exchangers with one shell pass and n tube passes are therefore referred to as 1- n heat exchangers.

One example of this flow arrangement is the one shell-pass two tube pass exchanger as shown in Figure 1.1.

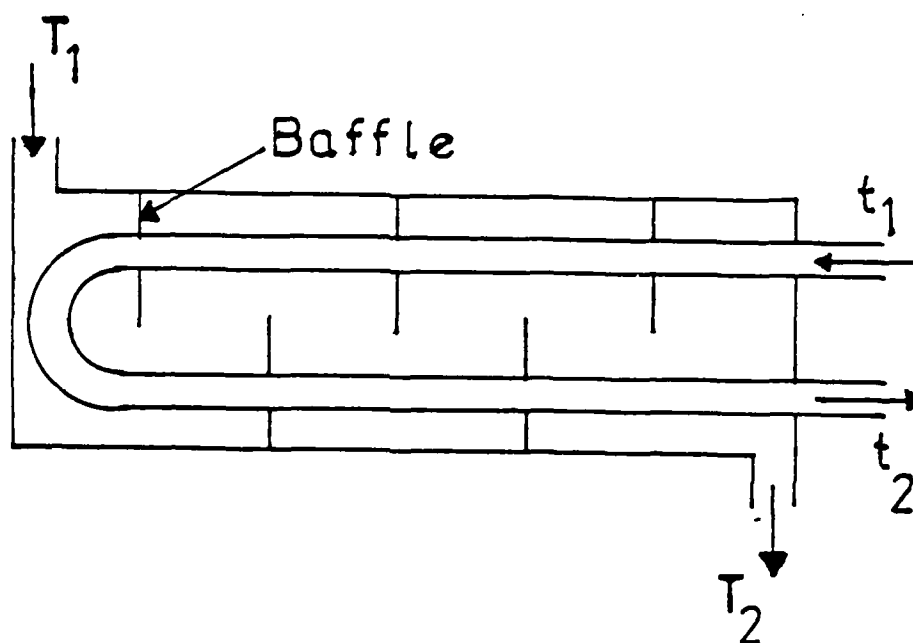


Figure 1.1 A 1-2 Heat Exchanger (One Shell Pass and Two Tube Passes)

This type of exchanger is configured so that all of the tube side fluid flows consecutively through half of the total number of tubes: The baffles in the shell serve to "mix" the shell fluid and to maintain fluid flow at right angles to the tube passes in order to obtain a maximum "shell side" heat transfer coefficient.

O'Hare [Ref. 1] has indicated that, to date, much work has been done on finding the logarithmic mean temperature difference for heat exchangers with an even number of passes but little has been done with exchangers having an odd number of passes. From this basic statement, he proceeded with a theoretical examination of the 1-3 heat exchanger which resulted in some startling conclusions. As a follow up to his work, this thesis will parallel and follow the format of O'Hare [Ref. 1] for the 1-5 parallel counter flow exchanger. One arrangement of the 1-5 exchanger is displayed in Figure 2.

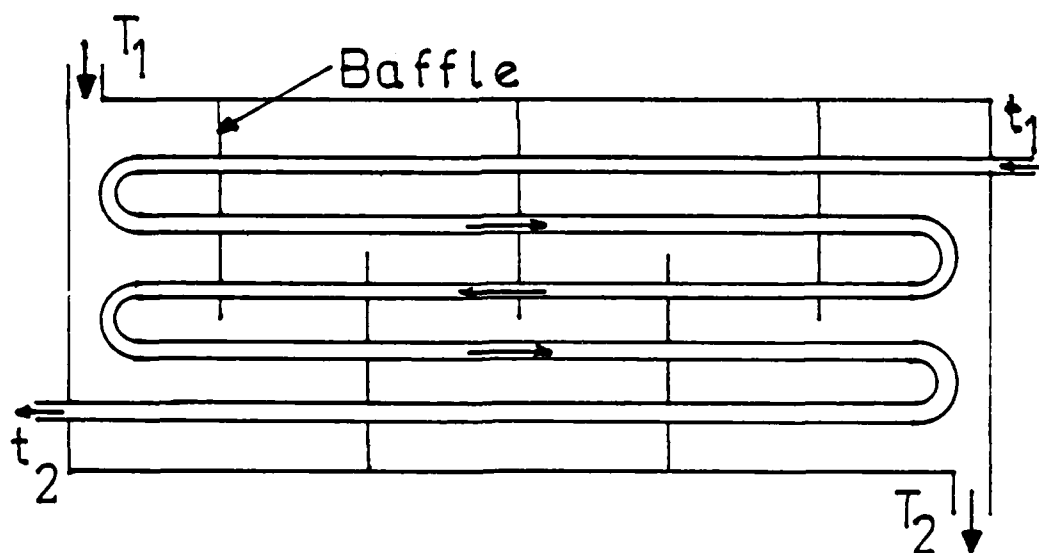


Figure 1.2 A 1-5 Heat Exchanger (One Shell Pass and Five Tube Passes)

II. THE DEVELOPMENT OF THE EFFECTIVENESS METHOD

A. HISTORICAL DEVELOPMENT

Nagle [Ref. 2: pp. 604-609], in 1931, credited Davis [Ref. 3] with a simplified method for computing actual temperature differences between two heat-interchanging streams which depart from true counter or concurrent (parallel) flow. This is now the familiar "F factor" method which expresses the actual mean temperature difference θ_m in $q = UA\theta_m$ as a fraction F of the counterflow logarithmic mean temperature difference, LTMD, θ_{mc} via $\theta_m = F\theta_{mc}$.

The example of initial interest was the 1-2 exchanger with a single shell pass and two continuous tube passes in counter and concurrent flow with it. The method involved derivation of the actual temperature difference for the flow pattern and formed the ratio $F = \theta_m/\theta_{mc}$. This familiar LMTD correction factor was plotted conveniently as functions of the effectiveness, ϵ , and the capacity rate ratio R with R as a parameter. These mean temperature difference correction charts are available for many flow arrangements [Ref. 4: pp. 829-833 and Ref. 5]. The effectiveness, ϵ (often called P or S), is always the cold fluid effectiveness and R is always the capacity rate ratio of cold fluid to hot fluid.

Nagle detailed assumptions and derivations for the 1-2, 1-4 and 1-6 exchangers. The F factors were obtained by Nagle through graphical integration and were accompanied by the comment that F factors for the 1-2 exchanger could be applied with negligible error to 1-4 and 1-6 exchangers. Underwood [Ref. 6: pp. 145-148] rederived the equations of Nagle for 1-2 and 1-4 exchangers to eliminate the need for obtaining F factors by graphical integration.

Bowman [Ref. 7: pp. 541-544] pointed out that for a very large or infinite number of tube passes, the F factor approached, as a limit, its value in crossflow with both fluids completely mixed. It was further stated that even at the limit, the F factors were only 1 to 2 percent lower than those for the 1-2 exchanger. A previous paper by Kraus and Kern [Ref. 8] did not confirm the generalization that 1-n exchangers differed only negligibly from the 1-2 exchanger although this lack of confirmation was obtained on an $\epsilon = f(R, N_{tu})$ basis. Moreover, the Kraus-Kern work does not confirm the generalizations on an $F = f(R, N_{tu}, \epsilon)$ basis.

From the standpoint of usefulness and good accuracy, it is essential that F factors, if they are to be used in preference to $\epsilon = f(R, N_{tu}, \text{flow arrangement})$, be obtained with precision. Plots of $F = f(R, \epsilon, = P \text{ or } S)$ [Ref. 4: pp. 829-833 and Ref. 5] show that the curves for particular values of R approach infinite slope as F decreases. While this can be partially alleviated by restricting $R < 1.0$ (a

constraint used in the $\epsilon = f(R, N_{tu}, \text{flow arrangement})$ approach), it is seen that small errors in the interpolation for R or $\epsilon = P$ or S can result in large fluctuations in the value of F .

In a comprehensive paper, Bowman, Mueller and Nagle [Ref. 9: pp. 283-294] presented graphs of F factors for shells with one through six shell passes and numbers of continuous tube passes respectively double the number of shell passes. In view of the earlier references to Nagle and Bowman, it should be noted that F factors were computed for the 1-2 exchanger in [Ref. 9: pp. 283-294] using the equations of Underwood [Ref. 6: pp. 145-158].

Ten Broeck [Ref. 10: pp. 1041-1042] prepared a graph of the dimensionless groups now known as ϵ , R and N_{tu} for the 1-2 exchanger. Such a graph had the added versatility of simplifying the calculation of performance in a given exchanger when operating at conditions different for those for which it was designed. Kays and London [Ref. 11: pp. 63-74] prepared similar graphs and tables of $\epsilon = f(R, N_{tu}, \text{flow arrangement})$ for the 1-2 exchanger and for several cases of crossflow and periodic flow.

In the foregoing discussion, it has been observed that there are two methods for the design and analysis of a heat exchanger. These are the so-called "F factor" and " ϵ - N_{tu} " approaches and it is to be noted that the Heat Transfer Literature contains many references of design equations for

either of these methods for exchangers that have one shell pass and even numbers of tube passes.

It was O'Hare [Ref. 1] who pointed out that there may be a virtue in having an odd number of tube passes particularly in a marine application. Such an arrangement allows the tube side fluid to enter one side of the exchanger and leave from the opposite side (see Figure 1.2).

With the possible use for an odd tube pass heat exchanger established, a literature search was conducted to uncover any previously solved cases of 1-n heat exchangers with n, the number of odd tube passes. O'Hare [Ref. 1], Fischer [Ref. 12], and Stevens, et. al. [Ref. 13] have dealt with this type of exchanger. Although Stevens, et. al. deal with multiple crossflow passes, all provide the foundation for the work reported here as well as additional work pertaining to the 1-3 exchanger. O'Hare's investigation centered around the development of a solution for the 1-3 exchanger in the effectiveness- N_{tu} framework while Fischer derived an equation using the mean temperature difference for the 1-3 exchanger. Moreover, Fischer expressed his results in terms of the correction factor F and treats only the case of the 1-3 exchanger. This thesis will expand on the N_{tu} method of thermal heat exchanger design by covering the 1-5 heat exchanger. The work will treat both the three counterflow and two parallel flow

and the two counterflow and three parallel flow (1-5:3P)
cases (see Figures 2.1 and 2.2).

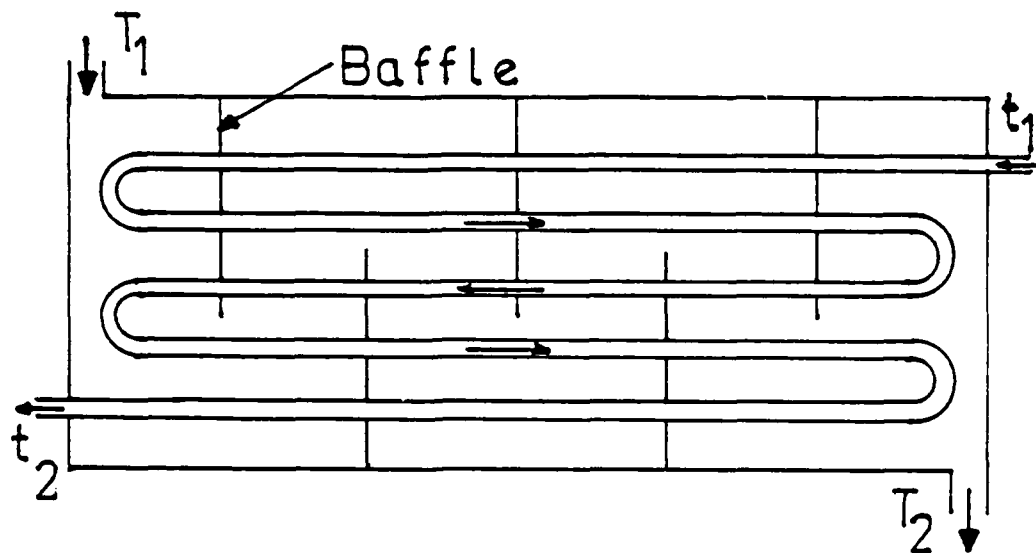


Figure 2.1 1-5:3C Five Tube Passes - Three in Counterflow

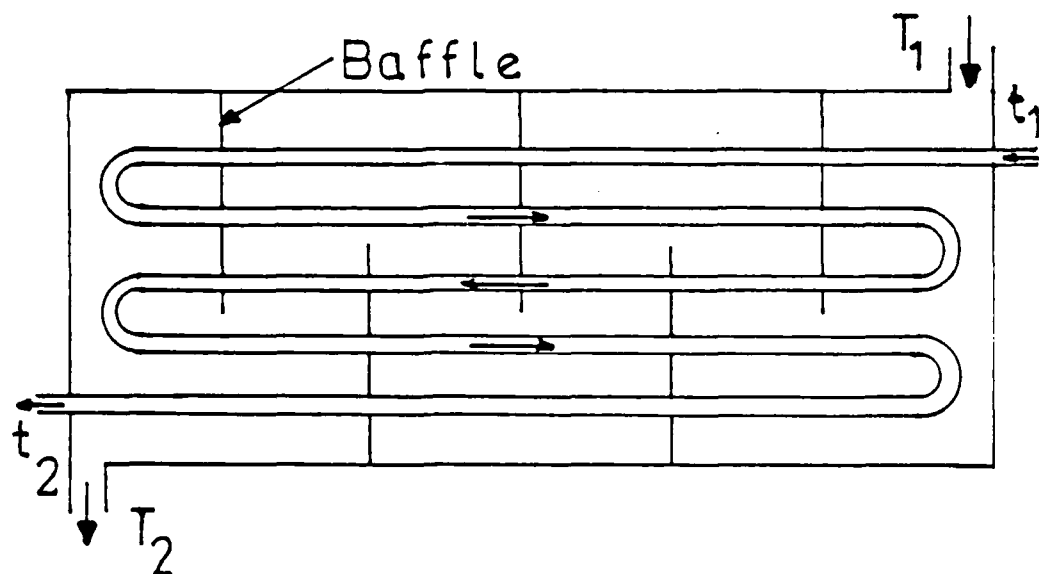


Figure 2.2 1-5:3P Five Tube Passes - Three in Parallel Flow

III. AN ATTEMPT AT AN ANALYTIC SOLUTION

A. EFFECTIVENESS AS A FUNCTION OF CAPACITY RATE RATIO AND EXCHANGER SIZE (N_{tu})

This section deals with an investigation into the effectiveness, ϵ , of a one shell pass-five tube pass heat exchanger, in which ϵ compares the actual heat transfer capability to the thermodynamically limited, maximum possible heat transfer capability. This exchanger heat transfer effectiveness is given by

$$\epsilon = \frac{q}{q_{\max}} = \frac{C_h(T_{\text{hot,in}} - T_{\text{hot,out}})}{C_{\min}(T_{\text{hot,in}} - t_{\text{cold,in}})} = \frac{C_c(t_{\text{cold,out}} - t_{\text{cold,in}})}{C_{\min}(T_{\text{hot,in}} - t_{\text{cold,in}})}$$

where $C_{\min}$ is the smaller of the C_h and C_c magnitudes (the capacity rates). Thus, ϵ possesses the significance of effectiveness of the heat exchanger from a thermodynamic point of view, with the magnitude of the effectiveness completely defining the heat transfer performance. In general we express $\epsilon = f(N_{tu}, R, \text{ and flow arrangement})$ and when the flow arrangement is specified or understood, it is said that $\epsilon = f(N_{tu}, R)$. [Ref. 11: pp. 14-26].

The number of heat transfer units N_{tu} is a nondimensional expression of the "heat transfer size" of the exchanger. When N_{tu} is small the exchanger effectiveness is low, and when N_{tu} is large, ϵ asymptotically approaches the limit

imposed by the flow arrangement and thermodynamic conditions. From inspection of the definition of N_{tu}

$$N_{tu} = \frac{AU}{C_{\min}} = \frac{1}{C_{\min}} \int_0^A U dA$$

it is clear that the overall conductance and transfer area affect the costs of attaining a high value for N_{tu} , ergo a high ϵ . The capacity rate ratio, R , as defined by

$$R = \frac{C_{\min}}{C_{\max}}$$

is simply the ratio of mass flow rate times specific heat capacity for the two streams. These can be considered as flow stream thermal-capacity rates, i.e., the energy storage rate in the stream per unit of temperature change. [Ref. 11: pp. 14-26]

The attempt taken in this thesis to develop a closed form solution has used the basic fundamentals of heat transfer as well as the foregoing definition. A closed form solution for ϵ was sought for both 1-5 exchangers with one having three out of five tube passes in parallel flow and the other having three out of five tube passes in counterflow. The analytical approach taken, and demonstrated in this section, is for three out of five tube passes in counterflow.

B. ANALYTICAL DEVELOPMENT

The derivation for the effectiveness, ϵ , of the 1-5 exchanger as a function of the capacity rate ratio, R , and number of transfer units, N_{tu} , depends on several assumptions.

- (1) The overall coefficient of heat transfer, U , does not vary within the exchanger.
- (2) The specific heat of both hot side and cold side fluids does not vary.
- (3) Each fluid is thoroughly mixed, that is, the temperature of both hot and cold side fluids is uniform over any cross section.
- (4) Steady flow conditions are maintained.
- (5) Heat losses to or from the environment are negligible.
- (6) No change of phase takes place; all heat transferred is sensible heat.
- (7) There is equal heat transfer surface in each pass.

The configuration is shown in Figure 3.1 where the five tube passes are designated with subscripts a, b, c, d and e. The temperature of the hot (shell side) fluid is indicated by upper case letters. For the cold (tube side) fluid, lower case letters are used. The subscript 1 always refers to the fluid inlet and the subscript 2 always refers to the fluid outlet.

With W_h and C_{ph} designating mass flow (kg/sec) and specific heat (Joules/kg $^{\circ}$ K) of hot fluid entering at T_1 and leaving at T_2 we define a capacity rate for the hot side

$$C_h = W_h C_{ph}$$

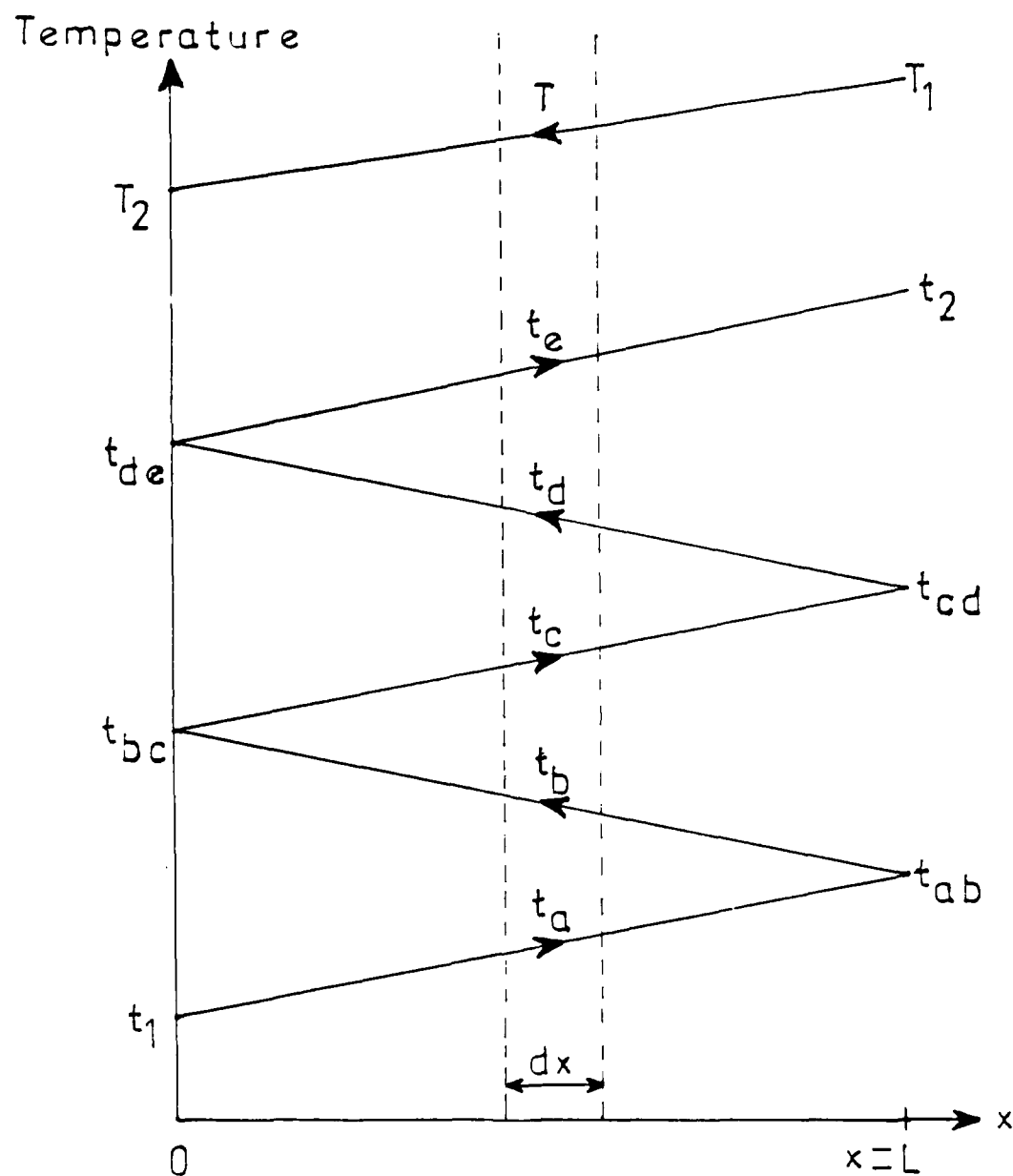


Figure 3.1 Three Counter Two Parallel Pass Configuration for Development of the Sought After Effectiveness Relationship

In similar fashion for the cold side (with W_c and C_{pc}) entering at t_1 and leaving at t_2 , we have

$$C_c = W_c C_{pc}$$

We then obtain an energy balance for the entire exchanger

$$C_h(T_1 - T_2) = C_c(t_2 - t_1) \quad (3.1)$$

Over the right hand side of the exchanger (Figure 3.1)

$$C_h(T_1 - T) = C_c(t_2 - t_e + t_d - t_c + t_b - t_a) \quad (3.2)$$

and a differentiation gives

$$C_h dT = C_c(dt_e - dt_d + dt_c - dt_b + dt_a) \quad (3.3)$$

Across dx , with a (m^2/m) , the surface per running meter of length of pass so that $A = 5aL$ is the total surface in the exchanger, we may write the heat transferred to the element dx in each cold pass.

$$C_c dt_a = Ua dx (T - t_a) \quad (3.4a)$$

$$C_c dt_b = -Ua dx (T - t_b) \quad (3.4b)$$

$$C_c dt_c = Ua dx (T - t_c) \quad (3.4c)$$

$$C_c dt_d = -Ua dx (T - t_d) \quad (3.4d)$$

$$C_c dt_e = Ua dx (T - t_e) \quad (3.4e)$$

Here it should be observed that due cognizance has been taken of the direction of the flow in each cold fluid pass with respect to the positive sense of the length coordinate, x , and U is the overall heat transfer coefficient ($W/m^2-^{\circ}C$).

With eqs. (3.4) in eq. (3.3)

$$C_h dT = Ua(5T - t_a - t_b - t_c - t_d - t_e)dx$$

or

$$\frac{dT}{dx} = n_h(5T - t_a - t_b - t_c - t_d - t_e) \quad (3.5)$$

where

$$n_h = \frac{Ua}{C_h}$$

is a sort of N_{tu} per unit length for the hot side.

Now differentiate eq. (3.5)

$$\frac{d^2T}{dx^2} = n_h \left(5 \frac{dT}{dx} - \frac{dt_a}{dx} - \frac{dt_b}{dx} - \frac{dt_c}{dx} - \frac{dt_d}{dx} - \frac{dt_e}{dx} \right)$$

and with eqs. (3.4) substituted

$$\frac{d^2T}{dx^2} = 5n_h \frac{dT}{dx} - n_c n_h (T - t_a + t_b - t_c + t_d - t_e) \quad (3.6)$$

where

$$n_c = \frac{Ua}{C_c}$$

where again the resemblance of n_c to N_{tu} can be noted.

From eq. (3.2) we obtain

$$\frac{C_h}{C_c} (T_1 - T) - t_2 = t_b - t_a - t_c + t_d - t_e \quad (3.7)$$

and with eq. (3.7) put into eq. (3.6)

$$\frac{d^2 T}{dx^2} - 5n_h \frac{dT}{dx} = -n_c n_h \left[T + \frac{C_h}{C_c} (T_1 - T) - t_2 \right]$$

or

$$\frac{d^2 T}{dx^2} - 5n_h \frac{dT}{dx} = -n_c n_h \frac{C_h}{C_c} [(R_c - 1)T + T_1 - R_c t_2] \quad (3.8)$$

where

$$R_c = C_c / C_h$$

is the capacity rate ratio for the cold side.

Notice that

$$n_c n_h \frac{C_h}{C_c} = \frac{Ua}{C_c} \cdot \frac{Ua}{C_h} \cdot \frac{C_h}{C_c} = \left(\frac{Ua}{C_c} \right)^2 = m$$

and

$$R_h = \frac{1}{R_c} = \frac{C_h}{C_c}$$

a capacity rate ratio for the hot side. Then, algebraic adjustment provides

$$\frac{d^2 T}{dx^2} - 5n_h \frac{dT}{dx} + m \left(\frac{1 - R_h}{R_h} \right) T = m \left(\frac{t_2}{R_h} - T_1 \right) \quad (3.9)$$

which is a linear, non-homogeneous, second order differential equation with constant coefficients having a complementary function

$$T_c = C_1 e^{\alpha_1 x} + C_2 e^{\alpha_2 x} \quad (3.10)$$

where C_1 and C_2 are arbitrary constants and where

$$\begin{aligned} \alpha_{1,2} &= \frac{5n_h}{2} \pm \frac{1}{2} \left[25n_h^2 - 4m \left(\frac{1 - R_h}{R_h} \right) \right]^{1/2} \\ &= \frac{5n_h}{2} \pm \frac{n_h}{2} \left[25 - \frac{4m}{n_h} \left(\frac{1 - R_h}{R_h} \right) \right]^{1/2} \end{aligned}$$

But

$$\frac{m}{n_h^2} = \frac{(U_a)^2}{(C_c)^2} \cdot \frac{(C_h)^2}{(U_a)^2} = \left(\frac{C_h}{C_c} \right)^2 = R_h^2 = \frac{1}{R_c^2}$$

so that

$$\alpha_{1,2} = \frac{5n_h}{2} \pm \frac{n_h}{2} \left[25 - 4R_h^2 \left(\frac{1 - R_h}{R_h} \right) \right]^{1/2}$$

or

$$\alpha_{1,2} = \frac{n_h}{2} (5 \pm \lambda) \quad (3.11)$$

where

$$\lambda = [25 - 4R_h(1 - R_h)]^{1/2} \quad (3.12)$$

Designate the particular integral as T_{pi} and by the method of undetermined coefficients let $T_{pi} = P$ so that in eq. (9)

$$m\left(\frac{1 - R_h}{R_h}\right) P = m\left(\frac{t_2}{R_h} - T_1\right)$$

This makes

$$T_{pi} = P = \left[\frac{t_2}{R_h} - T_1 \right] \left[\frac{R_h}{1 - R_h} \right]$$

so that

$$T_{pi} = \frac{t_2 - R_h T_1}{1 - R_h} \quad (3.13)$$

The general solution to eq. (3.9) is the sum of eqs. (3.10) and (3.13)

$$T(x) = C_1 e^{\alpha_1 x} + C_2 e^{\alpha_2 x} + \frac{t_2 - R_h T_1}{1 - R_h} \quad (3.14)$$

where the arbitrary constants, C_1 and C_2 are evaluated from conditions at $x = 0$ and $x = L$. At $x = 0$, $T(x = 0) = T_2$ and at $x = L$, $T(x = L) = T_1$. When these are inserted, in turn, into eq. (3.14), one obtains a pair of linear algebraic equations in the unknowns C_1 and C_2

$$T_2 = C_1 + C_2 + T_{pi}$$

$$T_1 = C_1 e^{\alpha_1 L} + C_2 e^{\alpha_2 L} + T_{pi}$$

where T_{pi} is given by eq. (3.13).

It is only a matter of algebra to show that

$$C_1 = \frac{(T_1 - T_{pi}) - (T_2 - T_{pi})e^{\alpha_2 L}}{e^{\alpha_1 L} - e^{\alpha_2 L}} \quad (3.15a)$$

and

$$C_2 = \frac{(T_2 - T_{pi})e^{\alpha_1 L} - (T_1 - T_{pi})}{e^{\alpha_1 L} - e^{\alpha_2 L}} \quad (3.15b)$$

It is easy to see from eq. (3.1) that

$$R_h = \frac{C_h}{C_c} = \frac{(t_2 - t_1)}{(T_1 - T_2)}$$

so that

$$t_2 = t_1 + R_h(T_1 - T_2)$$

Use of this in eq. (3.13) shows that

$$T_{pi} = \frac{t_1 + R_h(T_1 - T_2) - R_h T_1}{1 - R_h}$$

or

$$T_{pi} = \frac{t_1 - R_h T_2}{1 - R_h} \quad (3.16)$$

indicating two alternative forms for T_{pi} given by eqs. (3.13) and (3.16).

Insertion of eqs. (3.13) and (3.16) in eqs. (3.15) for C_1 and C_2 will yield after some algebra

$$C_1 = \frac{\left(\frac{T_1 - t_2}{1 - R_h}\right) - \left(\frac{T_2 - t_1}{1 - R_h}\right) e^{\alpha_2 L}}{e^{\alpha_1 L} - e^{\alpha_2 L}} \quad (3.17a)$$

and

$$C_2 = \frac{\left(\frac{T_2 - t_1}{1 - R_h}\right) e^{\alpha_1 L} - \left(\frac{T_1 - t_2}{1 - R_h}\right)}{e^{\alpha_1 L} - e^{\alpha_2 L}} \quad (3.17b)$$

Equation (3.14) is an expression for the hot side temperature at any location in the exchanger in terms of the extreme temperatures, t_1 , t_2 , T_1 and T_2 .

Next take eq. (3.5) and set it equal to the derivative of eq. (3.14) noting that C_1 , C_2 and T_{pi} are all known constants.

$$\frac{dT}{dx} = n_h (5T - t_a - t_b - t_c - t_d - t_e) = \alpha_1 C_1 e^{\alpha_1 x} + \alpha_2 C_2 e^{\alpha_2 x} \quad (3.18)$$

At $x = 0$, where $T = T_2$, $t_a = t_1$, $t_b = t_c = t_{bc}$, $t_d = t_e = t_{de}$

$$\frac{dT}{dx} = n_h (5T_2 - t_1 - 2t_{bc} - 2t_{de}) = \alpha_1 C_1 + \alpha_2 C_2 \quad (3.19)$$

and if we subtract eq. (3.4a) from eq. (3.4c) we obtain

$$\frac{dt_a - dt_c}{t_a - t_c} = -\frac{U_a}{C_c} dx = -n_c dx$$

which can be integrated using C_3 as the constant of integration

$$t_a - t_c = C_3 e^{-n_c x}$$

At $x = 0$ where $t_a = t_1$ and $t_c = t_{bc}$

$$t_1 - t_{bc} = C_3$$

or

$$t_{bc} = t_1 - C_3$$

In addition at $x = L$, $t_a = t_{ab}$ and $t_c = t_{cd}$ so that

$$t_{ab} - t_{cd} = C_3 e^{-n_c L}$$

or

$$C_3 = \frac{t_{ab} - t_{cd}}{e^{-n_c L}} = (t_{ab} - t_{cd}) e^{n_c L}$$

This gives a relationship between t_{ab} and t_{bc}

$$t_{bc} = t_1 - (t_{ab} - t_{cd}) e^{N_c} \quad (3.20)$$

where $N_c = n_c L$ can be considered as the total number of transfer units for the cold side.

The same procedure may be employed to find t_{de} .
Subtract eq. (3.4c) from eq. (3.4e)

$$\frac{dt_c - dt_e}{t_c - t_e} = - \frac{Ua}{C_c} dx = - n_c dx$$

and by integration

$$t_c - t_e = C_4 e^{-n_c x}$$

At $x = 0$ where $t_c = t_{bc}$ and $t_e = t_{de}$

$$t_{bc} - t_{de} = C_4$$

or

$$t_{de} = t_{bc} - C_4$$

At $x = L$ where $t_c = t_{cd}$ and $t_e = t_2$

$$t_{cd} - t_2 = C_4 e^{-n_c L}$$

and again with $n_c L = N_c$

$$C_4 = (t_{cd} - t_2) e^{N_c}$$

and

$$t_{de} = t_{bc} - (t_{cd} - t_2) e^{N_c} \quad (3.21)$$

As before subtract eq. (3.4b) from eq. (3.4d)

$$\frac{dt_b - dt_d}{t_b - t_d} = \frac{U_a}{C_c} dx = n_c dx$$

and by integrating find that

$$t_b - t_d = C_5 e^{n_c x}$$

at $x = 0$, $t_b = t_{bc}$ and $t_d = t_{de}$ so that

$$t_{bc} - t_{de} = C_5$$

and at $x = L$, $t_b = t_{ab}$ and $t_d = t_{cd}$. This shows that

$$t_{ab} - t_{cd} = C_5 e^{n_c L}$$

and

$$t_{cd} = t_{ab} - (t_{bc} - t_{de}) e^{N_c} \quad (3.22)$$

where $N_c = n_c L$.

Return to eq. (3.18) and look at the conditions at $x = L$ where $t_a = t_b = t_{ab}$, $t_c = t_d = t_{cd}$, $t_e = t_2$ and $T = T_1$. These conditions in eq. (3.18) give

$$n_h (5T_1 - 2t_{ab} - 2t_{cd} - t_2) = \alpha_1 C_1 e^{\alpha_1 L} + \alpha_2 C_2 e^{\alpha_2 L} \quad (3.23)$$

where again we remember that C_1 and C_2 are known constants.

Now with four equations, eq. (3.20), eq. (3.21), eq. (3.22), and eq. (3.23) and four unknown variables we

can solve for the four variables, t_{ab} , t_{bc} , t_{cd} , and t_e .
Cramer's rule will be used to solve for two of them; t_{bc} and t_{de} .

First arrange eqs. (3.20) to (3.23) in standard form with the unknowns appearing in columns.

$$t_{ab} + t_{bc}e^{-N_c} - t_{cd} = t_1e^{-N_c} \quad (3.20)$$

$$-t_{bc} + t_{cd}e^{N_c} + t_{de} = t_2e^{N_c} \quad (3.21)$$

$$t_{ab} - t_{bc} + t_{cd} + t_{de} = 0 \quad (3.22)$$

$$t_{ab} + t_{cd} = \beta \quad (3.23)$$

$$\text{where } \beta = 1/2(5T_1 - t_2 - \frac{1}{n_h}(\alpha_1 C_1 e^{\alpha_1 L} + \alpha_2 C_2 e^{\alpha_2 L}))$$

If

$$AX = B = \begin{bmatrix} 1 & e^{-N_c} & -1 & 0 \\ 0 & -1 & e^{N_c} & 1 \\ 1 & e^{N_c} & -1 & e^{N_c} \\ 1 & 0 & 1 & 0 \end{bmatrix} \begin{bmatrix} t_{ab} \\ t_{bc} \\ t_{cd} \\ t_{de} \end{bmatrix} = \begin{bmatrix} t_1 e^{-N_c} \\ t_2 e^{N_c} \\ 0 \\ \beta \end{bmatrix}$$

The solution for t_{bc} and t_{de} is

$$t_{bc} = \frac{\det A_{bc}}{\det A}, \quad t_{de} = \frac{\det A_{de}}{\det A}$$

where, A_{bc} and A_{de} are the matrices obtained by replacing the entries in the second and fourth columns of A by the entries in matrix B .

Compute the determinant, $\det A$ of matrix A (the matrix of coefficients)

$$\det A = \begin{vmatrix} 1 & e^{-N_c} & -1 & 0 \\ 0 & -1 & e^{N_c} & 1 \\ 1 & e^{N_c} & -1 & e^{N_c} \\ 1 & 0 & 1 & 0 \end{vmatrix}$$

$$\det A = -(e^{N_c} + 2e^{-N_c})$$

Since $\det A \neq 0$, the system should have a unique solution. Continue by computing $\det A_{bc}$ and $\det A_{de}$. Thus

$$\det A_{bc} = \begin{vmatrix} 1 & t_1 e^{-N_c} & -1 & 0 \\ 0 & t_2 e^{N_c} & e^{N_c} & 1 \\ 1 & 0 & -1 & e^{N_c} \\ 1 & \beta & 1 & 0 \end{vmatrix}$$

$$= e^{2N_c}(\beta - 2t_2) - t_1(e^{N_c} + 2e^{-N_c})$$

and

$$\det A_{de} = \begin{vmatrix} 1 & e^{-N_c} & -1 & t_1 e^{-N_c} \\ 0 & -1 & e^{N_c} & t_2 e^{N_c} \\ 1 & -e^{N_c} & -1 & 0 \\ 1 & 0 & 1 & \beta \end{vmatrix}$$

$$= (e^{2N_c} + 1)(\beta - 2t_2) - t_1(e^{N_c} + 2e^{-N_c})$$

Therefore

$$t_{bc} = \frac{\det A_{bc}}{\det A} = \frac{e^{2N_c}(\beta - 2t_2) - t_1(e^{N_c} + 2e^{-N_c})}{-(e^{N_c} + 2e^{-N_c})}$$

or

$$t_{bc} = t_1 - \frac{e^{N_c}(\beta - 2t_2)}{1 + 2e^{-2N_c}} \quad (3.24)$$

and

$$t_{de} = \frac{\det A_{de}}{\det A} = \frac{(e^{2N_c} + 1)(\beta - 2t_2) - t_1(e^{N_c} + 2e^{-N_c})}{-(e^{N_c} + 2e^{-N_c})}$$

or

$$t_{de} = t_1 - \left(\frac{(e^{2N_c} + 1)(\beta - 2t_2)}{e^{N_c} + 2e^{-N_c}} \right) \quad (3.25)$$

Then with eq. (3.24) and (3.25) in eq. (3.19) and some algebraic manipulation

$$\alpha_1 C_1 + \alpha_2 C_2 = n_h [5(T_2 - t_1) + 2 \left(\frac{(\beta - 2t_2)(2e^{N_c} + e^{-N_c})}{(1 + 2e^{-2N_c})} \right)] \quad (3.26)$$

Equation (3.26) is similar to the one derived by O'Hare [Ref. 1: eq. (22)]. At this point he continued to attempt a closed form solution for ϵ as a function of R and N_{tu} . It is to be noted, however, that he was unable to obtain the solution because of the presence of terms deriving from dimensional parameters such as n_h with dimensions m^{-1} [Ref. 1: pp. 46]. Since n_h is present in eq. (3.26), it must be concluded that a further attempt at an analytic solution for the effectiveness of the 1-5 exchanger will suffer a similar fate and be also unachievable.

This conclusion should be obvious because, when dealing with an equation derived from n equations with $n+1$ unknowns, one cannot create an additional equation by merely multiplying one of the n equations by a constant. This leads to a linearly dependent set which has no unique solution.

Thus, after observing that O'Hare's attempt failed, this thesis, like O'Hare's, turns to a numerical analysis to achieve the requisite objective.

IV. NUMERICAL AND COMPUTER ANALYSIS

As O'Hare discovered with the 1-3 heat exchanger [Ref. 1], an analytic solution for effectiveness as a function of the capacity rate ratio, R , and N_{tu} was also unattainable for the 1-5 exchanger. Hence, an alternate approach had to be taken and this involved utilizing a finite-difference thermal analyzer combined with a linearizing scheme for the solution of a set of nonlinear algebraic equations [Ref. 14]. This thermal analyzer has been employed to provide solutions for temperature that lead to effectiveness, ϵ , value for the 1-5:3C and 1-5:3P heat exchangers as a function of R and N_{tu} .

A. THERMAL ANALYZER TVSSI

The computer program TVSSI used in the development of the $\epsilon = f(R, N_{tu})$ graphs for the 1-5 heat exchanger [Ref. 1: Appendix A], was adapted from TVSS2 listed by Kern and Kraus [Ref. 14: Appendix C]. This adaptation consisted of modifying TVSS2 to compute solutions in the SI system and accept an input file specifically designed for the 1-5 heat exchanger. This program also had to be adapted to the IBM 3033 AP system. The program utilizes the Cholesky decomposition scheme, and because of the linearization of the radiation terms (not used in this study) the program is iterative.

B. DEVELOPMENT OF THE 1-5:3C and 1-5:3P HEAT-EXCHANGER MODELS

As indicated in the foregoing, TVSSI uses an input file to generate a solution for temperatures that will lead to the sought after effectiveness as a function of R and N_{tu} . This input file is created by a program which requires an input of given capacity rates (hot and cold), overall coefficient, surface area and inlet stream temperatures (hot and cold) values.

This required the development of a program which created such a file. O'Hare [Ref. 1: pp. 53-55] first developed a program using the 1-4 heat exchanger that would create an input file for TVSSI. He compared the effectiveness from the computer generated results and a known analytic solution of effectiveness developed by Kraus and Kern [Ref. 8]. Once O'Hare established confidence in his results, he proceeded to develop a program which would create an input file for the 1-3 exchanger. In this study, a similar technique was used to develop a computer program for the 1-5:3C and 1-5:3P heat exchangers. These programs are called NTU53C and NTU53P (see Appendices A and B) and, in them, the following parameters and techniques were utilized.

1. 300 nodes were used.
2. The initial temperature for the computer to begin the iterative process was set at 200°C.
3. An eventual accuracy of .05 between the final and next to last iterations was used.

4. A radiation coefficient convergence factor of 0.66667 between iterations was used. This is required by the program even if radiation is not considered as a node.
5. The maximum number of iterations that the computer was allowed to perform was set at 12.
6. A damping factor of .8 was set as an initial damping based on the number of non-linear terms in all of the node equations.

With the values of C_h , C_c , U , A , T_1 and t_1 set, the input is set and an input file for TVSSI was generated. In this file all node equations and internode conductance values were determined. This program specified the nodes that interact with each other and the methods by which the thermal interaction takes place such as in the forced convection and fluid flow modes.

Both programs make use of the fact that each term in a node equation shows three things. The first is the node that is coupled for heat flow with the node in question. The second is the method of heat flow between the nodes. In this case, forced convection and fluid flow are used. Finally, the node equation shows the magnitude of the internode heat flow. Here all the pieces of information are collected and presented for use by TVSSI as an input file with all items in the proper format.

It is the output values of both NTU53C and NTU53P (a typical result is shown in Appendix C) that are used by the thermal analyzer (as an input file) to determine

the temperatures T_2 and t_2 for the specific set of given initial parameters C_h , C_c , R , A , T_1 , and t_1 .

C. SCOPE OF COMPUTER ANALYSIS

With the development of NTU53C and NTU53P computer programs, the files that they generated could then be used to solve for temperatures which in turn could yield effectiveness values for a given R and N_{tu} . Of course, it must be realized that many computer runs are required to generate enough data to ensure confidence in the results which cover a wide range of capacity rate ratios and N_{tu} values.

To efficiently expedite the computer task, the Multiple Virtual System (MVS) with Job Entry Subsystem and Networking (JES3) was employed. The MVS coupled with JES3 is more commonly referred to as batch processing. Based on trial and error, it was determined that in order to build a solid data base, eleven different values for effectiveness were needed to best represent a particular value of R . Thus, a range of R from $R = 0.01$ to 1.0 was used. Due to the enormous amount of computer time required to solve a 300 node problem, R increments of 0.05 were used for this study and this thesis reports on this basis. In all, 42 curves for both the 1-5:3C and 1-5:3P heat exchangers were required. With this change in the increments between R values (O'Hare's work showed that an increment in R of 0.01 was not necessary), a linear interpolation was found to be acceptable to less than 0.02 percent error.

TVSSI was slightly modified in accordance with the appropriate guidelines of the job control language (JCL) needed to run on the batch processing system. These modifications were few and were needed only at the beginning and end of TVSSI. The modified version of TVSSI has been called TVCOUNT with changes shown in [Ref. 1: Appendix F]. It was TVCOUNT that was then used to activate TVSSI.

It also became necessary to modify the two input file programs NTU53P and NTU53C so that they needed to be compiled only once. They were then loaded in a library file to be used when called by another program. New programs utilizing the batch system were written that could easily be loaded with the appropriate input data for a specific R value. These, which are referred to as "sister programs," were used to go from the library file to TVSSI and cause TVSSI to be executed eleven times under TVCOUNT covering the desired range of N_{tu} for a specific R value. The modified input files and their associated "sister execution programs are found in Appendices D through G.

A flow chart of how all of the foregoing is accomplished is provided by O'Hare [Ref. 1: Figures 4.4 and 4.5]. It is noted that in these figures, TVSSI is referred to as TVSSIA through TVSSIV. These are the same programs as TVSSI but for bookkeeping purposes by the computer they are labeled A through V.

D. INTERPRETATION OF GRAPHS

Once all the data had been collected and the effectiveness for a given R and N_{tu} values had been computed, plots of effectiveness as a function of N_{tu} for the entire range of R values were plotted for both parallel and counterflow heat exchangers. These plots are shown in Appendices H and I.

It may be observed that for a particular value of R , the plot of effectiveness as a function of N_{tu} indicates that the 1-5-3C exchanger outperforms the 1-4, 1-3:2P and the 1-5:3P exchangers but not the 1-3:2C exchanger. This may be explained by the quite apparent fact that the 1-5:3C exchanger has one more counterflow pass than the 1-4 exchanger. Indeed, this argument can be extended to the fact that the 1-5:3C has one more parallel flow pass than the 1-3:2C. Figure 4.1. displays the graphical picture to support this contention.

EFFECTIVENESS VS. NTU FOR $R=0.5$

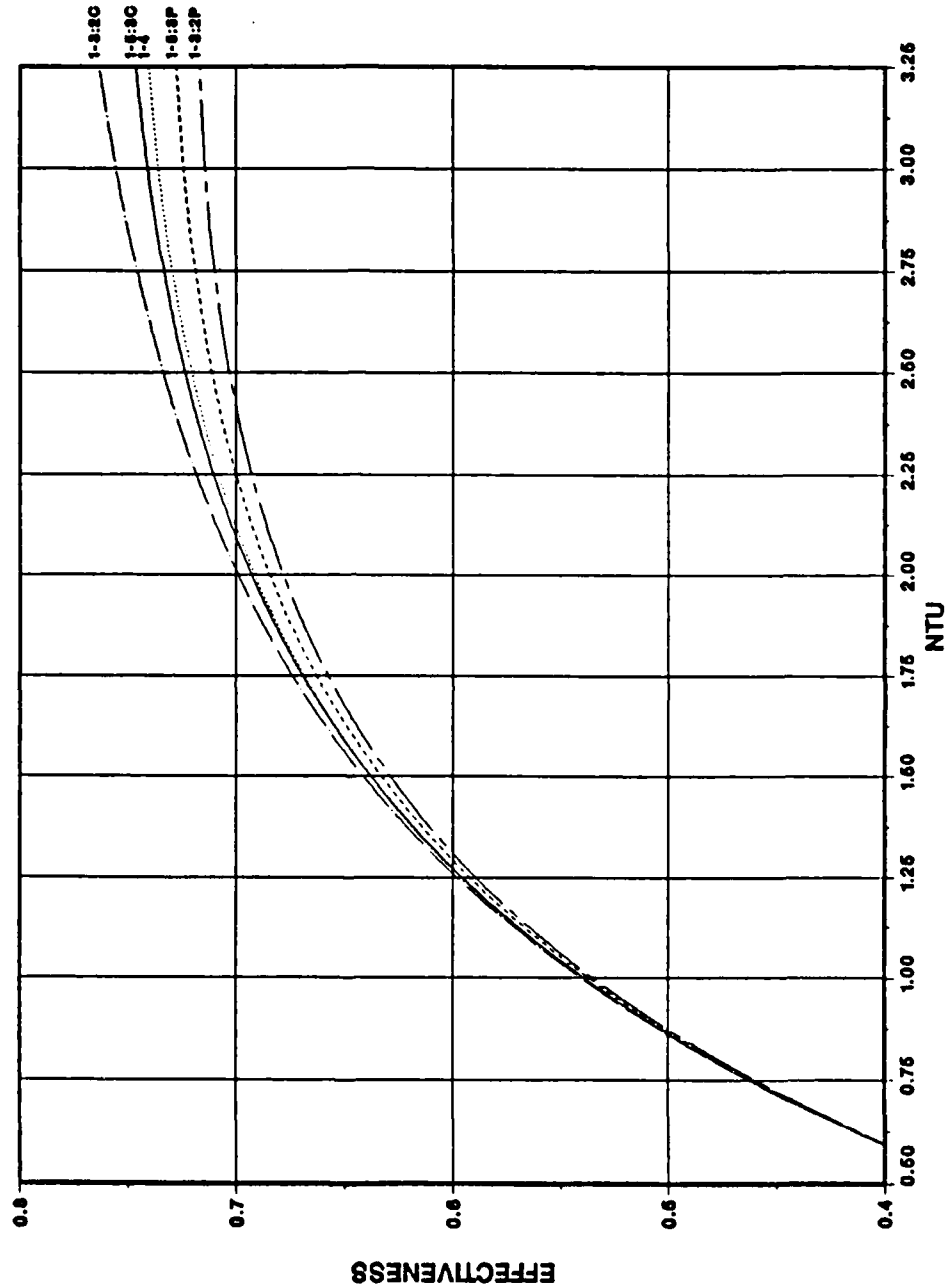


Figure 4.1 Comparison of Analytical (1-4) and Computer Results (1-3:2C and 1-3:2P) to Computer Results (1-5:3C and 1-5:3P) at $R = 0.5$

V. POLYNOMIAL REGRESSION

A. DEVELOPMENT OF POLYNOMIAL EQUATIONS

The empirical data obtained for the two 1-5 heat exchangers was designed to cover an extensive range of R values varying from 0.01 to 1.0 in increments of 0.05. As discussed earlier in Section IV, the data obtained at a specific value of R is the computer evaluated result of the effectiveness, for an associated N_{tu} value. With this accomplished, it then becomes possible to graph separate curves for each of the different R values as shown in Appendices H and I. Through a polynomial regression technique, as discussed in this section, it is also possible to develop implicit equations for the curves with $\epsilon = f(N_{tu}, R)$. It is also apparent from an inspection of the graphical representation of the empirical data in Appendices H and I, that the curves conform to a high degree polynomial. However, further analytical investigation is needed to ascertain the exact order of the polynomial terms. This investigation will not only lead to the order of the polynomial, but to the specific equation for each curve.

By use of polynomial regression, the least-squares method can be readily extended to best fit the data to the m^{th} -degree for the polynomial

$$y = A_0 + A_1x + A_2x^2 + \dots A_mx^m \quad (5.1)$$

with the error defined by

$$e_i = D_i - y_i = D_i - A_0 - A_1x - A_2x_i^2 - \dots - A_mx_i^m$$

where D_i represents the empirical data value corresponding to x_i , x_i being free of error.

The objective is to minimize the sum of the squares of the residuals, S_r ,

$$S_r = \sum_{i=1}^m e_i^2 = \sum_{i=1}^m (D_i - A_0 - A_1x_i - A_2x_i^2 + \dots - A_mx_i^m)^2 \quad (5.2)$$

Because at a minimum, the partial derivatives $\partial S_r / \partial A_0$, $\partial S_r / \partial A_1 \dots \partial S_r / \partial A_m$ vanish, after taking the derivative of S_r with respect to each of the coefficients of the polynomial, it can be seen that

$$\frac{\partial S_r}{\partial A_0} = 0 = -2 \sum (D_i - A_0 - A_1x_i - A_2x_i^2 - \dots - A_mx_i^m)$$

$$\frac{\partial S_r}{\partial A_1} = 0 = -2 \sum x_i (D_i - A_0 - A_1x_i - A_2x_i^2 - \dots - A_mx_i^m)$$

$$\frac{\partial S_r}{\partial A_2} = 0 = -2 \sum x_i^2 (D_i - A_0 - A_1x_i - A_2x_i^2 - \dots - A_mx_i^m)$$

$$\vdots$$

$$\frac{\partial S_r}{\partial A_m} = 0 = -2 \sum x_i^m (D_i - A_0 - A_1x_i - A_2x_i^2 - \dots - A_mx_i^m)$$

Then by dividing by -2 and rearranging we obtain

$$A_0 N + A_1 \sum x_i + A_1 x_i^2 + \dots + A_m \sum x_i^m = \sum D_i$$

$$A_0 \sum x_i + A_1 \sum x_i^2 + A_2 \sum x_i^3 + \dots + A_m \sum x_i^{m+1} = \sum x_i D_i$$

$$A_0 \sum x_i^2 + A_1 \sum x_i^3 + A_2 \sum x_i^4 + \dots + A_m \sum x_i^{m+2} = \sum x_i^2 D_i$$

$$\begin{array}{ccccccc} \cdot & \cdot & \cdot & \cdot & \cdot & \cdot & \cdot \\ \cdot & \cdot & \cdot & \cdot & \cdot & \cdot & \cdot \\ \cdot & \cdot & \cdot & \cdot & \cdot & \cdot & \cdot \end{array}$$

$$A_0 \sum x_i^m + A_1 \sum x_i^{m+1} + A_2 \sum x_i^{m+2} + \dots + A_m \sum x_i^{2m} = \sum x_i^m D_i$$

where all summations are from $i=1$ through n . All of the foregoing $m+1$ equations are linear and have $m+1$ unknowns: $A_0, A_1, A_2, \dots, A_m$. The coefficients of the unknowns can be calculated directly from the observed data. Thus, the problem of determining a least-squares polynomial of degree m is equivalent to solving a system of $m+1$ simultaneous linear equations. Putting the equations in matrix form yields

$$\begin{bmatrix} N & \sum x_i & \sum x_i^2 & \sum x_i^3 & \dots & \sum x_i^m \\ \sum x_i & \sum x_i^2 & \sum x_i^3 & \sum x_i^4 & \dots & \sum x_i^{m+1} \\ \sum x_i^2 & \sum x_i^3 & \sum x_i^4 & \sum x_i^5 & \dots & \sum x_i^{m+2} \\ \cdot & \cdot & \cdot & \cdot & \cdot & \cdot \\ \cdot & \cdot & \cdot & \cdot & \cdot & \cdot \\ \cdot & \cdot & \cdot & \cdot & \cdot & \cdot \\ \sum x_i^m & \sum x_i^{m+1} & \sum x_i^{m+2} & \sum x_i^{m+3} & \dots & \sum x_i^{2m} \end{bmatrix} A = \begin{bmatrix} \sum D_i \\ \sum x_i D_i \\ \sum x_i^2 D_i \\ \cdot \\ \cdot \\ \cdot \\ \sum x_i^m D_i \end{bmatrix}$$

[Ref. 15: pp. 302-309 and Ref. 16: 468-474].

From this point on, one finds that it is best to use a computer to assist in solving the simultaneous equations and this will also help alleviate any ill-conditioning that may otherwise occur. An existing "curvefit" program available through NON-IMSL [Ref. 16] was used although some modifications were made to the original program to best accommodate the goals of this work.

To determine the order of polynomial that should eventually be used, one increases the degree of the approximating polynomial as long as there is a statistically significant decrease in the variance σ^2 , which is computed by

$$\sigma^2 = \frac{\sum e_i^2}{N - m - 1} \quad (5.3)$$

In otherwords, the selection of the optimum degree polynomial is contingent upon a decreasing variance and once the variance begins to increase, the degree of the polynomial becomes too high. For all cases, it was found that the $\epsilon - N_{tu}$ developed curves are of the 5th order.

As shown in Figures 5.1 and 5.2 the computed values of effectiveness vs. N_{tu} for $R = 0.1, 0.5$ and 1.0 for both flow arrangements, (1-5:3P) and (1-5:3C), have been graphed and fitted by a 5th degree polynomial. Because all computed values for effectiveness follow a predictable trend, only a sample of the data covering the whole range of

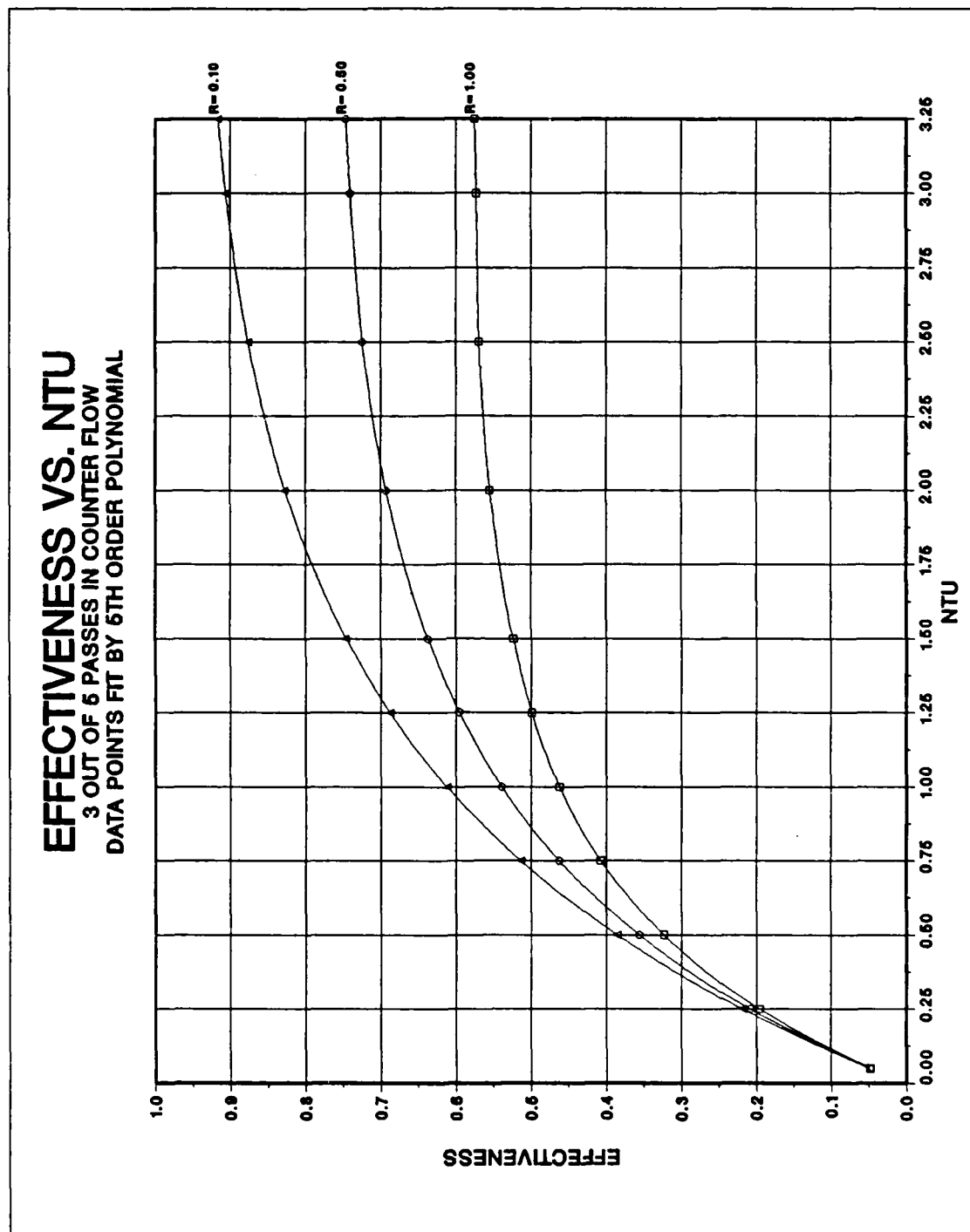


Figure 5.1 1-5:3C Data Fit by a 5th Order Polynomial

EFFECTIVENESS VS. NTU
3 OUT OF 5 PASSES IN PARALLEL FLOW
DATA POINTS FIT BY 5TH ORDER POLYNOMIAL

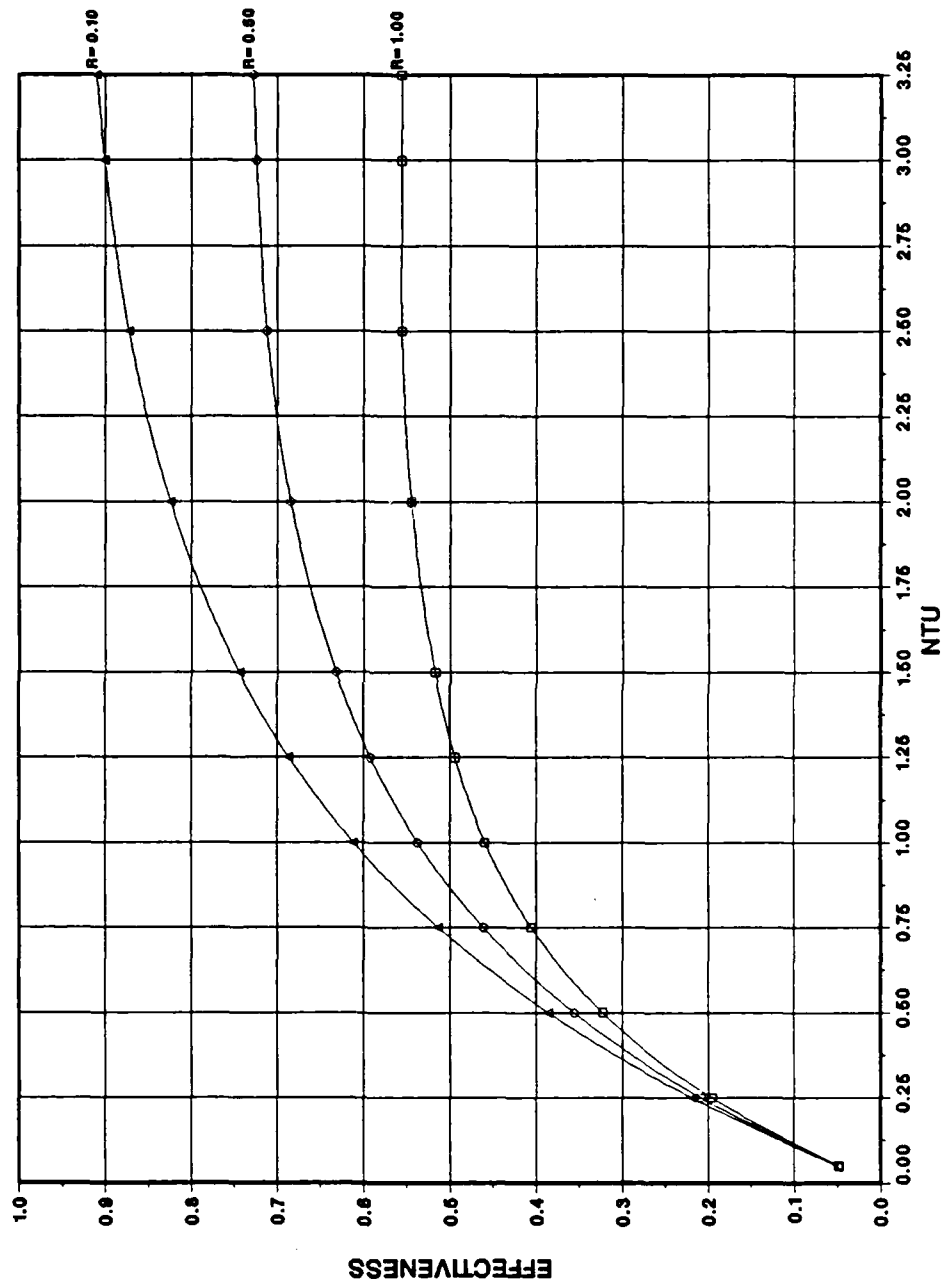


Figure 5.2 1-5:3P Data Fit by a 5th Order Polynomial

values of R have been shown. It is clear that the graphical interpretation strongly backs what is known numerically from the polynomial regression technique. Thus, the relationship for $\epsilon = f(N_{tu}, R)$ can be found explicitly from

$$\epsilon = A_5 N_{tu}^5 + A_4 N_{tu}^4 + A_3 N_{tu}^3 + A_2 N_{tu}^2 + A_1 N_{tu} + A_0 \quad (5.4)$$

where the coefficients A_5 , A_4 , A_3 , A_2 , A_1 , and A_0 relating to a specific value of R are found in Tables 1 and 2 for the (1-5:3C) and (1-5:3P) configurations.

In order to better utilize the coefficients found in Tables 1 and 2, an interactive program has been developed using equation (5.4) and the 1-5 heat exchanger polynomial approximation coefficients. This program was written for the IBM 3033 using the FORTRAN VS compiler (See Appendix J). By entering the values for NTU, R and the type of heat exchanger the effectiveness values are readily obtained directly or by linear interpolation.

An example of how to work with the effectiveness by using the Equation (5.4) follows.

B. NUMERICAL EXAMPLE

1. Statement of Problem

A 1-5:3C heat exchanger uses sea water ($C_p = 4.045$ kJ/kg-°C) at an initial temperature of 20°C to cool engine oil, flowing at 200 kg/s from 60°C to 40°C. The sea water flow rate is 80 kg/s. If the overall heat transfer

coefficient is $40 \text{ W/m}^2\text{°C}$, how much surface area is required in the exchanger?

2. Solution

At an average oil temperature of 50°C , the specific heat is $C_p = 2.004 \text{ kJ/kg-°C}$ and an energy balance gives

$$(WC_p\Delta T)_{\text{sea water}} = (WC_p\Delta T)_{\text{engine oil}}$$

$$(80 \text{ kg/s})(4.045 \text{ kJ/kg-°C})(t_2 - 20)^\circ\text{C}$$

$$= (200 \text{ kg/s})(2.004 \text{ kJ/kg-°C})(60 - 40)^\circ\text{C}$$

$$t_2 = 20 + \frac{200(2.004)(20)}{10(4.045)} = 44.8^\circ\text{C}$$

The number of transfer units is given by $N_{tu} = UA/C_{\min}$. To determine $C_{\min}$ we must compare the products of mass-flow rate and specific heat for sea water and oil.

$$(WC_p)_{\text{sw}} = (80 \text{ kg/s})(4.045 \text{ kJ/kg-°C})$$

$$= 323.6 \text{ kW/°C}$$

$$(WC_p)_{\text{oil}} = (200 \text{ kg/s})(2.004 \text{ kJ/kg-°C})$$

$$= 400.8 \text{ kW/°C}$$

Therefore $C_{\min} = 323.6 \text{ kW/°C}$.

The effectiveness is a function of R and N_{tu} . The capacity rate ratio, R , is

$$R = \frac{C_{\min}}{C_{\max}} = \frac{323.6}{400.8} = 0.8074$$

Because $C_c = C_{\min}$, the required effectiveness is

$$\frac{t_2 - t_1}{T_1 - t_1} = \frac{44.8 - 20}{60 - 20} = 0.6193$$

We must now go to Table 1 for the 1-5:3C arrangement with $R = 0.8$ and $R = 0.85$ and find the coefficients

$R = 0.8$	$R = 0.85$
$A_0 = 3.63419 \times 10^{-3}$	$A_0 = 3.82659 \times 10^{-3}$
$A_1 = 0.93822$	$A_1 = 0.93407$
$A_2 = -0.67053$	$A_2 = -0.67841$
$A_3 = 0.27531$	$A_3 = 0.28109$
$A_4 = -0.60558 \times 10^{-1}$	$A_4 = -0.62088 \times 10^{-1}$
$A_5 = 0.54393 \times 10^{-2}$	$A_5 = 0.55850 \times 10^{-2}$

A trial and error solution (assuming values of N_{tu} and by interpolating) gives a result

$$N_{tu} = 2.352$$

for which

$$A = N_{tu} C_{\min}/U$$

$$A = 19.03 \text{ m}^2$$

3. Observations

The primary observation made here is that by using the 5th order polynomial equation with the appropriate coefficients found in Table 1 or 2, an accurate value for effectiveness can be found thus allowing one to solve for a wide variety of heat exchanger parameters.

By comparing the value for effectiveness just computed with that of the 1-5:3P, 1-3:2P [Ref. 1] and 1-4 to 1-12 even pass exchangers [Ref. 8], the 1-5:3C has a higher effectiveness than all (see Table 3).

From this observation it is evident that the 1-5:3C exchanger outperforms not only the 1-4 to 1-12 even pass arrangements but also its counterpart, the 1-5:3P exchanger for these given values by at least 0.614%.

TABLE 1
1-5:3C COEFFICIENTS

R	$A_0 \times 10^3$	A_1	A_2	A_3	$A_4 \times 10^1$	$A_5 \times 10^2$
.01	0.57463	0.99093	-0.47938	0.13879	-0.23075	0.16779
.05	0.79100	0.98831	-0.49081	0.14654	-0.25068	0.18647
.10	1.08210	0.98622	-0.50716	0.15773	-0.28045	0.21547
.15	1.25311	0.98238	-0.52072	0.16779	-0.30947	0.24635
.20	1.42506	0.97866	-0.53259	0.17545	-0.32772	0.26203
.25	1.33145	0.97670	-0.54709	0.18482	-0.35072	0.28213
.30	1.51081	0.97405	-0.56166	0.19541	-0.38055	0.31252
.35	1.74198	0.97091	-0.57527	0.20542	-0.40903	0.34186
.40	1.84400	0.96879	-0.59067	0.21718	-0.44469	0.38122
.45	2.13420	0.96459	-0.60073	0.22416	-0.46295	0.39861
.50	2.30808	0.96140	-0.61293	0.23322	-0.48933	0.42669
.55	2.57953	0.95713	-0.62234	0.23996	-0.50762	0.44499
.60	2.74755	0.95336	-0.63230	0.24706	-0.52681	0.46391
.65	3.05249	0.94903	-0.64122	0.25366	-0.54530	0.48293
.70	3.19573	0.94580	-0.65184	0.26137	-0.56656	0.50422
.75	3.39253	0.94193	-0.66116	0.26833	-0.58615	0.52431
.80	3.63419	0.93822	-0.67053	0.27531	-0.60558	0.54393
.85	3.82659	0.93407	-0.67841	0.28109	-0.62088	0.55850
.90	3.98221	0.93052	-0.68748	0.28799	-0.64051	0.57874

TABLE 1 (cont'd)
1-5:3C COEFFICIENTS

R	$A_0 \times 10^3$	A_1	A_2	A_3	$A_4 \times 10^1$	$A_5 \times 10^2$
.95	4.26945	0.92609	-0.69496	0.29381	-0.65653	0.59442
1.0	4.40670	0.92259	-0.70365	0.30046	-0.67514	0.61309

TABLE 2
1-5:3P COEFFICIENTS

R	$A_0 \times 10^3$	A_1	A_2	A_3	$A_4 \times 10^1$	$A_5 \times 10^2$
.01	0.52233	0.99152	-0.48055	0.13953	-0.23283	0.16989
.05	0.81101	0.98817	-0.49062	0.14604	-0.24883	0.18421
.10	1.10555	0.98599	-0.50718	0.15721	-0.27865	0.21337
.15	1.14518	0.98309	-0.52246	0.16811	-0.30968	0.24604
.20	1.25862	0.97914	-0.53367	0.17485	-0.32443	0.25741
.25	1.29233	0.97701	-0.54864	0.18464	-0.34902	0.27929
.30	1.43113	0.97558	-0.56664	0.19807	-0.38885	0.32195
.35	1.69053	0.97206	-0.57958	0.20740	-0.41500	0.34854
.40	1.76316	0.96998	-0.59515	0.21912	-0.45054	0.38805
.45	2.10897	0.96559	-0.60498	0.22583	-0.46805	0.40487
.50	2.30583	0.96163	-0.61546	0.23327	-0.48857	0.42594
.55	2.59035	0.95726	-0.62480	0.23985	-0.50625	0.44354
.60	2.77374	0.95331	-0.63434	0.24638	-0.52303	0.45925
.65	2.91148	0.95025	-0.64574	0.25460	-0.54593	0.48260
.70	3.22294	0.94575	-0.65400	0.26039	-0.56053	0.49575
.75	3.38351	0.94231	-0.66425	0.26788	-0.58110	0.51617
.80	3.60234	0.93852	-0.67369	0.27495	-0.60079	0.53606
.85	3.82374	0.93414	-0.68130	0.28045	-0.61487	0.54884
.90	3.91805	0.93133	-0.69231	0.28893	-0.63953	0.57472

TABLE 2 (cont'd)
1-5:3P COEFFICIENTS

R	$A_0 \times 10^3$	A_1	A_2	A_3	$A_4 \times 10^1$	$A_5 \times 10^2$
.95	4.18844	0.92723	-0.70050	0.29533	-0.65754	0.59298
1.0	4.35186	0.92385	-0.71022	0.30310	-0.68037	0.61690

TABLE 3
COMPARISON OF EXAMPLE RESULTS
FOR $N_{tu} = 2.352$ AND $R = 0.8074$

NUMBER OF TUBE PASSES	EFFECTIVENESS
3:2P	.5990
4	.6155
5:3C	.6193
5:3P	.6067
6	.6145
8	.6141
10	.6140
12	.6139

VI. CONCLUSIONS AND RECOMMENDATIONS

A. CONCLUSIONS

The objective of this thesis was to provide effectiveness values for the 1-5:3C and 1-5:3P heat exchangers. Although these objectives were analytically unachievable, they became attainable through a fifth order polynomial approximation from numerical data. The data obtained covers a wide range of capacity rate ratios for values of N_{tu} from 0 to 3.25. With the knowledge of the 1-5 heat exchanger type (1-5:3C or 1-5:3P), size (surface area), the overall heat transfer coefficient and the fluid flow rates, the N_{tu} and capacity rate ratios may be computed and the exchanger effectiveness may then be determined from the appropriate coefficient tables or the effectiveness program provided.

It is indeed obvious that the effectiveness parameter is most useful in performance estimation and analysis for all types of heat exchangers. The work done here pertaining to the 1-5 exchanger is very helpful in constructing a comprehensive picture of the performance attainable for the 1-2 consecutively through the 1-6 for a diverse range of known conditions.

B. RECOMMENDATIONS

With proof in this thesis, and that of O'Hare [Ref. 1], that an odd number of tube passes per shell has a slightly better effectiveness when more than half the tube fluid flows in counterflow to the shell fluid, it is recommended that a feasibility study be conducted with regard to the structural and thermal problems that may arise in manufacturing and designing such heat exchangers.

APPENDIX A

NTU53C COMPUTER GENERATED INPUT ANALYZER PROGRAM

```

C C C THIS IS PROGRAM NTU53C
C C C
C C C IT GENERATES AN INPUT FILE FOR THERMAL ANALYZER TO OBTAIN
C C C 1-5 EFFECTIVENESS-NTU RELATIONSHIP THAT IS NOT AVAILABLE IN
C C C OPEN LITERATURE (3C MEANING TWO PARALLEL PASS AND THREE
C C C COUNTERFLOW PASSES).
C C C
C C DIMENSION COEF(300,6),KCON(300,6),L1(8),L2(3),L3(6),SET2(2),FL4(4)
C C CHARACTER *79 TITLE
C C CHARACTER *12 FNAME
C C DATA IOT,IN,IPR,IWR/6,5,4,8/
C C OPEN PRINTER OUTPUT FILE
C C OPEN(IPR,FILE='PRN' STATUS='NEW',FORM='FORMATTED',IOSTAT=ICK)
C C IF(ICK.NE.0) WRITE(IOT,920)
920 FORMAT(' Trouble opening printer output file' )
C C
C C WRITE(IOT,917)
917 FORMAT(/,Input the title,of this study - 79 columns only.' page',
      &,' This title,will appear',/, at the top of every printed ',
      &' of output:')
C C READ(IN,918) TITLE
918 FORMAT(A79)
C C WRITE(IOT,901)
901 FORMAT(/,INPUT HOT SIDE CAPACITY RATE:')
C C READ(IN,902) CHOT
902 FORMAT(BN,F10.0)
C C WRITE(IOT,903)
903 FORMAT(/,INPUT COLD SIDE CAPACITY RATE:')
C C READ(IN,902) CCLOD
C C WRITE(IOT,904)
904 FORMAT(/,INPUT OVERALL HEAT TRANSFER COEFFICIENT:')
C C READ(IN,902) U
C C WRITE(IOT,905)

```



```

KCON(1,3) = 2004
KCON(1,4) = 2014
KCON(1,5) = 3004
KCON(1,6) = 3015
COEF(1,6) = VALK1
DO 50 I = 1,5
50 COEF(1,I) = VALK3
CC
CC
      NODES 2 TO 50
      DO 75 I = 2,50
      J = 101 - I
      K = 100 + I
      L = 201 - I
      N = I - 1
      M = 200 + I
      MM = 301 - I
      KCON(I,1) = 10*N + 5
      KCON(I,2) = 10*J + 4
      KCON(I,3) = 10*K + 4
      KCON(I,4) = 10*L + 4
      KCON(I,5) = 10*M + 4
      KCON(I,6) = 10*MM + 4
      COEF(I,1) = VALK1
      DO 80 I = 1,5
      COEF(I,I) = VALK3
      COEF(I,II) = VALK3
80 CONTINUE
75 CONTINUE

```

```

CC
CC
      NODE 51
CC

```

```

KCON(51,1) = 3025
KCON(51,2) = 504
COEF(51,1) = VALK2
COEF(51,2) = VALK3

```

```

CC
CC
      NODES 52 TO 300
CC

```

```

      DO 120 I = 52,300
      K = I - 1
      IF(I.GT.100) GO TO 122
      L = I - 50
      M = 2*L - 1
      J = I - M
      GO TO 135
122 IF(I.GT.150) GO TO 124
      J = I - 100
      GO TO 135
124 IF(I.GT.200) GO TO 126
      L = I - 150

```



```

914 FORMAT(6F8.4)
200 CONTINUE
C
DO 250 I=51,300
WRITE(IWR,913) KCON(I,1),KCON(I,2)
WRITE(IWR,914) COEF(I,1),COEF(I,2)
250 CONTINUE
C
CLOSE(IWR,Iostat=ICK)
IF(ICK.NE.0) WRITE(IOT,921)EEX
921 FORMAT(' Trouble closing printer output file' )
C
STOP
END

```

NTU53P COMPUTER GENERATED INPUT ANALYZER PROGRAM

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```

      KCON(1,3) = 1514
      KCON(1,4) = 2504
      KCON(1,5) = 2514
      KCON(1,6) = 3015
      COEF(1,6) = VALK1
      DO 50 I = 1,5
50 COEF(1,I) = VALK3
      CC
      CC
      NODES 2 TO 50
      DO 75 I = 2,50
      J = I + 50
      K = 151 - I
      L = 150 + I
      N = I - 1
      M = 251 - I
      MM = 250 + I
      KCON(I,1) = 10*N + 5
      KCON(I,2) = 10*J + 4
      KCON(I,3) = 10*K + 4
      KCON(I,4) = 10*L + 4
      KCON(I,5) = 10*M + 4
      KCON(I,6) = 10*MM + 4
      COEF(I,1) = VALK1
      DO 80 I,II = 2,6
      COEF(I,II) = VALK3
80 CONTINUE
75 CONTINUE
      CC
      CC
      NODE 51
      KCON(51,1) = 3025
      KCON(51,2) = 14
      COEF(51,1) = VALK2
      COEF(51,2) = VALK3
      CC
      CC
      NODES 52 TO 300
      DO 120 I = 52,300
      K = I - 100
      IF(I.GT.100) GO TO 122
      J = I - 50
      GO TO 135
122 IF(I.GT.150) GO TO 124
      L = I - 100
      M = 2*L - 1
      N = M + 50
      J = I - N
      GO TO 135
124 IF(I.GT.200) GO TO 126

```

```

J = I - 150
GO TO 135
126 IF(I.GT.250) GO TO 128
L = I - 200
M = 2*L - 1
N=M+150
J = I - N
GO TO 135
128 J = I - 250
135 KCON(I,1) = 10*J + 4
KCON(I,2) = 10*K + 5
COEF(I,1) = VALK3
120 COEF(I,2) = VALK2

CC
CC
CC
END OF DATA SETUP
NOW CREATE INPUT FOR ANALYZER

WRITE(IOT, 922)
922 FORMAT(/, 'Enter name of input file, including drive',
& , 'DESIGNATION: ')
READ(IN, 923) FNAME
923 FORMAT(A12)

CC
CC
CC
OPEN INPUT FILE

OPEN(IWR, FILE=FNAME, STATUS='NEW', FORM='FORMATTED', IOSTAT=ICK)
IF(ICK.GT.0)WRITE(IOT,924)
924 FORMAT(/, 'Trouble opening input file')

CC
WRITE(IOT, 925) FNAME
925 FORMAT(/, 'Writing file : ', A14)
919 WRITE(IWR, 919) TITLE
919 FORMAT(1X, A79)
908 WRITE(IWR, 908) (L1(I), I=1, 8)
908 FORMAT(914)
WRITE(IWR, 908) (L2(I), I=1, 3)
WRITE(IWR, 908) (L3(I), I=1, 6)
911 WRITE(IWR, 911) (FL4(1), FL4(2), L4, FL4(3), FL4(4))
911 FORMAT(F8.3, F8.5, I8, F8.5, F8.2)
912 WRITE(IWR, 912) SET2(1), SET2(2)
912 FORMAT(2F8.0)

CC
DO 200 I = 1, 50
WRITE(IWR, 913) (KCON(I, J), J=1, 6)
913 FORMAT(918)
WRITE(IWR, 914) (COEF(I, J), J=1, 6)
914 FORMAT(6F8.4)
200 CONTINUE

CC
DO 250 I=51, 300

```

```

WRITE(IWR,913) KCON(I,1),KCON(I,2)
WRITE(IWR,914) COEF(I,1),COEF(I,2)
C 250 CONTINUE
CLOSE(IWR,Iostat=Ick)
IF(Ick.NE.0) WRITE(IOT,921)EEX
C 921 FORMAT(' Trouble closing printer output file' )
STOP
END

```

APPENDIX C

SAMPLE OUTPUT FROM NTU53C COMPUTER INPUT ANALYZER PROGRAM

R=0.5		NTU=1.0		0		0		0		0.8		125.0		3015	
300	2	0	0	0	0	0	0	0	0	0	0	0	0	0	0
300	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
300	50	0	0	0	0	0	0	0	0	0	0	0	0	0	0
0	0.050	0.6	0.6667	2	6	12	2004	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
200	100	100	1014	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
1004	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
0.5000	15	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	25	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	35	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	45	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	55	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	65	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	75	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	85	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	95	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	105	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	115	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	125	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	135	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	145	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	155	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	165	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	175	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000
250.0000	185	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000	0.5000

250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.195	0.814	0.1204	0.1814	0.2204	0.2814
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.205	0.804	0.1214	0.1804	0.2214	0.2804
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.215	0.794	0.1224	0.1794	0.2224	0.2794
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.225	0.784	0.1234	0.1784	0.2234	0.2784
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.235	0.774	0.1244	0.1774	0.2244	0.2774
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.245	0.764	0.1254	0.1764	0.2254	0.2764
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.255	0.754	0.1264	0.1754	0.2264	0.2754
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.265	0.744	0.1274	0.1744	0.2274	0.2744
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.275	0.734	0.1284	0.1734	0.2284	0.2734
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.285	0.724	0.1294	0.1724	0.2294	0.2724
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.295	0.714	0.1304	0.1714	0.2304	0.2714
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.305	0.704	0.1314	0.1704	0.2314	0.2704
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.315	0.694	0.1324	0.1694	0.2324	0.2694
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.325	0.684	0.1334	0.1684	0.2334	0.2684
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.335	0.674	0.1344	0.1674	0.2344	0.2674
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.345	0.664	0.1354	0.1664	0.2354	0.2664
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.355	0.654	0.1364	0.1654	0.2364	0.2654
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.365	0.644	0.1374	0.1644	0.2374	0.2644
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.375	0.634	0.1384	0.1634	0.2384	0.2634
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.385	0.624	0.1394	0.1624	0.2394	0.2624
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.395	0.614	0.1404	0.1614	0.2404	0.2614
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.405	0.604	0.1414	0.1604	0.2414	0.2604
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.415	0.594	0.1424	0.1594	0.2424	0.2594
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.425	0.584	0.1434	0.1584	0.2434	0.2584
250.0000	0.5000	0.5000	0.5000	0.0000	0.0000
250.435	0.574	0.1444	0.1574	0.2444	0.2574

250.0000	0.5000	0.5000	0.0000	0.0000
445	364	1454	0.2454	0.2564
250.0000	0.5000	0.5000	0.0000	0.2000
455	554	1464	0.2464	0.2554
250.0000	0.5000	0.5000	0.0000	0.2000
465	544	1474	0.2474	0.2544
250.0000	0.5000	0.5000	0.0000	0.2000
475	534	1484	0.2484	0.2534
250.0000	0.5000	0.5000	0.0000	0.2000
485	524	1494	0.2494	0.2524
250.0000	0.5000	0.5000	0.0000	0.2000
495	514	1504	0.2504	0.2514
250.0000	0.5000	0.5000	0.0000	0.2000
3025	504	0.5000	0.0000	0.0000
125.0000	0.5000			
494	515			
0.5000	125.0000			
484	525			
0.5000	125.0000			
474	535			
0.5000	125.0000			
464	545			
0.5000	125.0000			
454	555			
0.5000	125.0000			
444	565			
0.5000	125.0000			
434	575			
0.5000	125.0000			
424	585			
0.5000	125.0000			
414	595			
0.5000	125.0000			
404	605			
0.5000	125.0000			
394	615			
0.5000	125.0000			
384	625			
0.5000	125.0000			
374	635			
0.5000	125.0000			
364	645			
0.5000	125.0000			
354	655			
0.5000	125.0000			
344	665			
0.5000	125.0000			
334	675			
0.5000	125.0000			
324	685			

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314 695
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304 705
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284 725
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274 735
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244 765
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224 785
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214 795
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204 805
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194 815
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184 825
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174 835
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74 935

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14 995
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14 1005
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24 1015
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44 1035
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74 1065
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104 1095
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114 1105
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124 1115
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134 1125
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144 1135
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154 1145
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164 1155
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174 1165
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184 1175
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194 1185

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204 1195
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214 1205
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224 1215
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234 1225
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244 1235
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254 1245
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264 1255
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274 1265
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284 1275
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294 1285
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324 1315
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394 1385
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414 1405
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414 1595
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404 1605
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374 1635
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364 1645
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354 1655
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214 1795
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204 1805
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194 1815
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184 1825
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174 1835
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164 1845
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154 1855
0.5000125.0000
144 1865
0.5000125.0000
134 1875
0.5000125.0000
124 1885
0.5000125.0000
114 1895
0.5000125.0000
104 1905
0.5000125.0000
94 1915
0.5000125.0000
84 1925
0.5000125.0000
74 1935

0.5000125.0000
64 1945
0.5000125.0000
54 1955
0.5000125.0000
44 1965
0.5000125.0000
34 1975
0.5000125.0000
24 1985
0.5000125.0000
14 1995
0.5000125.0000

APPENDIX D

MODIFIED NTU53C PROGRAM USED TO RUN ON BATCH SYSTEM

```

//HESS JOB (2054,0267), 'NTU53C', CLASS=B
//*MAIN ORG=NPVGM1.2054P,SYSTEM=SY2,
// EXEC FORTVCL,PARM.LKED= LIST,MAP,
//FORT.SYSIN DD*
C THIS IS PROGRAM NTU53C
C
C IT GENERATES AN INPUT FILE FOR THERMAL ANALYZER TO OBTAIN
C 1-5 EFFECTIVENESS-NTU RELATIONSHIP THAT IS NOT AVAILABLE IN
C OPEN LITERATURE (3C MEANING TWO PARALLEL PASS AND THREE
C COUNTERFLOW PASSES).
C
C INTEGER O,P
C DIMENSION COEF(300,6),KCON(300,6),L1(8),L2(3),L3(6),SET2(2),FL4(4)
C 1,CHOT(22,22),CCLD(22,22),U(22,22),SURFTO(22,22),THOTIN(22,22),TCLD
C 2IN(22,22),TITLE(22,22),FNAME(22,22)
C
C CHARACTER *25 TITLE
C CHARACTER *25 FNAME
C
C DO 7 O=1,21,2
C P=O+1
C READ(1,900) CHOT(O,1),CCLD(O,2),U(O,3),SURFTO(O,4),THOTIN(O,5),TCL
C 1DIN(O,6)
C 900 FORMAT(2F10.0,F10.5,3F10.0)
C 918 READ(1,918) TITLE(P,1),FNAME(P,2)
C FORMAT(2A25)
C OPEN OUTPUT FILE
C OPEN(2,FILE=FNAME(P,2),FORM='FORMATTED')
C
C VALK1 = CHOT(O,1)
C VALK2 = CCLD(O,2)
C VALK3 = U(O,3)*SURFTO(O,4)/250.
C TINIT = 125.
C
C FRONT END
C
C L1(1) = 300
C L1(2) = 2
C DO 10 I=3,8
C 10 L1(I) = 0

```

```

C      DO 20 I=1,3
C      20 L2(I) = 0

C      L3{1} = 300
C      L3{2} = 50
C      L3{3} = 6
C      L3{4} = 2
C      L3{5} = 4
C      L3{6} = 6

C      FL4{1} = .05
C      FL4{2} = .66667
C      FL4{3} = .8
C      FL4{4} = TINIT
C      L4 = 12

C      CONSTANT TEMPERATURES
C      SET2{1} = THOTIN(0,5)
C      SET2{2} = TCLDIN(0,6)

C      READY FOR INPUT SET 4
C      NODE 1
C      KCON{1,1} = 1004
C      KCON{1,2} = 1014
C      KCON{1,3} = 2004
C      KCON{1,4} = 2014
C      KCON{1,5} = 3004
C      KCON{1,6} = 3015
C      COEF{1,6} = VALK1
C      DO 50 I = 1,5
C      50 COEF(1,I) = VALK3

C      NODES 2 TO 50
C      DO 75 I = 2,50
C      J = 101 - I
C      K = 100 + I
C      L = 201 - I
C      N = I - 1
C      M = 200 + I
C      MM = 301 - I
C      KCON{I,1} = 10*N + 5
C      KCON{I,2} = 10*J + 4
C      KCON{I,3} = 10*K + 4
C      KCON{I,4} = 10*L + 4
C      KCON{I,5} = 10*M + 4

```

```

      KCON(I,6) = 10*MM + 4
      COEF(I,1) = VALK1
      DO 80 I1 = 2,6
      COEF(I,I1) = VALK3
80 CONTINUE
75 CONTINUE

```

```

C
C
C

```

```

      KCON(51,1) = 3025
      KCON(51,2) = 504
      COEF(51,1) = VALK2
      COEF(51,2) = VALK3

```

```

C
C
C

```

```

      NODES 52 TO 300

```

```

      DO 120 I = 52,300
      K = I - 1
      IF(I.GT.100) GO TO 122
      L = I - 50
      M = 2*L - 1
      J = I - M
      GO TO 135
122 IF(I.GT.150) GO TO 124
      J = I - 100
      GO TO 135
124 IF(I.GT.200) GO TO 126
      L = I - 150
      M = 2*L - 1
      N = M + 100
      J = I - N
      GO TO 135
126 IF(I.GT.250) GO TO 128
      J = I - 200
      GO TO 135
128 L = I - 250
      M = 2*L - 1
      N = M + 200
      J = I - N
135 KCON(I,1) = 10*J + 4
      KCON(I,2) = 10*K + 5
      COEF(I,1) = VALK3
      COEF(I,2) = VALK2
120 CONTINUE

```

```

C
C
C
C
      END OF DATA SETUP
      NOW CREATE INPUT FOR ANALYZER
      WRITE(2,919) TITLE(P,1)
919 FORMAT(IX,A25)
      WRITE(2,908)(LI(I),I=1,8)

```

```

908 FORMAT(9I4)
WRITE(2,908) (L2(I), I=1,3)
WRITE(2,908) (L3(I), I=1,6)
WRITE(2,911) FL4(1), FL4(2), L4, FL4(3), FL4(4)
911 FORMAT(F8.3, F8.5, I8, 2F8.1)
WRITE(2,912) SET2(1), SET2(2)
912 FORMAT(2F8.0)
C
DO 200 I = 1, 50
WRITE(2,913) (KCON(I,J), J=1,6)
913 FORMAT(9I8)
WRITE(2,914) (COEF(I,J), J=1,6)
914 FORMAT(6F8.4)
200 CONTINUE
C
DO 250 I=51, 300
WRITE(2,913) KCON(I,1), KCON(I,2)
WRITE(2,914) COEF(I,1), COEF(I,2)
250 CONTINUE
C
7 CONTINUE
STOP
END
/*
//LKED.SYSLMOD DD DISP=SHR, DSN=NAME=MSS.S2054.LOADLIB
//LKED.SYSIN DD
//NAME NTU53C(R)
/*
//

```

APPENDIX E

MASTER EXECUTION PROGRAM FOR NTU53C AND TVCOUNT

```
//HESS30C JOB (2054 0267) 'L E HESS', CLASS=P
//*MAIN ORG=NPVMI.2054P, LINES=(5000,W)
//*FORMAT PR, DDNAME=, DEST=LOCAL
//EXEC FORTVG, PROG=NTU53C, LIB='MSS.S2054.LOADLIB'
//GO.TVSSIA
//DD DISP=(NEW,PASS) DSN=&TVSSIA,
//UNIT=SYSDA, SPACE=(CYL(2,2))
//DCB=(RECFM=FB, LRECL=80, BLKSIZE=6160)
//DD DISP=(NEW,PASS) DSN=&TVSSIB,
//UNIT=SYSDA, SPACE=(CYL(2,2))
//DCB=(RECFM=FB, LRECL=80, BLKSIZE=6160)
//GO.TVSSIC
//DD DISP=(NEW,PASS) DSN=&TVSSIC,
//UNIT=SYSDA, SPACE=(CYL(2,2))
//DCB=(RECFM=FB, LRECL=80, BLKSIZE=6160)
//GO.TVSSID
//DD DISP=(NEW,PASS) DSN=&TVSSID,
//UNIT=SYSDA, SPACE=(CYL(2,2))
//DCB=(RECFM=FB, LRECL=80, BLKSIZE=6160)
//GO.TVSSIE
//DD DISP=(NEW,PASS) DSN=&TVSSIE,
//UNIT=SYSDA, SPACE=(CYL(2,2))
//DCB=(RECFM=FB, LRECL=80, BLKSIZE=6160)
//GO.TVSSIF
//DD DISP=(NEW,PASS) DSN=&TVSSIF,
//UNIT=SYSDA, SPACE=(CYL(2,2))
//DCB=(RECFM=FB, LRECL=80, BLKSIZE=6160)
//GO.TVSSIG
//DD DISP=(NEW,PASS) DSN=&TVSSIG,
//UNIT=SYSDA, SPACE=(CYL(2,2))
//DCB=(RECFM=FB, LRECL=80, BLKSIZE=6160)
//GO.TVSSIH
//DD DISP=(NEW,PASS) DSN=&TVSSIH,
//UNIT=SYSDA, SPACE=(CYL(2,2))
//DCB=(RECFM=FB, LRECL=80, BLKSIZE=6160)
//GO.TVSSII
//DD DISP=(NEW,PASS) DSN=&TVSSII,
//UNIT=SYSDA, SPACE=(CYL(2,2))
//DCB=(RECFM=FB, LRECL=80, BLKSIZE=6160)
//GO.TVSSIJ
//DD DISP=(NEW,PASS) DSN=&TVSSIJ,
//UNIT=SYSDA, SPACE=(CYL(2,2))
//DCB=(RECFM=FB, LRECL=80, BLKSIZE=6160)
//GO.TVSSIK
//DD DISP=(NEW,PASS) DSN=&TVSSIK,
//UNIT=SYSDA, SPACE=(CYL(2,2))
//DCB=(RECFM=FB, LRECL=80, BLKSIZE=6160)
//GO.FT01F001 DD *
//NTU=0.05 R=0.30 COUNTER TVSSIA
//NTU=0.25 R=0.30 COUNTER TVSSIB
//NTU=0.25 R=0.30 COUNTER TVSSIB
//NTU=0.25 R=0.30 COUNTER TVSSIB
```

100.
100.
100.

200.
200.
200.

15.
15.
15.

0.25000
1.25000
2.50000

NTU=0.50	R=0.30	COUNTER	TVSSIC	15.	200.	100.
250.		75.0	3.75000			
NTU=0.75	R=0.30	COUNTER	TVSSID	15.	200.	100.
250.		75.0	5.00000			
NTU=1.00	R=0.30	COUNTER	TVSSIE	15.	200.	100.
250.		75.0	6.25000			
NTU=1.25	R=0.30	COUNTER	TVSSIF	15.	200.	100.
250.		75.0	7.50000			
NTU=1.50	R=0.30	COUNTER	TVSSIG	15.	200.	100.
250.		75.0	10.00000			
NTU=2.00	R=0.30	COUNTER	TVSSIH	15.	200.	100.
250.		75.0	12.50000			
NTU=2.50	R=0.30	COUNTER	TVSSII	15.	200.	100.
250.		75.0	15.00000			
NTU=3.00	R=0.30	COUNTER	TVSSIJ	15.	200.	100.
250.		75.0	16.25000			
NTU=3.25	R=0.30	COUNTER	TVSSIK	15.	200.	100.

```

// STEPA EXEC FORTVG, PROG=TVSSIIAC, LIB='MSS.S2054.LOADLIB'
//GO.FT01F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT02F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT09F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT10F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT03F001 DD DUMMY
//GO.FT04F001 DD DISP=(OLD,DELETE), UNIT=SYSDA, DSN=&TVSSIA
//GO.FT08F001 DD SYSOUT=A, DCB=RECFM=FBA
// STEPB EXEC FORTVG, PROG=TVSSIIAC, LIB='MSS.S2054.LOADLIB'
//GO.FT01F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT02F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT09F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT10F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT03F001 DD DUMMY
//GO.FT04F001 DD DISP=(OLD,DELETE), UNIT=SYSDA, DSN=&TVSSIB
//GO.FT08F001 DD SYSOUT=A, DCB=RECFM=FBA
// STEPC EXEC FORTVG, PROG=TVSSIIAC, LIB='MSS.S2054.LOADLIB'
//GO.FT01F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT02F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT09F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT10F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT03F001 DD DUMMY
//GO.FT04F001 DD DISP=(OLD,DELETE), UNIT=SYSDA, DSN=&TVSSIC
//GO.FT08F001 DD SYSOUT=A, DCB=RECFM=FBA
// STEPD EXEC FORTVG, PROG=TVSSIIAC, LIB='MSS.S2054.LOADLIB'
//GO.FT01F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT02F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT09F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT10F001 DD UNIT=SYSDA, SPACE=(CYL,(1,1))
//GO.FT03F001 DD DUMMY
//GO.FT04F001 DD DISP=(OLD,DELETE), UNIT=SYSDA, DSN=&TVSSID
//GO.FT08F001 DD SYSOUT=A, DCB=RECFM=FBA

```



```

//GO.FT02F001 DD UNIT=SYSDA,SPACE={CYL,{1,1}}
//GO.FT09F001 DD UNIT=SYSDA,SPACE={CYL,{1,1}}
//GO.FT10F001 DD UNIT=SYSDA,SPACE={CYL,{1,1}}
//GO.FT03F001 DD DUMMY
//GO.FT04F001 DD DISP=(OLD,DELETE),UNIT=SYSDA,DSN=&TVSSIK
//GO.FT08F001 DD SYSOUT=A,DCB=RECFM=FBA
//

```

MODIFIED NTU53P PROGRAM USED TO RUN ON BATCH SYSTEM

91

```

C      DO 20 I=1,3
      20 L2(I) = 0

      L3{1} = 300
      L3{2} = 50
      L3{3} = 6
      L3{4} = 2
      L3{5} = 4
      L3{6} = 6

      FL4{1} = .05
      FL4{2} = .66667
      FL4{3} = .8
      FL4{4} = TINIT
      L4 = 12

C      CONSTANT TEMPERATURES

C      SET2{1} = THOTIN{0,5}
C      SET2{2} = TCLDIN{0,6}

C      READY FOR INPUT SET 4

C      NODE 1

      KCON{1,1} = 514
      KCON{1,2} = 1504
      KCON{1,3} = 1514
      KCON{1,4} = 2004
      KCON{1,5} = 2014
      KCON{1,6} = 3015
      COEF{1,6} = VALK1
      DO 50 I = 1,5
      50 COEF(1,I) = VALK3

C      NODES 2 TO 50

      DO 75 I = 2,50
      J = I + 50
      K = 151 - I
      L = 150 - I
      N = I - 1
      M = 251 - I
      MM = 250 - I
      KCON{1,1} = 10*N + 5
      KCON{1,2} = 10*J + 4
      KCON{1,3} = 10*K + 4
      KCON{1,4} = 10*L + 4
      KCON{1,5} = 10*M + 4
      KCON{1,6} = 10*MM + 4

```



```

WRITE(2,908){(L3(I), I=1,6)
WRITE(2,911){FL4(1), FL4(2), L4, FL4(3), FL4(4)
911 FORMAT(F8.3, F8.5, I8, F8.5, F8.2)
912 WRITE(2,912){SET2(1), SET2(2)}
912 FORMAT(2F8.0)
C
DO 200 I = 1, 50
WRITE(2,913){KCON(I, J), J=1,6)
913 FORMAT(9I8)
914 WRITE(2,914){COEF(I, J), J=1,6)
200 CONTINUE
C
DO 250 I=51, 300
WRITE(2,913){KCON(I, 1), KCON(I, 2)}
913 FORMAT(2,914){COEF(I, 1), COEF(I, 2)}
250 CONTINUE
C
7 CONTINUE
STOP
END
/*
//LKED.SYSLMOD DD DISP=SHR, DSN=NAME=MSS.S2054.LOADLIB
//LKED.SYSLMOD DD DISP=SHR, DSN=NAME=MSS.S2054.LOADLIB
//LKED.SYSLMOD DD DISP=SHR, DSN=NAME=MSS.S2054.LOADLIB
/*
//

```

MASTER EXECUTION PROGRAM FOR NTU53C AND TVCOUNT

95

AD-A161 019

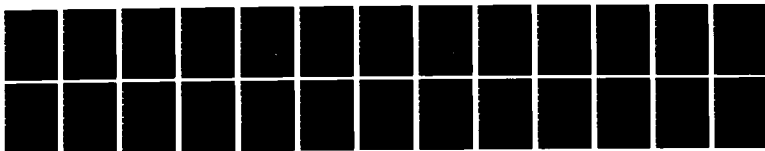
THE EFFECTIVENESS OF HEAT EXCHANGERS WITH ONE SHELL
PASS AND FIVE TUBE PASSES(U) NAVAL POSTGRADUATE SCHOOL
MONTEREY CA L E HESS SEP 85

2/2

UNCLASSIFIED

F/G 13/1

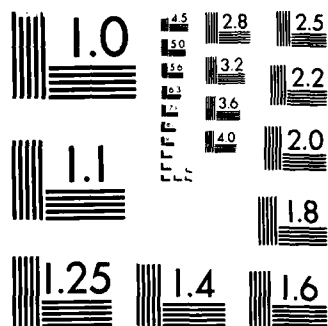
NL



END

FILED

DTIC



MICROCOPY RESOLUTION TEST CHART
NATIONAL BUREAU OF STANDARDS-1963-A

NTU=0.50	R=0.30	PARALLEL	TVSSIN	15.	200.	100.
250.		75.0	3.75000			
NTU=0.75	R=0.30	PARALLEL	TVSSIO	15.	200.	100.
250.		75.0	5.00000			
NTU=1.00	R=0.30	PARALLEL	TVSSIP	15.	200.	100.
250.		75.0	6.25000			
NTU=1.25	R=0.30	PARALLEL	TVSSIQ	15.	200.	100.
250.		75.0	7.50000			
NTU=1.50	R=0.30	PARALLEL	TVSSIR	15.	200.	100.
250.		75.0	10.00000			
NTU=2.00	R=0.30	PARALLEL	TVSSIS	15.	200.	100.
250.		75.0	12.50000			
NTU=2.50	R=0.30	PARALLEL	TVSSIT	15.	200.	100.
250.		75.0	15.00000			
NTU=3.00	R=0.30	PARALLEL	TVSSIU	15.	200.	100.
250.		75.0	16.25000			
NTU=3.25	R=0.30	PARALLEL	TVSSIV	15.	200.	100.
250.		75.0				


```

//STEPL EXEC FORTVG PROG=TVSSSIAC, LIB= 'MSS, S2054. LOADLIB'
//GO. FT01F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT02F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT09F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT10F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT03F001 DD DUMMY
//GO. FT04F001 DD DISP=(OLD, DELETE) UNIT=SYSDA, DSN=&TVSSIL
//GO. FT08F001 DD SYSOUT=A, DCB=RECFM=FBA
//STEPM EXEC FORTVG PROG=TVSSSIAC, LIB= 'MSS, S2054. LOADLIB'
//GO. FT01F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT02F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT09F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT10F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT03F001 DD DUMMY
//GO. FT04F001 DD DISP=(OLD, DELETE) UNIT=SYSDA, DSN=&TVSSIM
//GO. FT08F001 DD SYSOUT=A, DCB=RECFM=FBA
//STEPN EXEC FORTVG PROG=TVSSSIAC, LIB= 'MSS, S2054. LOADLIB'
//GO. FT01F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT02F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT09F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT10F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT03F001 DD DUMMY
//GO. FT04F001 DD DISP=(OLD, DELETE) UNIT=SYSDA, DSN=&TVSSIN
//GO. FT08F001 DD SYSOUT=A, DCB=RECFM=FBA
//STEPO EXEC FORTVG PROG=TVSSSIAC, LIB= 'MSS, S2054. LOADLIB'
//GO. FT01F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT02F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT09F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT10F001 DD UNIT=SYSDA, SPACE= {CYL, {1,1}}
//GO. FT03F001 DD DUMMY
//GO. FT04F001 DD DISP=(OLD, DELETE) UNIT=SYSDA, DSN=&TVSSIO
//GO. FT08F001 DD SYSOUT=A, DCB=RECFM=FBA

```



```

//GO.FT02F001 DD UNIT=SYSDA, SPACE={CYL,{1,1}}
//GO.FT09F001 DD UNIT=SYSDA, SPACE={CYL,{1,1}}
//GO.FT10F001 DD UNIT=SYSDA, SPACE={CYL,{1,1}}
//GO.FT03F001 DD DUMMY
//GO.FT04F001 DD DISP=(OLD,DELETE), UNIT=SYSDA, DSN=&TVSSIV
//GO.FT08F001 DD SYSOUT=A, DCB=RECFM=FBA
//

```

APPENDIX H

1-5:3P EFFECTIVENESS VS. N_{tu} GRAPHS AT VARIOUS R VALUES

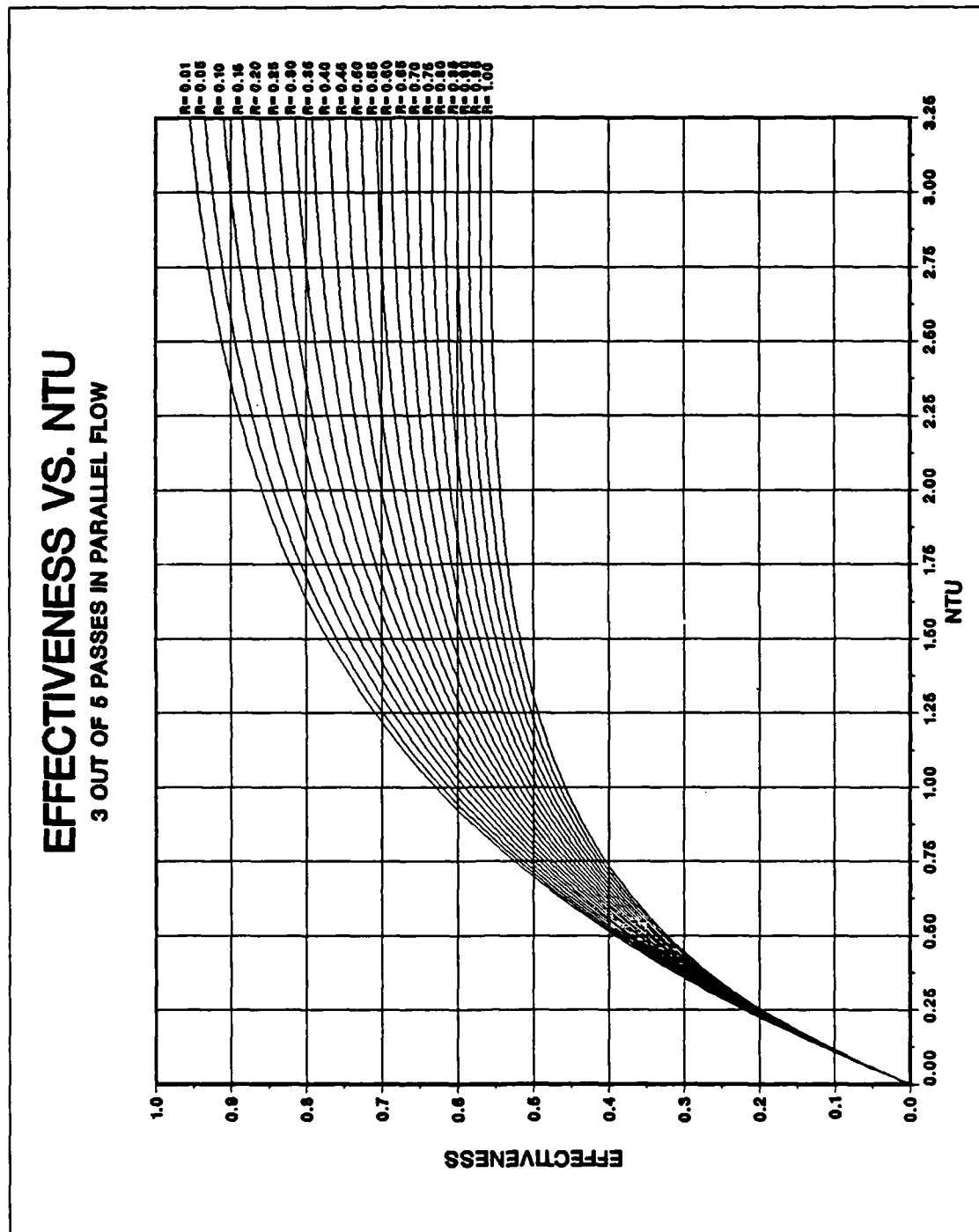


Figure H.1 1-5:3P Effectiveness vs. N_{tu} over Range of R from 0.01 to 1.0

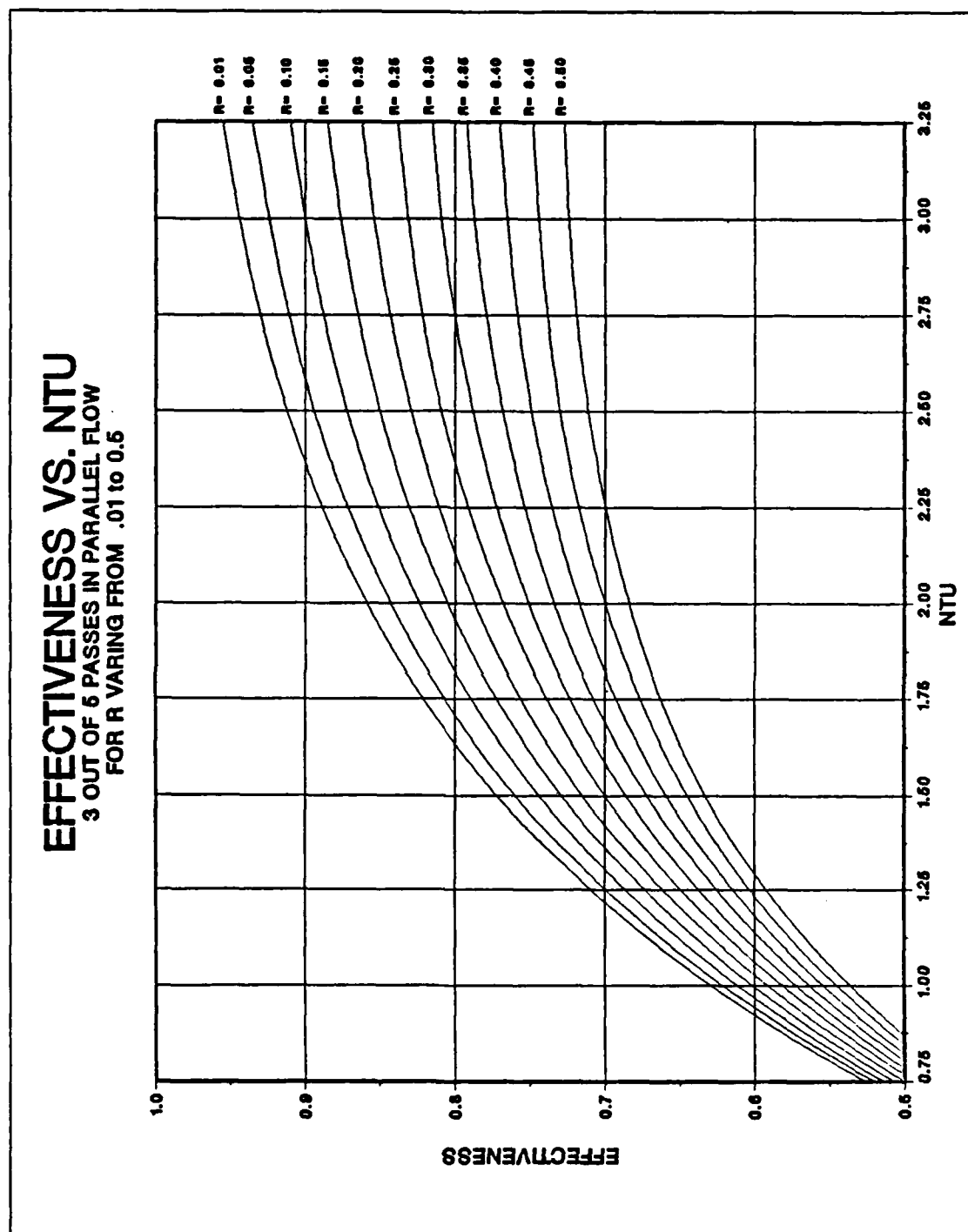


Figure H.2 1-5:3P Effectiveness vs. N_{tu} over Range of R from 0.01 to 0.5

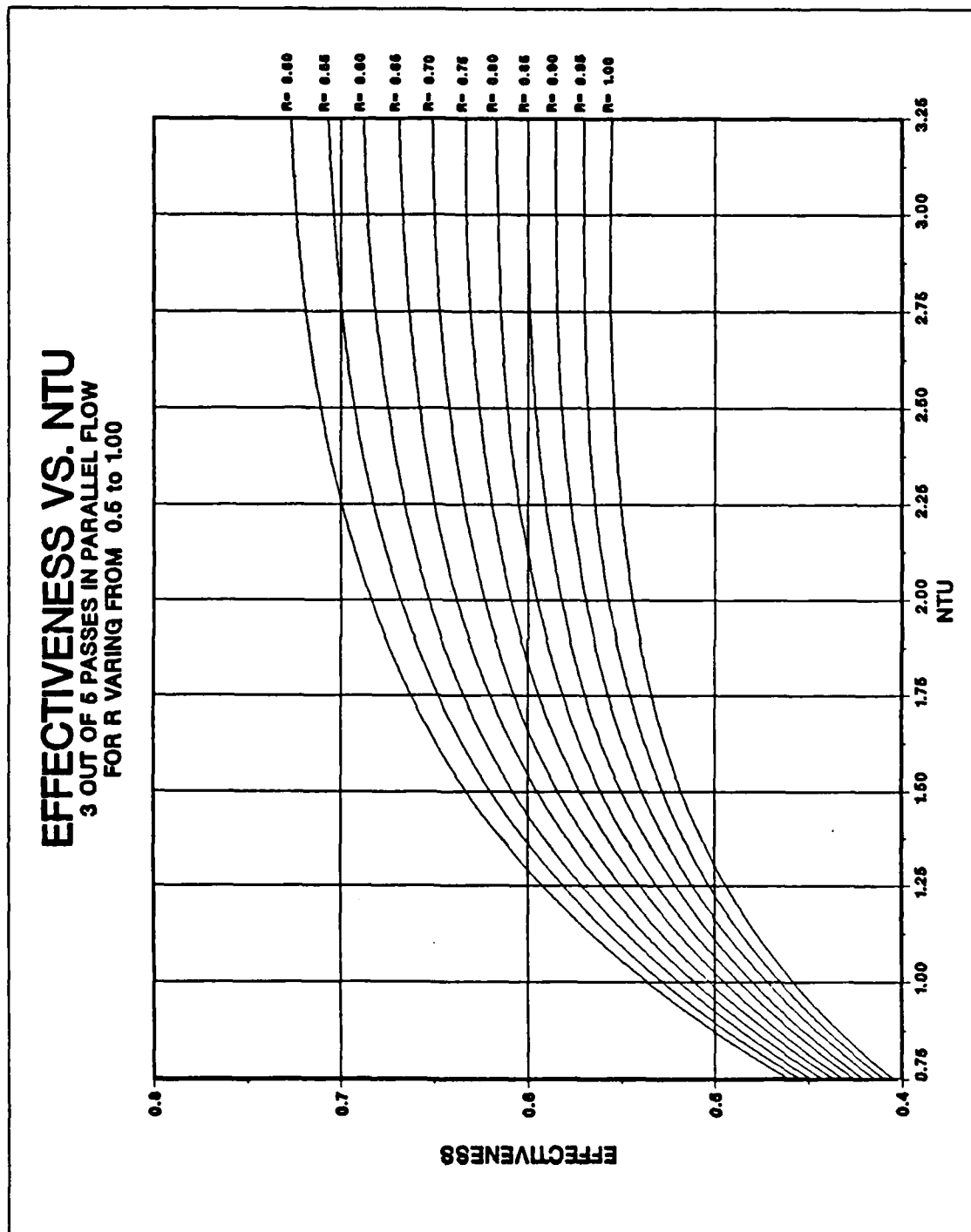


Figure H.3 1-5:3P Effectiveness vs. N_{tu} over Range of R from 0.5 to 1.00

APPENDIX I

1-5:3C EFFECTIVENESS VS. N_{tu} GRAPHS AT VARIOUS R VALUES

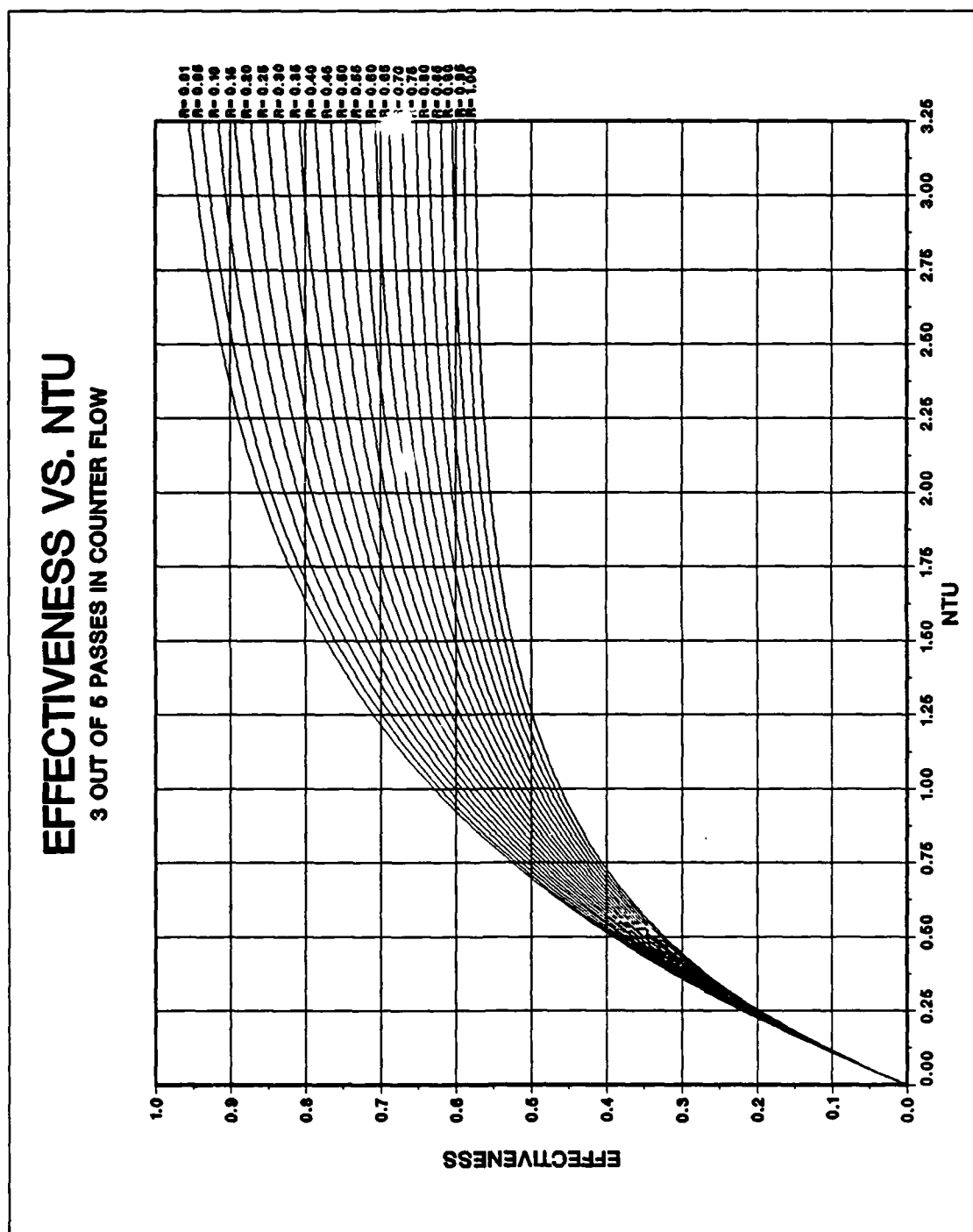


Figure I.1 1-5:3C Effectiveness vs. N_{tu} over Range of R from 0.01 to 1.0

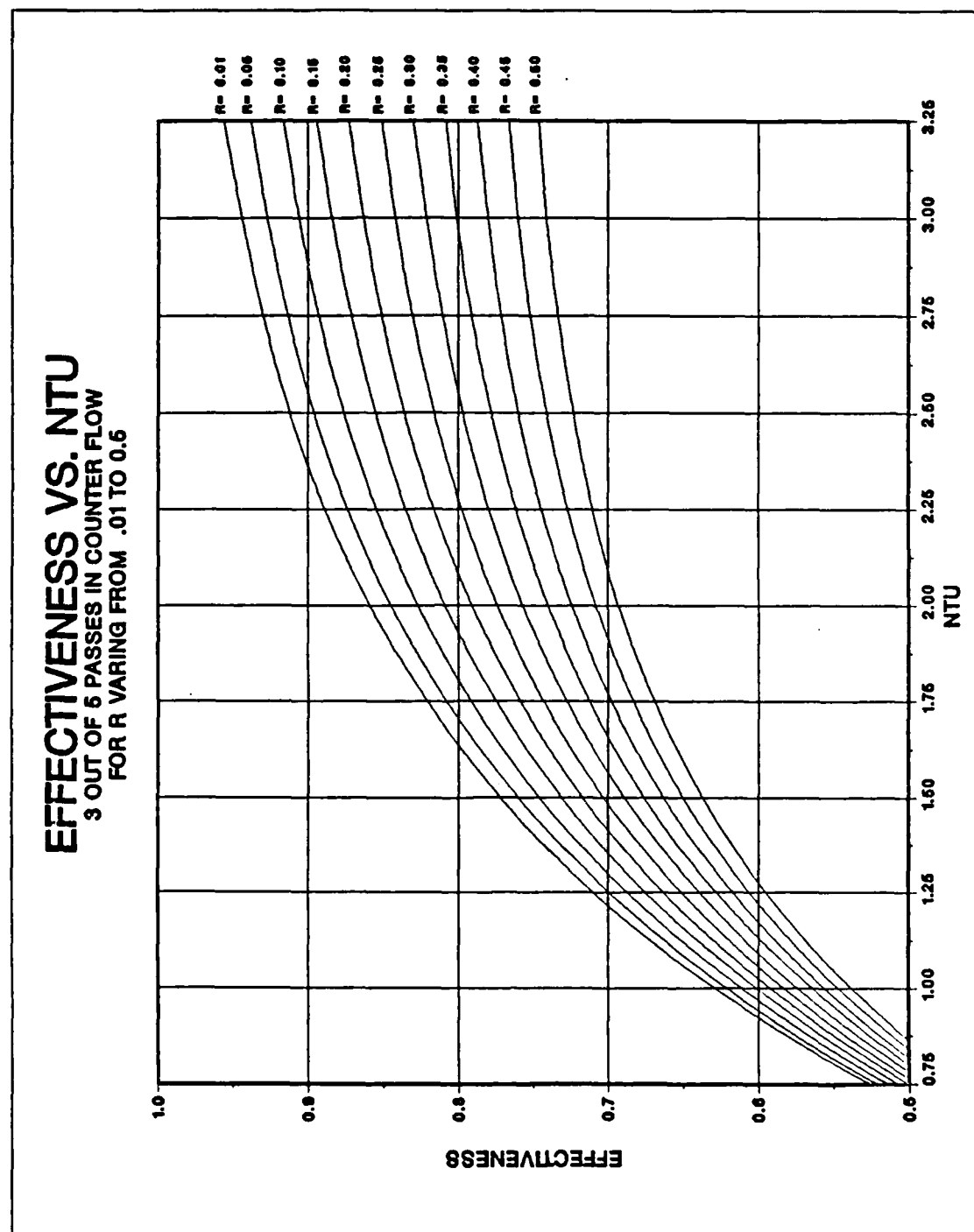


Figure I.2 1-5:3C Effectiveness vs. N_{tu} over Range of R from 0.01 to 0.5

EFFECTIVENESS VS. NTU **3 OUT OF 5 PASSES IN COUNTER FLOW** **FOR R VARYING FROM 0.5 TO 1.00**

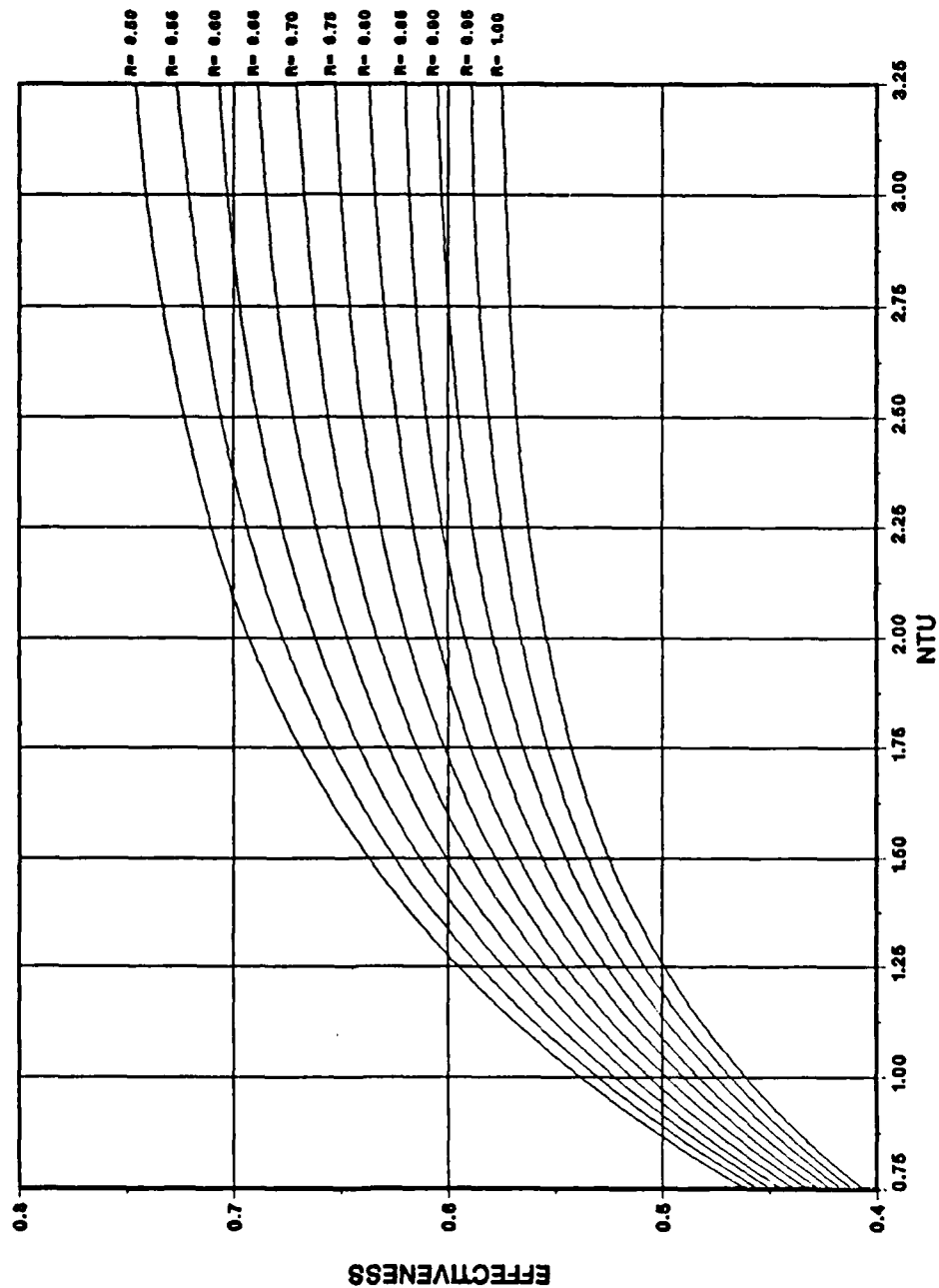


Figure I.3 1-5:3C Effectiveness vs. N_{tu} over Range of R from 0.5 to 1.00

APPENDIX J

EFFECTIVENESS COMPUTER GENERATED ANALYZER PROGRAM

```

C*****
C      EFFECTIVENESS PROGRAM
C      LCDR L. E. HESS
C      12 AUGUST 1985
C*****
C      THIS PROGRAM CONTAINS THE 1-5 POLYNOMIAL APPROXIMATION COEFFICIENTS.
C      BY ENTERING THE VALUES FOR NTU, R AND THE TYPE OF HEAT EXCHANGER, THE
C      EFFECTIVENESS VALUES ARE READILY OBTAINED. BY EITHER USING THE 1-5
C      COUNTER OR PARALLEL COEFFICIENTS DIRECTLY OR BY LINEAR INTERPOLATION
C
C      REAL NTU, E, E1, E2, R, R1, R2
C      CHARACTER*10 EXCH
C      WRITE(6,10)
C      FORMAT (// INPUT THE TYPE OF HEAT EXCHANGER (PARALLEL OR COUNTER)')
C      *)
C      READ(5,20) EXCH
C      FORMAT(A10)
C      WRITE(6,30)
C      FORMAT (// INPUT NUMBER OF TRANSFER UNITS (NTU)')
C      READ(5,40) NTU
C      FORMAT(BN,F10.0)
C      WRITE(6,50)
C      FORMAT (// INPUT CAPACITY RATE RATIO (R). R MUST BE GREATER THAN 0
C      *R EQUAL TO 0.01, /, AND LESS THAN OR EQUAL TO 1.00')
C      READ(5,40) R
C      IF (EXCH.EQ.'COUNTER') THEN
C      IF (R.GE.0.01) THEN
C      IF (R.LE.0.05) THEN
C      R1=0.01
C      R2=0.05
C      E1=.00057463+0.99093*NTU-0.47938*NTU**2+0.13879*NTU**3-0.023
C      *075*NTU**4+0.0016779*NTU**5
C      *E2=.00079100+0.98831*NTU-0.49081*NTU**2+0.14654*NTU**3-0.025
C      *068*NTU**4+0.0018647*NTU**5
C      IF (R.EQ.0.01) THEN
C      WRITE(6,60) E1
C      FORMAT (// EFFECTIVENESS =',F7.4)
C      ELSE IF (R.EQ.0.05) THEN
C      ELSE IF
C      WRITE(6,60) E2
C      ELSE
C      CALL INTERP (R,R1,R2,E1,E2,E)
C      WRITE (6,60) E

```

```

ENDIF
ENDIF
IF (R.GT.0.05) THEN
IF (R.LE.0.10) THEN
R1=0.05
R2=0.10
E1=.00079100+0.98831*NTU-0.49081*NTU**2+0.14654*NTU**3-0.025
068*NTU**4+0.0018647*NTU**5
E2=.00108210+0.98622*NTU-0.50716*NTU**2+0.15773*NTU**3-0.028
045*NTU**4+0.0021547*NTU**5
IF (R.EQ.0.10) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E

```

* *

```

ENDIF
ENDIF
IF (R.GT.0.10) THEN
IF (R.LE.0.15) THEN
R1=0.10
R2=0.15
E1=.00108210+0.98622*NTU-0.50716*NTU**2+0.15773*NTU**3-0.028
045*NTU**4+0.0021547*NTU**5
E2=.00125311+0.98238*NTU-0.52072*NTU**2+0.16779*NTU**3-0.030
947*NTU**4+0.0024635*NTU**5
IF (R.EQ.0.15) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E

```

* *

```

ENDIF
ENDIF
IF (R.GT.0.15) THEN
IF (R.LE.0.20) THEN
R1=0.15
R2=0.20
E1=.00125311+0.98238*NTU-0.52072*NTU**2+0.16779*NTU**3-0.030
947*NTU**4+0.0024635*NTU**5
E2=.00142506+0.97866*NTU-0.53259*NTU**2+0.17545*NTU**3-0.032
772*NTU**4+0.0026203*NTU**5
IF (R.EQ.0.20) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E

```

* *

```

ENDIF
ENDIF

```

```

ENDIF
IF (R.GT.0.20) THEN
IF (R.LE.0.25) THEN
R1=0.20
R2=0.25
E1=.00142506+0.97866*NTU-0.53259*NTU**2+0.17545*NTU**3-0.032
772*NTU**4+0.0026203*NTU**5
E2=.00133145+0.97670*NTU-0.54709*NTU**2+0.18482*NTU**3-0.035
072*NTU**4+0.0028213*NTU**5
IF(R.EQ.0.25) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
IF (R.GT.0.25) THEN
IF (R.LE.0.30) THEN
R1=0.25
R2=0.30
E1=.00133145+0.97670*NTU-0.54709*NTU**2+0.18482*NTU**3-0.035
072*NTU**4+0.0028213*NTU**5
E2=.00151081+0.97405*NTU-0.56166*NTU**2+0.19541*NTU**3-0.038
055*NTU**4+0.0031252*NTU**5
IF (R.EQ.0.30) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
IF (R.GT.0.30) THEN
IF (R.LE.0.35) THEN
R1=0.30
R2=0.35
E1=.00151081+0.97405*NTU-0.56166*NTU**2+0.19541*NTU**3-0.038
055*NTU**4+0.0031252*NTU**5
E2=.00174198+0.97091*NTU-0.57527*NTU**2+0.20542*NTU**3-0.040
903*NTU**4+0.0034186*NTU**5
IF(R.EQ.0.35) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
IF (R.GT.0.35) THEN
ENDIF
ENDIF
IF (R.GT.0.35) THEN

```

```

IF (R.LE.0.40) THEN
  R1=0.35
  R2=0.40
  E1=00174198+0.97091*NTU-0.57527*NTU**2+0.20542*NTU**3-0.040
  903*NTU**4+0.0034186*NTU**5
  E2=00184400+0.96879*NTU-0.59067*NTU**2+0.21718*NTU**3-0.044
  469*NTU**4+0.0038122*NTU**5
  IF (R.EQ.0.40) THEN
    WRITE (6,60) E2
  ELSE
    CALL INTERP (R,R1,R2,E1,E2,E)
    WRITE (6,60) E
  ENDIF
ENDIF
ENDIF
IF (R.GT.0.40) THEN
  IF (R.LE.0.45) THEN
    R1=0.40
    R2=0.45
    E1=00184400+0.96879*NTU-0.59067*NTU**2+0.21718*NTU**3-0.044
    469*NTU**4+0.0038122*NTU**5
    E2=00213420+0.96459*NTU-0.60073*NTU**2+0.22416*NTU**3-0.046
    295*NTU**4+0.0039861*NTU**5
    IF (R.EQ.0.45) THEN
      WRITE (6,60) E2
    ELSE
      CALL INTERP (R,R1,R2,E1,E2,E)
      WRITE (6,60) E
    ENDIF
  ENDIF
ENDIF
IF (R.GT.0.45) THEN
  IF (R.LE.0.50) THEN
    R1=0.45
    R2=0.50
    E1=00213420+0.96459*NTU-0.60073*NTU**2+0.22416*NTU**3-0.046
    295*NTU**4+0.0039861*NTU**5
    E2=00230808+0.96140*NTU-0.61293*NTU**2+0.23322*NTU**3-0.048
    933*NTU**4+0.0042669*NTU**5
    IF (R.EQ.0.50) THEN
      WRITE (6,60) E2
    ELSE
      CALL INTERP (R,R1,R2,E1,E2,E)
      WRITE (6,60) E
    ENDIF
  ENDIF
ENDIF
IF (R.GT.0.50) THEN
  IF (R.LE.0.55) THEN
    R1=0.50

```

```

*
*
R2=0.55
E1=00230808+0.96140*NTU-0.61293*NTU**2+0.23322*NTU**3-0.048
933*NTU**4+0.0042669*NTU**5
E2=00257953+0.95713*NTU-0.62234*NTU**2+0.23996*NTU**3-0.050
762*NTU**4+0.0044499*NTU**5
IF (R.EQ.0.55) THEN
  WRITE (6,60) E2
ELSE
  CALL INTERP (R,R1,R2,E1,E2,E)
  WRITE (6,60) E
ENDIF
ENDIF
IF (R.GT.0.55) THEN
  IF (R.LE.0.60) THEN
    R1=0.55
    R2=0.60
    E1=00257953+0.95713*NTU-0.62234*NTU**2+0.23996*NTU**3-0.050
    762*NTU**4+0.0044499*NTU**5
    E2=00274755+0.95336*NTU-0.63230*NTU**2+0.24706*NTU**3-0.052
    681*NTU**4+0.0046391*NTU**5
    IF (R.EQ.0.60) THEN
      WRITE (6,60) E2
    ELSE
      CALL INTERP (R,R1,R2,E1,E2,E)
      WRITE (6,60) E
    ENDIF
  ENDIF
  IF (R.GT.0.60) THEN
    IF (R.LE.0.65) THEN
      R1=0.60
      R2=0.65
      E1=00274755+0.95336*NTU-0.63230*NTU**2+0.24706*NTU**3-0.052
      681*NTU**4+0.0046391*NTU**5
      E2=00305249+0.94903*NTU-0.64122*NTU**2+0.25366*NTU**3-0.054
      530*NTU**4+0.0048293*NTU**5
      IF (R.EQ.0.65) THEN
        WRITE (6,60) E2
      ELSE
        CALL INTERP (R,R1,R2,E1,E2,E)
        WRITE (6,60) E
      ENDIF
    ENDIF
  ENDIF
  IF (R.GT.0.65) THEN
    IF (R.LE.0.70) THEN
      R1=0.65
      R2=0.70
      E1=00305249+0.94903*NTU-0.64122*NTU**2+0.25366*NTU**3-0.054

```

```

*
*
530*NTU**4+0.0048293*NTU**5
E2=.00319573+0.94580*NTU-0.65184*NTU**2+0.26137*NTU**3-0.056
656*NTU**4+0.0050422*NTU**5
IF(R.EQ.0.70) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
ENDIF
IF (R.GT.0.70) THEN
IF (R.LE.0.75) THEN
R1=0.70
R2=0.75
E1=.00319573+0.94580*NTU-0.65184*NTU**2+0.26137*NTU**3-0.056
656*NTU**4+0.0050422*NTU**5
E2=.00339253+0.94193*NTU-0.66116*NTU**2+0.26833*NTU**3-0.058
615*NTU**4+0.0052431*NTU**5
IF(R.EQ.0.75) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
ENDIF
IF (R.GT.0.75) THEN
IF (R.LE.0.80) THEN
R1=0.75
R2=0.80
E1=.00339253+0.94193*NTU-0.66116*NTU**2+0.26833*NTU**3-0.058
615*NTU**4+0.0052431*NTU**5
E2=.00363419+0.93822*NTU-0.67053*NTU**2+0.27531*NTU**3-0.060
558*NTU**4+0.0054393*NTU**5
IF(R.EQ.0.80) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
ENDIF
IF (R.GT.0.80) THEN
IF (R.LE.0.85) THEN
R1=0.80
R2=0.85
E1=.00363419+0.93822*NTU-0.67053*NTU**2+0.27531*NTU**3-0.060
558*NTU**4+0.0054393*NTU**5
E2=.00382659+0.93407*NTU-0.67841*NTU**2+0.28109*NTU**3-0.062

```

```

*      088*NTU**4+0.0055850*NTU**5
      IF(R.EQ.0.85) THEN
        WRITE (6,60) E2
      ELSE
        CALL INTERP (R,R1,R2,E1,E2,E)
        WRITE (6,60) E
      ENDIF
    ENDIF
    IF (R.GT.0.85) THEN
      IF (R.LE.0.90) THEN
        R1=0.85
        R2=0.90
        E1=0.0382659+0.93407*NTU-0.67841*NTU**2+0.28109*NTU**3-0.062
        088*NTU**4+0.0055850*NTU**5
        E2=0.0398221+0.93052*NTU-0.68748*NTU**2+0.28799*NTU**3-0.064
        051*NTU**4+0.0057874*NTU**5
        IF(R.EQ.0.90) THEN
          WRITE (6,60) E2
        ELSE
          CALL INTERP (R,R1,R2,E1,E2,E)
          WRITE (6,60) E
        ENDIF
      ENDIF
      IF (R.GT.0.90) THEN
        IF (R.LE.0.95) THEN
          R1=0.90
          R2=0.95
          E1=0.0398221+0.93052*NTU-0.68748*NTU**2+0.28799*NTU**3-0.064
          051*NTU**4+0.0057874*NTU**5
          E2=0.0426945+0.92609*NTU-0.69496*NTU**2+0.29381*NTU**3-0.065
          653*NTU**4+0.0059442*NTU**5
          IF(R.EQ.0.95) THEN
            WRITE (6,60) E2
          ELSE
            CALL INTERP (R,R1,R2,E1,E2,E)
            WRITE (6,60) E
          ENDIF
        ENDIF
        IF (R.GT.0.95) THEN
          IF (R.LE.1.00) THEN
            R1=0.95
            R2=1.00
            E1=0.0426945+0.92609*NTU-0.69496*NTU**2+0.29381*NTU**3-0.065
            653*NTU**4+0.0059442*NTU**5
            E2=0.0440670+0.92259*NTU-0.70365*NTU**2+0.30046*NTU**3-0.067
            514*NTU**4+0.0061309*NTU**5
            IF(R.EQ.1.00) THEN
              WRITE (6,60) E2
            ELSE
              CALL INTERP (R,R1,R2,E1,E2,E)
              WRITE (6,60) E
            ENDIF
          ENDIF
        ENDIF
      ENDIF
    ENDIF
  ENDIF

```

```

WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
ELSE IF (EXCH.EQ.'PARALLEL') THEN
IF (R.GE.0.01) THEN
IF (R.LE.0.05) THEN
R1=0.01
R2=0.05
E1=0.0052233+0.99152*NTU-0.48055*NTU**2+0.13953*NTU**3-0.023
283*NTU**4+0.0016989*NTU**5
E2=0.0081101+0.98817*NTU-0.49062*NTU**2+0.14604*NTU**3-0.024
883*NTU**4+0.0018421*NTU**5
IF (R.EQ.0.01) THEN
WRITE (6,60) E1
ELSE IF (R.EQ.0.05) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
IF (R.GT.0.05) THEN
IF (R.LE.0.10) THEN
R1=0.05
R2=0.10
E1=0.0081101+0.98817*NTU-0.49062*NTU**2+0.14604*NTU**3-0.024
883*NTU**4+0.0018421*NTU**5
E2=0.0110555+0.98599*NTU-0.50718*NTU**2+0.15721*NTU**3-0.027
865*NTU**4+0.0021337*NTU**5
IF (R.EQ.0.10) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
IF (R.GT.0.10) THEN
IF (R.LE.0.15) THEN
R1=0.10
R2=0.15
E1=0.0110555+0.98599*NTU-0.50718*NTU**2+0.15721*NTU**3-0.027
865*NTU**4+0.0021337*NTU**5
E2=0.0114518+0.98309*NTU-0.52246*NTU**2+0.16811*NTU**3-0.030
968*NTU**4+0.0024604*NTU**5

```

```

IF(R.EQ.0.15) THEN
  WRITE(6,60) E2
ELSE
  CALL INTERP (R,R1,R2,E1,E2,E)
  WRITE(6,60) E
ENDIF
ENDIF
ENDIF
IF (R.GT.0.15) THEN
  IF (R.LE.0.20) THEN
    R1=0.15
    R2=0.20
    E1=0.00114518+0.98309*NTU-0.52246*NTU**2+0.16811*NTU**3-0.030
    968*NTU**4+0.0024604*NTU**5
    E2=0.00125862+0.97914*NTU-0.53367*NTU**2+0.17485*NTU**3-0.032
    443*NTU**4+0.0025741*NTU**5
    IF (R.EQ.0.20) THEN
      WRITE(6,60) E2
    ELSE
      CALL INTERP (R,R1,R2,E1,E2,E)
      WRITE(6,60) E
    ENDIF
  ENDIF
ENDIF
IF (R.GT.0.20) THEN
  IF (R.LE.0.25) THEN
    R1=0.20
    R2=0.25
    E1=0.00125862+0.97914*NTU-0.53367*NTU**2+0.17485*NTU**3-0.032
    443*NTU**4+0.0025741*NTU**5
    E2=0.00129233+0.97701*NTU-0.54864*NTU**2+0.18464*NTU**3-0.034
    902*NTU**4+0.0027929*NTU**5
    IF (R.EQ.0.25) THEN
      WRITE(6,60) E2
    ELSE
      CALL INTERP (R,R1,R2,E1,E2,E)
      WRITE(6,60) E
    ENDIF
  ENDIF
ENDIF
IF (R.GT.0.25) THEN
  IF (R.LE.0.30) THEN
    R1=0.25
    R2=0.30
    E1=0.00129233+0.97701*NTU-0.54864*NTU**2+0.18464*NTU**3-0.034
    902*NTU**4+0.0027929*NTU**5
    E2=0.00143113+0.97558*NTU-0.56664*NTU**2+0.19807*NTU**3-0.038
    885*NTU**4+0.0032195*NTU**5
    IF (R.EQ.0.30) THEN
      WRITE(6,60) E2
    ELSE
      CALL INTERP (R,R1,R2,E1,E2,E)
      WRITE(6,60) E
    ENDIF
  ENDIF
ENDIF
IF (R.GT.0.30) THEN
  IF (R.LE.0.35) THEN
    R1=0.30
    R2=0.35
    E1=0.00143113+0.97558*NTU-0.56664*NTU**2+0.19807*NTU**3-0.038
    885*NTU**4+0.0032195*NTU**5
    E2=0.00157113+0.97415*NTU-0.58664*NTU**2+0.21807*NTU**3-0.042
    885*NTU**4+0.0034195*NTU**5
    IF (R.EQ.0.35) THEN
      WRITE(6,60) E2
    ELSE
      CALL INTERP (R,R1,R2,E1,E2,E)
      WRITE(6,60) E
    ENDIF
  ENDIF
ENDIF

```

```

ELSE
  CALL INTERP (R,R1,R2,E1,E2,E)
  WRITE (6,60) E
ENDIF
ENDIF
IF (R.GT.0.30) THEN
  IF (R.LE.0.35) THEN
    R1=0.30
    R2=0.35
    E1=0.00143113+0.97558*NTU-0.56664*NTU**2+0.19807*NTU**3-0.038
    885*NTU**4+0.0032195*NTU**5
    E2=0.00169053+0.97206*NTU-0.57958*NTU**2+0.20740*NTU**3-0.041
    500*NTU**4+0.0034854*NTU**5
    IF (R.EQ.0.35) THEN
      WRITE (6,60) E2
    ELSE
      CALL INTERP (R,R1,R2,E1,E2,E)
      WRITE (6,60) E
    ENDIF
  ENDIF
ENDIF
IF (R.GT.0.35) THEN
  IF (R.LE.0.40) THEN
    R1=0.35
    R2=0.40
    E1=0.00169053+0.97206*NTU-0.57958*NTU**2+0.20740*NTU**3-0.041
    500*NTU**4+0.0034854*NTU**5
    E2=0.00176316+0.96998*NTU-0.59515*NTU**2+0.21912*NTU**3-0.045
    054*NTU**4+0.0038805*NTU**5
    IF (R.EQ.0.40) THEN
      WRITE (6,60) E2
    ELSE
      CALL INTERP (R,R1,R2,E1,E2,E)
      WRITE (6,60) E
    ENDIF
  ENDIF
ENDIF
IF (R.GT.0.40) THEN
  IF (R.LE.0.45) THEN
    R1=0.40
    R2=0.45
    E1=0.00176316+0.96998*NTU-0.59515*NTU**2+0.21912*NTU**3-0.045
    054*NTU**4+0.0038805*NTU**5
    E2=0.00210897+0.96559*NTU-0.60498*NTU**2+0.22583*NTU**3-0.046
    805*NTU**4+0.0040487*NTU**5
    IF (R.EQ.0.45) THEN
      WRITE (6,60) E2
    ELSE
      CALL INTERP (R,R1,R2,E1,E2,E)
      WRITE (6,60) E
    ENDIF
  ENDIF
ENDIF
IF (R.GT.0.45) THEN
  IF (R.LE.0.50) THEN
    R1=0.45
    R2=0.50
    E1=0.00210897+0.96559*NTU-0.60498*NTU**2+0.22583*NTU**3-0.046
    805*NTU**4+0.0040487*NTU**5
    E2=0.00249999+0.96119*NTU-0.61998*NTU**2+0.23998*NTU**3-0.047
    500*NTU**4+0.0042999*NTU**5
    IF (R.EQ.0.50) THEN
      WRITE (6,60) E2
    ELSE
      CALL INTERP (R,R1,R2,E1,E2,E)
      WRITE (6,60) E
    ENDIF
  ENDIF
ENDIF
IF (R.GT.0.50) THEN
  IF (R.LE.0.55) THEN
    R1=0.50
    R2=0.55
    E1=0.00249999+0.96119*NTU-0.61998*NTU**2+0.23998*NTU**3-0.047
    500*NTU**4+0.0042999*NTU**5
    E2=0.00289999+0.95679*NTU-0.63498*NTU**2+0.25498*NTU**3-0.048
    000*NTU**4+0.0044999*NTU**5
    IF (R.EQ.0.55) THEN
      WRITE (6,60) E2
    ELSE
      CALL INTERP (R,R1,R2,E1,E2,E)
      WRITE (6,60) E
    ENDIF
  ENDIF
ENDIF
IF (R.GT.0.55) THEN
  IF (R.LE.0.60) THEN
    R1=0.55
    R2=0.60
    E1=0.00289999+0.95679*NTU-0.63498*NTU**2+0.25498*NTU**3-0.048
    000*NTU**4+0.0044999*NTU**5
    E2=0.00329999+0.95239*NTU-0.64998*NTU**2+0.26998*NTU**3-0.049
    000*NTU**4+0.0046999*NTU**5
    IF (R.EQ.0.60) THEN
      WRITE (6,60) E2
    ELSE
      CALL INTERP (R,R1,R2,E1,E2,E)
      WRITE (6,60) E
    ENDIF
  ENDIF
ENDIF

```

```

WRITE (6,60) E
ENDIF
ENDIF
IF (R.GT.0.45) THEN
IF (R.LE.0.50) THEN
R1=0.45
R2=0.50
E1=0.00210897+0.96559*NTU-0.60498*NTU**2+0.22583*NTU**3-0.046
805*NTU**4+0.0040487*NTU**5
E2=0.00230583+0.96163*NTU-0.61546*NTU**2+0.23327*NTU**3-0.048
857*NTU**4+0.0042594*NTU**5
IF (R.EQ.0.50) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
IF (R.GT.0.50) THEN
IF (R.LE.0.55) THEN
R1=0.50
R2=0.55
E1=0.00230583+0.96163*NTU-0.61546*NTU**2+0.23327*NTU**3-0.048
857*NTU**4+0.0042594*NTU**5
E2=0.00259035+0.95726*NTU-0.62480*NTU**2+0.23985*NTU**3-0.050
625*NTU**4+0.0044354*NTU**5
IF (R.EQ.0.55) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
IF (R.GT.0.55) THEN
IF (R.LE.0.60) THEN
R1=0.55
R2=0.60
E1=0.00259035+0.95726*NTU-0.62480*NTU**2+0.23985*NTU**3-0.050
625*NTU**4+0.0044354*NTU**5
E2=0.00277374+0.95331*NTU-0.63434*NTU**2+0.24638*NTU**3-0.052
303*NTU**4+0.0045925*NTU**5
IF (R.EQ.0.60) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
ENDIF

```

* * * * *

```

ENDIF
ENDIF
IF (R.GT.0.60) THEN
IF (R.LE.0.65) THEN
R1=0.60
R2=0.65
E1=0.00277374+0.953331*NTU-0.63434*NTU**2+0.24638*NTU**3-0.052
303*NTU**4+0.0045925*NTU**5
E2=0.00291148+0.95025*NTU-0.64574*NTU**2+0.25460*NTU**3-0.054
593*NTU**4+0.0048260*NTU**5
IF (R.EQ.0.65) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
ENDIF
IF (R.GT.0.65) THEN
IF (R.LE.0.70) THEN
R1=0.65
R2=0.70
E1=0.00291148+0.95025*NTU-0.64574*NTU**2+0.25460*NTU**3-0.054
593*NTU**4+0.0048260*NTU**5
E2=0.00322294+0.94575*NTU-0.65400*NTU**2+0.26039*NTU**3-0.056
053*NTU**4+0.0049575*NTU**5
IF (R.EQ.0.70) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
ENDIF
IF (R.GT.0.70) THEN
IF (R.LE.0.75) THEN
R1=0.70
R2=0.75
E1=0.00322294+0.94575*NTU-0.65400*NTU**2+0.26039*NTU**3-0.056
053*NTU**4+0.0049575*NTU**5
E2=0.00338351+0.94231*NTU-0.66425*NTU**2+0.26788*NTU**3-0.058
110*NTU**4+0.0051617*NTU**5
IF (R.EQ.0.75) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E
ENDIF
ENDIF
ENDIF

```

* *

* *

* *

```

IF (R.GT.0.75) THEN
IF (R.LE.0.80) THEN
R1=0.75
R2=0.80
E1=0.0338351+0.94231*NTU-0.66425*NTU**2+0.26788*NTU**3-0.058
110*NTU**4+0.0051617*NTU**5
E2=0.0360234+0.93852*NTU-0.67369*NTU**2+0.27495*NTU**3-0.060
079*NTU**4+0.0053606*NTU**5
IF (R.EQ.0.80) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E

```

* *

```

ENDIF
ENDIF
IF (R.GT.0.80) THEN
IF (R.LE.0.85) THEN
R1=0.80
R2=0.85
E1=0.0360234+0.93852*NTU-0.67369*NTU**2+0.27495*NTU**3-0.060
079*NTU**4+0.0053606*NTU**5
E2=0.0382374+0.93414*NTU-0.68130*NTU**2+0.28045*NTU**3-0.061
487*NTU**4+0.0054884*NTU**5
IF (R.EQ.0.85) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E

```

* *

```

ENDIF
ENDIF
IF (R.GT.0.85) THEN
IF (R.LE.0.90) THEN
R1=0.85
R2=0.90
E1=0.0382374+0.93414*NTU-0.68130*NTU**2+0.28045*NTU**3-0.061
487*NTU**4+0.0054884*NTU**5
E2=0.0391805+0.93133*NTU-0.69231*NTU**2+0.28893*NTU**3-0.063
953*NTU**4+0.0057472*NTU**5
IF (R.EQ.0.90) THEN
WRITE (6,60) E2
ELSE
CALL INTERP (R,R1,R2,E1,E2,E)
WRITE (6,60) E

```

* *

```

ENDIF
ENDIF
IF (R.GT.0.90) THEN
IF (R.LE.0.95) THEN

```

```

R1=0.90
R2=0.95
E1=0.00391805+0.93133*NTU-0.69231*NTU**2+0.28893*NTU**3-0.063
953*NTU**4+0.0057472*NTU**5
E2=0.00418844+0.92723*NTU-0.70050*NTU**2+0.29533*NTU**3-0.065
754*NTU**4+0.0059298*NTU**5
IF(R.EQ.0.95) THEN
  WRITE (6,60) E2
ELSE
  CALL INTERP (R,R1,R2,E1,E2,E)
  WRITE (6,60) E
ENDIF
ENDIF
ENDIF
IF (R.GT.0.95) THEN
  IF (R.LE.1.00) THEN
    R1=0.95
    R2=1.00
    E1=0.00418844+0.92723*NTU-0.70050*NTU**2+0.29533*NTU**3-0.065
    754*NTU**4+0.0059298*NTU**5
    E2=0.00435186+0.92385*NTU-0.71022*NTU**2+0.30310*NTU**3-0.068
    037*NTU**4+0.0061690*NTU**5
    IF(R.EQ.1.00) THEN
      WRITE (6,60) E2
    ELSE
      CALL INTERP (R,R1,R2,E1,E2,E)
      WRITE (6,60) E
    ENDIF
  ENDIF
ENDIF
ENDIF
ENDIF
STOP
END
SUBROUTINE INTERP (R,R1,R2,E1,E2,E)
  E=0.0
  E=(E1-E2)*(R-R2)/(R1-R2)+E2
  RETURN
END

```

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