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IBIS

Quarterly Report

Analysis of Cost:
Combustion Flame CVD Diamond Deposition

Contract Number: N00014-93-C2044

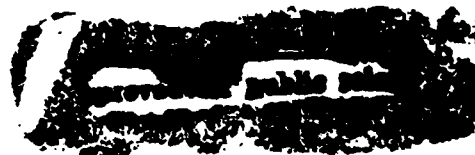
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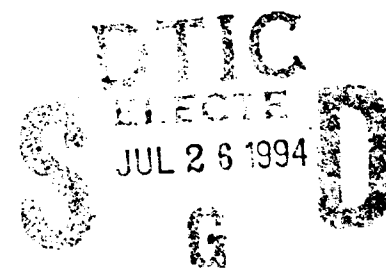
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Second Quarter 1994

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Executive Summary

IBIS Associates has improved its predictive spreadsheet model of combustion flame chemical vapor deposition (CVD) diamond film fabrication. This report explains the improvements on the combustion flame deposition theory, and shows preliminary results of the economics of this CVD diamond process.

The changes to the model include the incorporation of thermal conductivity as an input to the model, allowing the user to specify the thermal properties of the diamond being formed. Also, the deposition theory in the model has been streamlined with the assistance of diamond deposition experts. Numerous inputs have been eliminated in this process, making the model easier to use.

For this report and the results contained herein, it is assumed that the transport theory model which predicts growth rates in the CVD diamond technical cost model closely predicts actual growth rates for the combustion flame technology and that the input values for variables such as the gas flow rate and substrate diameter are physically achievable.

To be investigated are alternative combustion flame deposition geometries and chemistries. Expert review has revealed that the deposition geometry assumptions (i.e. nozzle:substrate diameter ratio) in the IBIS model may not be optimal for combustion flame deposition. Suggested changes in deposition geometries involve the size, shape, and distance to substrate of the combustion nozzle, as well as higher flow rates at smaller nozzle sizes. Suggested changes in deposition chemistry include using ethylene as the carbon fuel instead of acetylene. Lastly, expert approval of the models is continually in progress.

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Combustion Flame TCM Expert Review

The combustion flame CVD diamond Technical Cost Model (in the Appendix) has been reviewed by deposition experts representing Sandia National Laboratories in both Albuquerque, NM and Livermore, CA; Stanford University; Caltech; and Lockheed. Copies of the model were transferred to these theorists along with a non-transferable site license, and all were tutored on the Technical Cost Modeling methodology. A thorough expert review of the combustion flame model was undertaken during this tutorial. In response to the model criticism that surfaced, a plan for the revision of the cost model was drafted.

The expert review of the combustion flame CVD diamond cost model produced no significant criticisms. There was a consensus among the theorists that two of the three quality measures, as reported in the first quarter report for 1994, are unnecessary. The model has been streamlined to use only one of the quality measures (H/CH₃), which is believed to correlate the closest to thermal conductivity.

A defect-based model of CVD diamond material properties has been developed by Michael Coltrin at Sandia National Laboratories and David Dandy at Colorado State University. Inputs to this model include the hydrogen (H) and methyl radical (CH₃) mole fractions at the growth surface, as well as numerous rate constants for the reactions considered at the growth surface. Outputs of this model include the growth rate and defect density, which are used to determine thermal conductivity. IBIS generated data from this model and performed regression analysis in order to find the H/CH₃ ratio as a function of thermal conductivity. As shown later in this report, the relationship assumed to exist between H/CH₃ and the thermal conductivity of the CVD diamond allows thermal conductivity to exist as an input to the cost model.

The model's shortcomings were identified by the experts as its inability to predict the effects of changing in reactor pressure, fuel chemistry, or nozzle count. The consensus was reached that a new version of the model should be developed with the ability to predict changes in these three conditions. Due to the large amount of data required to derive predictive relationships for all these processing parameters and the nonexistence of this data in the public domain, a plan for data collection from numerical models was established. As agreed, all organizations involved in the expert review with the exception of Lockheed will cooperate in the data generation.

Sensitivity Analysis

Technical Cost Modeling permits the flexibility of performing sensitivity analyses. Using sensitivity analyses, it is possible to explore the cost implications of changing key input variables such as gas composition, production volume, material prices, product dimensions, etc. As an R&D management tool, these analyses help set development goals for cost effective manufacturing. Further, they help in long term planning, by indicating the cost savings that may be realized through scale-up. For the purpose of these sensitivity analyses it is assumed that the transport theory model which is used to estimate the diamond growth rate closely predicts actual growth rates and that the input values for variables such as gas flow rate and substrate temperature are physically achievable. Presented in the following sections are the following analyses, all based on the assumption of thermal management quality diamond:

- Cost vs Substrate Diameter and Gas Consumption
- Cost vs Thermal Conductivity and Gas Ratio
- Cost vs Thermal Conductivity and Substrate Diameter

For all of these analyses, the ratio of substrate to duct area is held constant. This constraint is due to the geometry assumed for the combustion flame technology as modeled (i.e., a single nozzle torch). The area of the gas duct is the cross-sectional area of the flame before it is affected by the flow pattern around the substrate. For a combustion flame with a corresponding duct area impinging on an infinite plane, there will be a circular region of desirable diamond and a surrounding region of unacceptable diamond. Consider the similar case of a flame impinging on a substrate of the same area. As a substrate diameter increases while the duct diameter remains constant, there is a point at which the substrate extends into this zone of unacceptable diamond. Therefore, there is a maximum substrate:duct area ratio that should not be exceeded. Experts in CVD diamond deposition suggest that this ratio is roughly 3:1 for single nozzle torches. When the substrate diameter is varied in the following analyses, the duct diameter is adjusted so that the ratio of substrate to duct area is constant.

Cost vs Substrate Diameter and Gas Consumption

Figure 1 shows the combustion flame deposition cost per square centimeter of one millimeter thick polycrystalline diamond varying with the diameter of the deposited wafer. In addition, because the duct area and gas flow rate increase with substrate area, Figure 1 shows the total gas flow rate changing with the substrate diameter. The volumetric gas flow rate must change with the duct diameter, if constant quality is to be maintained, due to the assumptions in deposition theory that are mentioned in the first quarter report of 1994. At about nine centimeters in diameter, the cost per square centimeter of combustion flame CVD diamond reaches a minimum of roughly \$60. The incorporation of the gas flow rate plot illustrates why there exists an optimum substrate diameter: as the duct area increases to

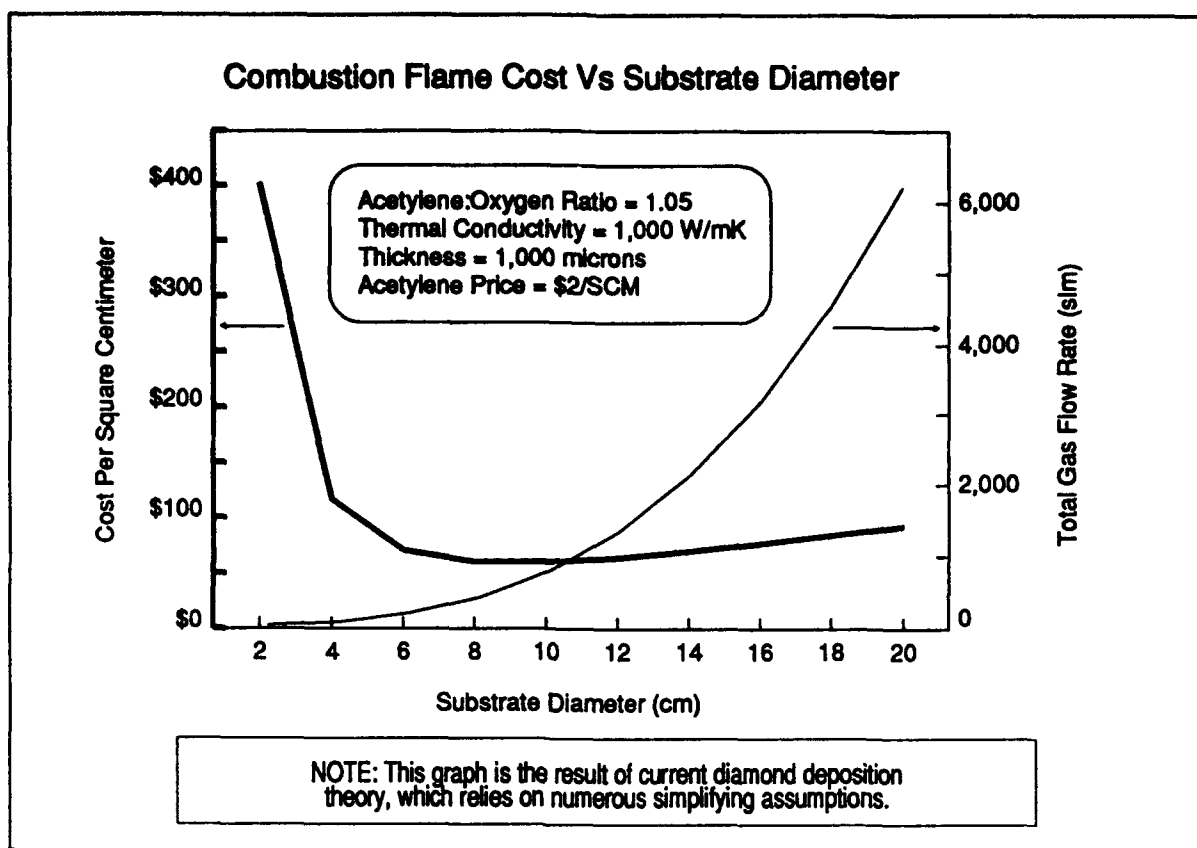


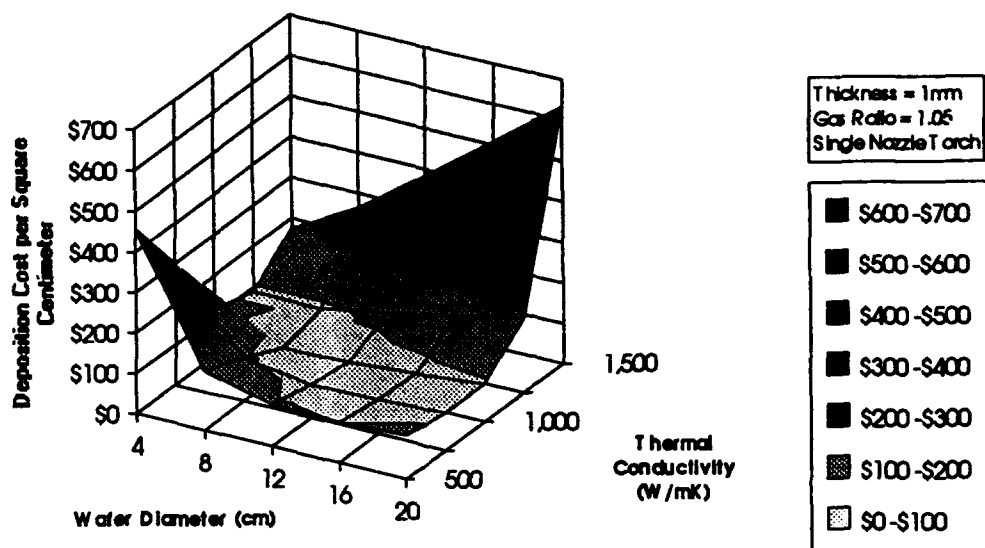
Figure 1

maintain the substrate to duct area ratio, the volumetric gas flow rate must also increase to sustain the same strain rate parameter (same quality diamond). Therefore, the economy of scaling the substrate diameter peaks at about nine centimeters, above which the required gas flow increases the cost.

Cost vs Thermal Conductivity and Gas Ratio

The effect of quality, in terms of thermal conductivity, on CVD diamond deposition cost at different gas ratios can be seen in Figure 2. The reason for the rise in cost with thermal conductivity relates to the correlation between purity and thermal conductivity. For this simulation, the purity of diamond is assumed to depend on the ratio of atomic hydrogen to methyl radicals at the growth surface; this model predicts that thermal conductivity will increase with this ratio. Increasing the ratio of atomic hydrogen to methyl radicals, while keeping the proportion of acetylene to oxygen flow constant, requires an increase in the flow rate of the inlet gases. As shown in Figure 1, increasing flow rates leads to rising costs. From Figure 2, higher thermal conductivity diamond (1,000 to 1,500 W/mK) should be grown at lower ratios of acetylene to oxygen, dropping the cost by a factor of four when lowering this ratio from 1.10 to 1.02 at 1,500 W/mK. Also shown in Figure 2 is the cost of thermal conductivity. CVD diamond grown to achieve 1,000 W/mK thermal conductivity costs about an order of magnitude less than diamond with 1,500 W/mK thermal

Deposition Cost Vs. Thermal Conductivity and Substrate Diameter



NOTE: This graph is the result of current diamond deposition theory, which relies on numerous simplifying assumptions.

Figure 3

Conclusions

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Appendix

COMBUSTION FLAME CVD DIAMOND TECHNICAL COST MODEL - LONG TERM
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COMBUSTION FLAME CVD DIAMOND TECHNICAL COST MODEL - LONG TERM
IBIS ASSOCIATES, INC. Copyright (c) 1991 v4.0

Revision Date: 6/30/94

PRODUCT SPECIFICATIONS

Torch Type Single Nozzle
Part Name 6 in. substrate
Wafer Diameter 15.24 cm
Finished Wafer Thickness 1,000 um
Thermal Conductivity 1,000 W/mK
Annual Production Volume 1.0 (000/yr)
Length of Production Run 5 yrs

PROCESS RELATED FACTORS - SURFACE PREPARATION

Process In Use? 1 [1-Y 0=N]
Dedicated Investment 0 [1-Y 0=N]
Process Yield 95.0%
Average Equipment Downtime 20.0%
Direct Laborers Per Station 0.50

Building Space Requirement

Substrate Material 11 [menu #]
Pieces Per Batch 20 pcs/batch
Process Time 60.00 min/batch
Building Space Requirement 250 sqft/sta

PROCESS RELATED FACTORS - DEPOSITION

Process In Use? 1 [1-Y 0=N]
Dedicated Investment 0 [1-Y 0=N]
Process Yield 87.5%
Average Equipment Downtime 15.0%
Direct Laborers 0.40 /sta

Machine Power

Machine Load/Unload Time 2 kW
Available Deposition Time 120 min/batch
Heat Removal via Substrate 8,640 hrs/yr
Coolant Temp. Rise 50.0% of total
Heat Capacity of Coolant 50 C
Building Space Requirement 1.0 cal/g/C
1,500 sqft/sta

Acetylene:Oxygen Ratio (R)

Oxygen 1.05 [1.02<x<1.1] GRATIO2
Acetylene 26 [menu #] GAS2
20 [menu #] GASB2

Oxygen Recycle Rate

Carrier Gas Recycle Rate 0.0%
Gas Recycle Equipment Cost 0.0%
#N/A total

Growth Correction Factor (f)

Substrate:Duct Area Ratio 0.50
Substrate Distance:Duct Diam 3.00 [1<x<=4]
1.00 [0<x<=10] L:D2

PROCESS RELATED FACTORS - ETCHING

GAS DATABASE

#	Gas	Source	Purity	Price \$/SCM	No. of carbons	Mo. Tank	Rental	Price Update
0	None			\$0.00	0.00	0E+00		
1	Liq Hydrogen	Airco 99.998%		\$0.34	0.00	3E+04	\$2,070	1/93
2	Liq Hydrogen	Airco 99.998%		\$0.32	0.00	4E+04	\$2,970	1/93
3	Liq Hydrogen	Airco 99.998%		\$0.30	0.00	1E+05	\$4,500	1/93
4	Liq Argon	Airco 99.998%		\$1.41	0.00	8E+03	\$590	1/93
5	Liq Argon	Airco 99.998%		\$1.32	0.00	2E+04	\$820	1/93
6	Liq Argon	Airco 99.998%		\$1.29	0.00	3E+04	\$1,300	1/93
7	Hydrogen	MG Ind. 99.999%		\$29.86	0.00	0E+00		1/93
8	Hydrogen	MG Ind. 99.999%		\$40.61	0.00	0E+00		1/93
9	Hydrogen	MG Ind. 99.999%		\$10.28	0.00	0E+00		1/93
10	Hydrogen	Air Prod. 99.95%		\$1.59	0.00	0E+00		1/93
11	Argon	MG Ind. 99.999%		\$33.09	0.00	0E+00		1/93
12	Argon	Air Prod. 99.999%		\$37.33	0.00	0E+00		1/93
13	Argon	Air Prod. 99.999%		\$11.74	0.00	0E+00		1/93
14	Argon	Air Prod. 99.997%		\$2.03	0.00	0E+00		1/93
15	Methane	Air Prod. 99.99%		\$21.99	1.00	0E+00		1/93
16	Methane	Air Prod. 99%		\$13.76	1.00	0E+00		1/93
17	Methane	Air Prod. 93%		\$4.93	1.00	0E+00		1/93
18	Acetylene	Air Prod. 99.6%		\$9.70	2.00	0E+00		1/93
19	Acetylene	Air Prod. 98.5%		\$5.30	2.00	0E+00		1/93
20	Acetylene	Pipeline 98.5%		\$2.00	2.00	0E+00		1/93
21	Helium	Air Prod. 99.999%		\$15.90	0.00	0E+00		1/93
22	Helium	Air Prod. 99.995%		\$4.77	0.00	0E+00		1/93
23	Nitrogen	Air Prod. 99.999%		\$45.50	0.00	0E+00		1/93
24	Nitrogen	MG Ind. 99.999%		\$9.23	0.00	0E+00		1/93
25	Nitrogen	Air Prod. 99.998%		\$1.24	0.00	0E+00		1/93
26	Liq Oxygen	Air Prod. 99.5%		\$0.21	0.00	1E+00	\$350	1/93
27	Oxygen	Air Prod. 99.5%		\$0.58	0.00	0E+00		1/93

SUBSTRATE DATABASE

#	Substrate	Source	Price \$/ea	Thick um	Diam cm	Etch um/min	Life use#	Price Update
0	None		\$0.00	1	1.00	1.00	1.00	
1	Silicon	SI-Tech	\$2.65	1270.00	5.08	20.00	1	1/93
2	Silicon	SI-Tech	\$3.50	1270.00	7.62	20.00	1	1/93
3	Silicon	SI-Tech	\$6.25	1270.00	10.16	20.00	1	1/93
4	Silicon	SI-Tech	\$9.70	1270.00	12.70	20.00	1	1/93
5	Silicon	SI-Tech	\$18.60	1270.00	15.24	20.00	1	1/93
6	Silicon	SI-Tech	\$57.95	1270.00	20.32	20.00	1	1/93
7	Silicon	SI-Tech	\$4.35	3810.00	5.08	20.00	1	1/93
8	Silicon	SI-Tech	\$8.15	3810.00	7.62	20.00	1	1/93
9	Silicon	SI-Tech	\$14.50	3810.00	10.16	20.00	1	1/93
10	Silicon	SI-Tech	\$22.65	3810.00	12.70	20.00	1	1/93

Process In Use?	1 [1-Y 0=N]	USE3	11	Silicon	SI-Tech	\$43.45	3810.00	15.24	20.00	1	1/93
Dedicated Investment	0 [1-Y 0=N]	DED3	12	Silicon	SI-Tech	\$135.20	3810.00	20.32	20.00	1	1/93
Process Yield	99.0%	YLD3	13	Silicon	SI-Tech	\$6.85	6350.00	5.08	20.00	1	1/93
Average Equipment Downtime	10.0%	DOWN3	14	Silicon	SI-Tech	\$12.80	6350.00	7.62	20.00	1	1/93
Direct Laborers Per Station	1.00	NLAB3	15	Silicon	SI-Tech	\$22.75	6350.00	12.70	20.00	1	1/93
Load/Unload and Rinse Time	30.00 min/batch	PRIME3	16	Silicon	SI-Tech	\$35.55	6350.00	10.16	20.00	1	1/93
Pieces Per Batch	20	PCS3	17	Silicon	SI-Tech	\$68.30	6350.00	15.24	20.00	1	1/93
Machine Cost	\$6,000 /sta	MCH3	18	Silicon	SI-Tech	\$212.45	6350.00	20.32	20.00	1	1/93
Echant Cost	\$70 /liter	ETCH3A	19	Molybdenum Phil. Elmet		\$3.90	254	5.08	10.00	1	1/93
Echant Disposal Cost	\$30 /liter	ETCH3B	20	Molybdenum Phil. Elmet		\$8.20	254	10.16	10.00	1.00	1/93
Machine Echant Capacity	1.00 l/batch	CAP3	21	Molybdenum Phil. Elmet		\$14.50	254	15.24	10.00	1.00	1/93
Machine Power	0.00 kW	POW3	22	Molybdenum.logies Corp		\$25.35	254	20.32	10.00	1.00	1/93
Building Space Requirement	100 sqft/sta	FLR3	23	Molybdenum.logies Corp		\$4.80	508.00	5.08	10.00	4	1/93
PROCESS RELATED FACTORS - LASER TRIMMING			24	Molybdenum.logies Corp		\$14.75	508.00	10.16	10.00	4	1/93
Process In Use?	1 [1-Y 0=N]	USE4	25	Molybdenum.logies Corp		\$24.30	508.00	15.24	10.00	4	1/93
Dedicated Investment	0 [1-Y 0=N]	DED4	26	Molybdenum.logies Corp		\$37.10	508.00	20.32	10.00	4	1/93
Process Yield	99.0%	YLD4	27	Molybdenum Phil. Elmet		\$9.15	1524.00	5.08	10.00	20	1/93
Average Equipment Downtime	10.0%	DOWN4	28	Molybdenum.logies Corp		\$27.60	1524.00	10.16	10.00	20	1/93
Direct Laborers Per Station	1.00	NLAB4	29	Molybdenum.logies Corp		\$52.25	1524.00	15.24	10.00	20	1/93
Machine Cost	\$6,000 /sta	MCH4	30	Molybdenum.logies Corp		\$85.25	1524.00	20.32	10.00	20	1/93
Trimming Rate	1.00 cm/s	RATE4	31	Molybdenum.logies Corp		\$14.75	2286.00	5.08	10.00	32.00	1/93
Machine Power	0.00 kW	POW4	32	Molybdenum.logies Corp		\$36.00	2286.00	10.16	10.00	32.00	1/93
Building Space Requirement	100 sqft/sta	FLR4	33	Molybdenum.logies Corp		\$69.00	2286.00	15.24	10.00	32.00	1/93
PROCESS RELATED FACTORS - LAPPING			34	Molybdenum.logies Corp		\$113.50	2286.00	20.32	10.00	32.00	1/93
Process In Use?	1 [1-Y 0=N]	USE5	35	Molybdenum.logies Corp		\$18.50	3175.00	5.08	10.00	46.00	1/93
Dedicated Investment	0 [1-Y 0=N]	DED5	36	Molybdenum.logies Corp		\$46.75	3175.00	10.16	10.00	46.00	1/93
Process Yield	90.0%	YLD5	37	Molybdenum.logies Corp		\$90.50	3175.00	15.24	10.00	46.00	1/93
Average Equipment Downtime	15.0%	DOWN5	38	Molybdenum.logies Corp		\$149.00	3175.00	20.32	10.00	46.00	1/93
Direct Laborers Per Station	1.00	NLAB5	39	Tungsten.logies Corp		\$7.75	254	5.08	10.00	1	1/93
Lapped Material Removal	10.0% by wgt	TLAP5	40	Tungsten.logies Corp		\$24.50	254	10.16	10.00	1.00	1/93
No of Lapping Steps	2	LAPS5	41	Tungsten.logies Corp		\$50.00	254	15.24	10.00	1.00	1/93
Pieces Per Batch	5	PCS5	42	Tungsten.logies Corp		\$79.25	254	20.32	10.00	1.00	1/93
Load/Unload and Clean Wafers	40.00 min/batch	PRIME5	43	Tungsten.logies Corp		\$10.00	508.00	5.08	10.00	4.00	1/93
Average Lapping Rate	1.0 um/hr	RATE5	44	Tungsten.logies Corp		\$35.10	508.00	10.16	10.00	4.00	1/93
Lapping Slurry Cost	\$53 /liter	LAPSL5	45	Tungsten.logies Corp		\$67.00	508.00	15.24	10.00	4.00	1/93
Lapping Slurry Usage Rate	0.50 liter/hr	LAPRS5	46	Tungsten.logies Corp		\$109.20	508.00	20.32	10.00	4.00	1/93
Lapping Plate Life	320 hrs	PLAL5	47	Tungsten.logies Corp		\$50.00	1524.00	5.08	10.00	20.00	1/93
Available Lapping Time	8,640 hrs/yr	DAYHR5	48	Tungsten.logies Corp		\$112.00	1524.00	10.16	10.00	20.00	1/93
Building Space Requirement	400 sqft/sta	FLR5	49	Tungsten.logies Corp		\$317.00	1524.00	15.24	10.00	20.00	1/93
PROCESS RELATED FACTORS - MICROSCOPY			50	Tungsten.logies Corp		\$422.00	1524.00	20.32	10.00	20.00	1/93
Process In Use?	1 [1-Y 0=N]	USE6	51	Tungsten.logies Corp		\$60.00	3175.00	5.08	10.00	46.00	1/93
Dedicated Investment	0 [1-Y 0=N]	DED6	52	Tungsten.logies Corp		\$161.25	3175.00	10.16	10.00	46.00	1/93
Process Yield	95.0%	YLD6	53	Tungsten.logies Corp		\$21.30	3175.00	15.24	10.00	46.00	1/93
Average Equipment Downtime	5.0%	DOWN6	54	Tungsten.logies Corp		\$687.00	3175.00	20.32	10.00	46.00	1/93
Direct Laborers Per Station	1.00	NLAB6	55	Tungsten.logies Corp							

Average Inspection Time	15.00 min/batch	PTIME6
Percent Inspection	100%	INSP6
Machine Cost	\$50,000 /sta	MCH6
Machine Power	0.10 kW	POW6
Building Space Requirement	50 sqft/sta	FLR6

PROCESS RELATED FACTORS - INSPECTION - THERMAL CONDUCTIVITY

Process In Use?	1 [1-Y 0-N]	USE7
Dedicated Investment	0 [1-Y 0-N]	DED7
Process Yield	95.0%	YLD7
Average Equipment Downtime	5.0%	DOWN7
Direct Laborers Per Station	1.00	NLAB7

Average Inspection Time	15.00 min/batch	PTIME7
Percent Inspection	100%	INSP7
Machine Cost	\$50,000 /sta	MCH7
Machine Power	0.10 kW	POW7
Building Space Requirement	50 sqft/sta	FLR7

OPTIONAL INPUTS

Surface Preparation	override	estimate	
Machine Cost	\$0	\$65,774 /sta	OMCH1
Machine Power	0.0	19.2 kW	OPOW1
Deposition			
Duct Area	0.00	60.80 sqcm	ODAREA2
Total Gas Flow Rate	0	2,743 slm	OTFLOW2
Deposition Rate	0.00	1.14 g/hr	ODRATE2
Deposition Equipment Cost	\$0	\$71 ks/sta	OMCK2
Etching			
Process Cycle Time	0.00	0.18 hrs	OCTIME3
Chemical Requirement	\$0	\$5.00 /pc	OCHEM3
Laser Trimming			
Process Cycle Time	0.00	0.01 hrs	OCTIME4
Lapping			
Lapping Time	0.00	111.11 hrs	OCTIME5
Lapping Plate Cost	\$0	\$869 /ea	OWHEEL5
Lapping Machine Cost	\$0	\$11,939 /sta	OMCH5
Lapping Machine Power	0.00	4.2 kW	OPWR5

EXOGENOUS COST FACTORS

Direct Wages	\$13.33 /hr	WAGE
Indirect Salary	\$50,000 /yr	SALARY
Indirect:Direct Labor Ratio	1.00	ILAB
Benefits on Wage and Salary	35.0%	BENI
Working Days per Year	360.00	DAYS
Working Hours per Day (*)	8.00 /hr	HRS
Capital Recovery Rate	10%	CRR
Capital Recovery Period	5.00 yrs	ELIFE
Building Recovery Life	20.00 yrs	BLIFE
Working Capital Period	3.00 months	WCP

* cxc. dep. & lap

Price of Electricity	\$0.050 /kwh	ELEC
Price of Natural Gas	\$6.50 /MBTU	GAS
Price of Building Space	\$100 /sqft	PBLD
Price of Cooling Water	\$0.03 /100 gal	WATER
Auxiliary Equipment Cost	15.0%	AUX
Equipment Installation Cost	35.0%	INST
Maintenance Cost	8.0%	MNT

REGRESSION CONSTANTS, COEFFICIENTS, AND EXPONENTS

-Surface Preparation-

Machine Cost Constant	1,334	MCH1A
Machine Cost Capacity Coef	3,222	MCH1B
Machine Power Constant	-0.75	PWR1A
Machine Power Capacity Coef	1.00	PWR1B

-Deposition-

Diamond Density (g/cc)	3.52	DENS
[H]/[CH3] Quality Constant	133	QUAL3
[H]/[CH3] Quality Coefficient	164	QUAL3A
[H]/[CH3] Qual. GRatio Exp.	20	QUAL3B
[H]/[CH3] Qual. QMult. Exp.	1.77	QUAL3C

QMult. Coefficient	0.00	QM2A
QMult. Tc Exponent	4.07	QM2B
[H]/[CH3] Qual. Baseline	10.15	QUAL3D

Vol. Expansion Factor Const.	4.76	VEFA2
Vol. Expansion Factor Coeff.1	4.46	VEFB2
Vol. Expansion Factor Coeff.2	-1.83	VEFC2

Growth Rate 10 ^x Coeff. 3	-3.91	GRA2
Growth Rate "a" Expon. 3	2.91	GRB2
Growth Rate "a2" Expon. 3	-0.39	GRC2
Growth Rate "R" Expon. 3	23.97	GRD2
Growth Rate "R2" Expon. 3	-334.80	GRE2

Enthalpy (kcal/mol) - C2H2	54.19	HF2A
Enthalpy (kcal/mol) - CO	-26.42	HF2B

Machine Cost Wafer Area Coef	161.46	MCH2Y
Machine Cost Area Exponent	1.00	MCH2Z
Machine Cost Area Constant	41,667	MCH2X

-Etching-

-Lapping-

Machine Cost Constant	2,719	MCH5A
Machine Cost Capacity Coef	1,844	MCH5B
Machine Power Constant	-0.75	PWR5A
Machine Power Capacity Coef	1.00	PWR5B
Tool Cost Constant	771.00	TOOL5A

Tool Cost Capacity Coef 0.92 TOOL5B
Tool Cost Capacity Exponent 2.90 TOOL5C

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TECHNICAL COST MODEL (C) 1993
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COMBUSTION CVD TCM: SURFACE PREPARATION
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COMBUSTION CVD TCM: DEPOSITION			IBIS ASSOCIATES, INC. Copyright (c) 1991 v4.0		
VARIABLE COST ELEMENTS			per piece	per year percent	investment
Material Cost	\$65.66	\$65,660	94.1%		
Direct Labor Cost	\$0.85	\$850	1.2%		
Utility Cost	\$0.07	\$72	0.1%		
TOTAL FABRICATION COST					

FIXED COST ELEMENTS			per piece	per year percent	investment
Equipment Cost	\$0.65	\$647	0.9%		
Tooling Cost	\$0.00	\$0	0.0%		
Building Cost	\$0.04	\$41	0.1%		
Maintenance Cost	\$0.32	\$324	0.5%		
Overhead Labor Cost	\$0.82	\$820	1.2%		
Cost of Capital	\$1.36	\$1,364	2.0%		
TOTAL FABRICATION COST					

INTERMEDIATE CALCULATIONS			per piece	per year percent	investment
Process In Use	1.00	[1-Y 0-N]			
Cumulative Yield	66.2%				
Effective Production Volume	1,511	/yr			

INTERMEDIATE CALCULATIONS			per piece	per year percent	investment
Substrate Area	182.4	sq cm			
New Substrate Cost	\$43.45	/pc			
Substrate Useful Life	1.00	cycle			
Process Cycle Time	3	min/pc			
Runtime for One Station	3%				
Number of Parallel Stations	0.03				
Energy Requirement	0.959	kwh/pc			
Building Space/Station	250	sqft			
Machine Cost	\$65,774	/sta			
Machine Power	19.2	kW			
Installed Equipment Cost	\$88,795	/sta			
Auxiliary Equipment Cost	\$9,866	/sta			
Equipment Annuity	\$825	/yr			
Tooling Annuity	\$0	/yr			
Building Annuity	\$95	/yr			
Working Annuity	\$68,858	/yr			

INTERMEDIATE CALCULATIONS			per piece	per year percent	investment
Process In Use	1.00	[1-Y 0-N]			
Cumulative Yield	66.2%				
Effective Production Volume	1,511	/yr			

INTERMEDIATE CALCULATIONS			per piece	per year percent	investment
Process In Use	1.00	[1-Y 0-N]			
Cumulative Yield	66.2%				
Effective Production Volume	1,511	/yr			

Combustion Power	836 kW	CPOM2
Cooling Water Flow Rate	31.7 gal/min	WATER2
Cooling Water Requirement	119,343 gal/pc	COOL2
Energy Requirement	126 kWh/pc	ENERGY2
Building Space/Station	1,500 sqft	SPACE2
Recycle Equipment Cost	\$0 /sta	REC2
Liquid Oxygen Tank Rental	\$350 /mo/tank	XRENT2
Gas Storage Equipment Rent	\$4,200 /year	GTANK2
Machine Cost	\$71,120 /sta	MCH2B
Installed Equipment Cost	\$96,012 /sta	IEQUIP2
Auxiliary Equipment Cost	\$10,668 /sta	AEQUIP2
Equipment Annuity	\$344,666 /yr	EINT2
Tooling Annuity	\$0 /yr	TINT2
Building Annuity	\$220,114 /yr	BINT2
Working Annuity	\$18,394,945 /yr	WINT2

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COMBUSTION CVD TCM: IBIS ASSOCIATES, INC.				ETCHING		COMBUSTION CVD TCM: SER TRIMMING IBIS ASSOCIATES, INC.				Copyright (c) 1991 v4.0				
				per piece	per year percent	investment	VARIABLE COST ELEMENTS				per piece	per year percent	investment	
VARIABLE COST ELEMENTS														
Material Cost	\$3.98	\$3,980	29.0%				Material Cost	\$0.00	\$0	0.0%				
Direct Labor Cost	\$4.62	\$4,616	33.7%				Direct Labor Cost	\$0.33	\$331	47.8%				
Utility Cost	\$0.00	\$0	0.0%				Utility Cost	\$0.00	\$0	0.0%				
FIXED COST ELEMENTS							FIXED COST ELEMENTS							
Equipment Cost	\$0.16	\$160	1.2%	\$9,000			Equipment Cost	\$0.01	\$11	1.7%	\$9,000			
Tooling Cost	\$0.00	\$0	0.0%	\$0			Tooling Cost	\$0.00	\$0	0.0%	\$0			
Building Cost	\$0.04	\$45	0.3%	\$10,000			Building Cost	\$0.00	\$3	0.5%	\$10,000			
Maintenance Cost	\$0.14	\$135	1.0%				Maintenance Cost	\$0.01	\$10	1.4%				
Overhead Labor Cost	\$4.45	\$4,452	32.5%				Overhead Labor Cost	\$0.32	\$319	46.1%				
Cost of Capital	\$0.32	\$323	2.4%				Cost of Capital	\$0.02	\$18	2.7%				
TOTAL FABRICATION COST				\$13.71	\$13,712	100.0%	\$19,000	TOTAL FABRICATION COST				\$0.69	\$693	100.0%
														\$19,000

INTERMEDIATE CALCULATIONS				INTERMEDIATE CALCULATIONS			
	1.00	(1-Y 0-N)	PRO3		1.00	(1-Y 0-N)	PRO4
	79.6%		CYLD3		80.4%		CYLD4
	1,256	/yr	ENUM3		1,244	/yr	ENUM4
Effective Production Volume				Effective Production Volume			
Total Etchod Thickness	3,810	um	ETHIK3	Process Cycle Time	0.01	hrs/pc	CTIME4
Average Etchant Rate	20.00	um/min	ERATE3	Runtime for One Station	1%		RTIME4
Process Cycle Time	0.18	hrs/pc	CTIME3	Number of Parallel Stations	0.01		NSTAT4
Runtime for One Station	9%		RTIME3				
Number of Parallel Stations	0.09		NSTAT3				
Chemical Requirement			CHEM3	Energy Requirement	0	kWh/pc	ENERGY4
Energy Requirement	\$5.00	/pc	ENERGY3	Building Space/Station	100	sq ft	SPACE4
Building Space/Station	100	sq ft	SPACE3	Installed Equipment Cost	\$8,100	/sta	IEQUIP4
Installed Equipment Cost	\$8,100	/sta	IEQUIP3	Auxiliary Equipment Cost	\$900	/sta	AEQUIP4
Auxiliary Equipment Cost	\$900	/sta	AEQUIP3				
Equipment Annuity	\$204	/yr	EINT3	Equipment Annuity	\$15	/yr	EINT4
Tooling Annuity	\$0	/yr	TINT3	Tooling Annuity	\$0	/yr	TINT4
Building Annuity	\$103	/yr	BINT3	Building Annuity	\$7	/yr	BINT4
Working Annuity	\$13,405	/yr	WINT3	Working Annuity	\$671	/yr	WINT4

COMBUSTION CVD TCM: LAPPING				COMBUSTION CVD TCM: INSPECTION - MICROSCOPY			
IBIS ASSOCIATES, INC.				IBIS ASSOCIATES, INC.			
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per piece				per piece			
per year percent				per year percent			
investment				investment			
VARIABLE COST ELEMENTS				VARIABLE COST ELEMENTS			
Material Cost	\$725.01	\$725,009	43.2%	Material Cost	\$0.00	\$0	0.0%
Direct Labor Cost	\$586.32	\$586,316	34.9%	Direct Labor Cost	\$5.25	\$5,249	39.9%
Utility Cost	\$5.79	\$5,786	0.3%	Utility Cost	\$0.00	\$1	0.0%
FIXED COST ELEMENTS				FIXED COST ELEMENTS			
Equipment Cost	\$13.50	\$13,503	0.8%	Equipment Cost	\$1.52	\$1,519	11.6%
Tooling Cost	\$74.41	\$74,415	4.4%	Tooling Cost	\$0.00	\$0	0.0%
Building Cost	\$7.54	\$7,540	0.4%	Building Cost	\$0.03	\$25	0.2%
Maintenance Cost	\$17.47	\$17,465	1.0%	Maintenance Cost	\$0.65	\$648	4.9%
Overhead Labor Cost	\$188.50	\$188,502	11.2%	Overhead Labor Cost	\$5.06	\$5,062	38.5%
Cost of Capital	\$59.54	\$59,540	3.5%	Cost of Capital	\$0.63	\$634	4.8%
TOTAL FABRICATION COST	\$1,678.08	\$1,678,077	100.0%	TOTAL FABRICATION COST	\$13.14	\$13,138	100.0%
\$603,707				\$80,000			

INTERMEDIATE CALCULATIONS				INTERMEDIATE CALCULATIONS			
Process In Use				Process In Use			
Cumulative Yield				Cumulative Yield			
Effective Production Volume				Effective Production Volume			
1.00	(1-Y 0-N)	PRO5	PRO6	1.00	(1-Y 0-N)	PRO6	PRO6
81.2%		CYD5	CYD6	90.3%		CYD6	CYD6
1,231	/yr	ENUM5	ENUM6	1,108	/yr	ENUM6	ENUM6
Thickness of Material Lapped	111.11	um	HLAP5	Process Cycle Time	0.25	hrs	CTIME6
Setup Time	1.33	hrs/batch	CTIME5A	Runtime for One Station	10%		RTIME6
Lapping Time	111.11	hrs/batch	CTIME5B	Number of Parallel Stations	0.10		NSTAT6
Runtime for One Station	377%		RTIME5	Energy Requirement	0	kWh/pc	ENERGY6
Number of Parallel Stations	3.77		NSTAT5	Building Space/Station	50	sq ft	SPACE6
Lapping Plate Cost	\$869	/ea	PLA5	Installed Equipment Cost	\$67,500	/sta	IEQUIP6
Lapping Plate Life	14	pcs	WHEEL5	Auxiliary Equipment Cost	\$7,500	/sta	AEQUIP6
Number of Plates Required	428.00		PLAT5	Equipment Annuity	\$1,936	/yr	EINT6
Lapping Slurry Consumption	11.11	l/pc	GRIT5	Tooling Annuity	\$0	/yr	TINT6
Machine Power	4.2	kW	PWR5	Building Annuity	\$59	/yr	BINT6
Energy Requirement	94	kWh/pc	ENERGY5	Working Annuity	\$11,143	/yr	WINT6
Machine Cost	\$11,939	/sta	MCH5	*****			
Building Space/Station	400	sq ft	SPACE5	*****			
Installed Equipment Cost	\$16,118	/sta	IEQUIP5	*****			
Auxiliary Equipment Cost	\$1,791	/sta	AEQUIP5	*****			
Equipment Annuity	\$17,214	/yr	EINT5	*****			
Tooling Annuity	\$94,865	/yr	TINT5	*****			
Building Annuity	\$17,463	/yr	BINT5	*****			
Working Annuity	\$1,548,534	/yr	WINT5	*****			

COMBUSTION CVD TCM: INSPECTION - THERMAL CONDUCTIVITY
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COMBUSTION CVD TCM: COST SUMMARY
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VARIABLE COST ELEMENTS			VARIABLE COST ELEMENTS		
per piece	per year	percent	per piece	per year	percent
Material Cost	\$0.00	0.0%	Material Cost	\$17,524.87	84.5%
Direct Labor Cost	\$4.99	38.7%	Direct Labor Cost	\$1,390.63	6.7%
Utility Cost	\$0.00	0.0%	Utility Cost	\$66.28	0.3%
FIXED COST ELEMENTS			FIXED COST ELEMENTS		
Equipment Cost	\$1.52	11.8%	Equipment Cost	\$287.72	1.4%
Tooling Cost	\$0.00	0.0%	Tooling Cost	\$74.41	0.4%
Building Cost	\$0.03	0.2%	Building Cost	\$102.72	0.5%
Maintenance Cost	\$0.65	5.0%	Maintenance Cost	\$279.44	1.3%
Overhead Labor Cost	\$5.06	39.3%	Overhead Labor Cost	\$457.65	2.2%
Cost of Capital	\$0.63	4.9%	Cost of Capital	\$564.26	2.7%
TOTAL FABRICATION COST	\$12.87	100.0%	TOTAL FABRICATION COST	\$20,747.99	100.0%
				\$113.74 /sqcm	

INTERMEDIATE CALCULATIONS

Process In Use	1.00 [1-Y 0-N]	PRO7
Cumulative Yield	95.0%	CYLD7
Effective Production Volume	1.053 /yr	ENUM7
Process Cycle Time	0.25 hrs	CTIME7
Runtime for One Station	10%	RTIME7
Number of Parallel Stations	0.10	NSTAT7
Energy Requirement	0 kWh/pc	ENERGY7
Building Space/Station	50 sq ft	SPACE7
Installed Equipment Cost	\$67,500 /sta	IEQUIP7
Auxiliary Equipment Cost	\$7,500 /sta	AEQUIP7
Equipment Annuity	\$1,936 /yr	EINT7
Tooling Annuity	\$0 /yr	TINT7
Building Annuity	\$59 /yr	BINT7
Working Annuity	\$10,877 /yr	WINT7

SUMMARY INFORMATION

Part Name 6 in. substrate	
Total Direct Laborers	13.70 /shift
Total Floor Space	21,650 sqft
Total Capital Investment	\$4.3 MM
Area Cost	\$113.74 /sqcm
Cost Per Carat	\$64.81 /ct

Operation	Equipment	Material	Labor	Other
Surface Preparation	\$1	\$66	\$2	\$2
Deposition	\$270	\$16,730	\$1,042	\$917
Etching	\$0	\$4	\$9	\$1
Laser Trimming	\$0	\$0	\$1	\$0
Lapping	\$14	\$725	\$775	\$165
Inspect - Microscopy	\$2	\$0	\$10	\$1
Inspect - Thermal Cond'vity	\$2	\$0	\$10	\$1
Total	\$288	\$17,525	\$1,848	\$1,087
Total =	\$20,748			